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Subject: Comments in Opposition to Proposed RCRA permit for Evoqua Water Technologies LLC from Greenaction for Health and Environmental Justice
Date: Monday, January 09, 2017 12:34:23 PM
Attachments: [evoqua_proposed_permit_fs_english_26sep2016_web.pdf](#)
[evoqua-hhera-risk-assess-factsheet-2016-06.pdf](#)
[FINAL-Evoqua CI FS Mailer English Spanish 6.15.16-1.pdf](#)
[US Filter Westates Facility Description document.pdf](#)
[WestatesPDTReportRev0 2012 \(of 2006 test\).pdf](#)
[Chairman Eddy letter to EPA re NHPA & sacred areas Sept 10, 2003.pdf](#)
[EPA LETTER TO CRIT Council 8-30-09.pdf](#)
[Comments on Evoqua draft permit by Greenaction for Health and Environmental Justice.pdf](#)

Attached please find comments from Greenaction for Health and Environmental Justice in opposition to the Proposed RCRA permit for the Evoqua Water Technologies LLC facility near Parker, Arizona on the lands of the Colorado River Indian Tribes.

Please confirm that you have received these comments which include the narrative and attachments.

Thank you,

Bradley Angel

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January 9, 2017

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Submitted January 9, 2017 by email to Zabaneh.Mahfouz@epa.gov

Greenaction for Health and Environmental Justice Comments to US EPA in Opposition to Proposed Permit for the Evoqua Water Technologies LLC facility near Parker, Arizona on the Colorado River Indian Tribes reservation

Greenaction for Health and Environmental Justice submits these comments in opposition to the proposed permit for the Evoqua Water Technologies LLC facility (Evoqua) operating on the Colorado River Indian Tribes (CRIT) reservation near Parker, Arizona. We submit these comments on behalf of Greenaction's members and constituents who are CRIT tribal members and other Greenaction members who live in the area.

I. Issuance of a RCRA permit would violate numerous laws and policies:

US EPA must not and cannot issue a permit for the Evoqua facility. EPA's has continuously violated its responsibility to conduct a fair, impartial, unbiased, accurate and just permit process that complies with your regulatory, legal and environmental justice obligations. Your regulatory history at the facility and the proposed permit clearly violate the following:

- USEPA's trust responsibility to Native Nations including, timely and good faith tribal consultation
- National Historic Preservation Act
- Executive Order 12898 on Environmental Justice
- Title VI of the US Civil Rights Act
- RCRA
- Clean Air Act
- Native American Graves Protection and Repatriation Act of 1990 (NAGPRA)
- American Indian Religious Freedom Act of 1978
- Executive Order 13007 – Indian Sacred Sites.

II. USEPA bias completely tainted legitimacy of the permit process by improperly allowing the facility to operate for a quarter of a century without proper permits or landowner signature:

The fact that USEPA has improperly allowed this hazardous waste facility to operate and pollute the air, water, people, sacred and culturally significant sites of the Colorado River Indian Tribes for a quarter of a century without proper studies, permit application requirements or permits is nothing less than environmental racism as it demonstrates a complete bias in favor of the company and violation of numerous laws and policies.

The first part of the permit application was submitted to USEPA in 1995, four years after the facility began operating and four years after EPA required such facilities to obtain hazardous waste permits.

The fact that EPA has allowed this permit process to drag on for 22 years is improper and illegal, demonstrating either incompetence or illegal bias in favor of a company that treats hazardous waste shipped to the facility from federal government agencies and industries across the nation.

Very importantly, USEPA violated RCRA by allowing the facility to operate on tribal lands on “interim status” for approximately 25 years without the required landowner signature on a Final Part B permit application. The USEPA should have denied the permit application in 1995 when it lacked landowner signature – the signature of the Colorado River Indian Tribes government.

We incorporate into our comments (attached) the July 30, 2009 USEPA Region IX document entitled “SUBJECT: Key US EPA Messages for the Colorado River Indian Tribes (CRIT) August 3, 2009 Council Meeting Regarding the Siemens Water Technologies/CRIT Final Permit Application” included the following “Key US EPA Messages”:

“6) At the May 18, 2009 CRIT Council Meeting, USEPA requested a decision by June 12, 2009, from the Council on whether it intended to sign the Final Part B Application;

7) To date CRIT has neither signed the Application nor in any way indicated its intention to do so;

8) Therefore, the USEPA considers it no longer appropriate for Siemens to continue operating under interim status conditions without a targeted date for resolution of the pending application status;

9) *Accordingly, if USEPA does not receive a complete Final Part B Application from Siemens and the CRIT by September 1, 2009, it plans to issue a formal Notice of Deficiency (NOD) of the Application and proceed to denial of a final operating permit;” (Emphasis added).*

It is a fact that USEPA did not receive a complete Final Part B Application until April 25, 2016, seven years after its alleged deadline that would trigger a permit denial. Instead of denying the permit as it was legally required to do, USEPA continued to improperly allow the facility to operate and emit hazardous pollutants into the air and Colorado River for seven more years.

In addition, these comments – from EPA’s own records and documents – will clearly demonstrate that EPA provided misinformation to the tribal government and tribal members and also withheld other important information that may have led to the tribe signing the permit application last year.

III. USEPA permit process has been illegitimate and biased due to pre-determined outcome - USEPA always intended to issue permit and admitted so in writing, even while claiming they were neutral:

USEPA’s own “fact sheets,” public statements and actions over 25 years demonstrate USEPA’s pro-facility bias.

However, clear written proof of USEPA’s pro-polluter bias can be seen in print and proves that USEPA always intended to issue the permit to this facility even before any public comment period began, any test burn was done, or any Statement of Basis written.

A USEPA “fact sheet” found at <https://www3.epa.gov/region9/waste/hazwaste/index.html> states the following:

“EPA Region 9 is in the process of issuing permits at the following facilities:

- [Evoqua Carbon/U.S. Filter \(Parker, AZ\)](#)
- [Romic \(Chandler, AZ\)”](#)

USEPA’s written statement in this document that they were “in the process of issuing permits...” proves that USEPA has for many years always intended to issue a permit regardless of the facts including public comments submitted during the public comment period. The document was likely written at least a decade ago and is still publicly available.

This pre-determined outcome in the permit process is completely improper and illegal, and makes a mockery of USEPA’s written and verbal claims (including at the November 1, 2016 public hearing) that they were neutral in the permit process – and violates legal mandates for meaningful public participation and a legitimate permit decision based on all the relevant facts.

It must be noted that the Romic facility referenced in the EPA document excerpted above was also located on tribal lands on the Gila River Indian Community and was allowed to operate by USEPA without landowner signature, proper permits, or environmental review for decades.

Romic was yet another example of USEPA's practice of environmental racism against indigenous peoples.

IV. USEPA has illegally allowed the facility to operate for a quarter of a century without an Environmental Impact Statement and an EIS public participation process:

No Environmental Impact Statement was ever performed for this hazardous waste facility. The failure of USEPA and BIA to require an EIS resulted in the lack of a robust public process and thorough environmental review of the proposed facility which emits a wide range of hazardous chemicals into the air and Colorado River.

V. USEPA allowed the facility to operate for 15 years without requiring a "Human Health and Ecological Risk Assessment" and the assessment done by the company in 2007 lacked any public participation component:

The facility completed a "Human Health and Ecological Risk Assessment" in 2007, 15 years after being allowed by EPA to pollute the air, water, land, people and culturally significant sites of the Colorado River Indian Tribes. According to an EPA "fact sheet," USEPA used this study to conclude "that human health impacts from long term exposure to stack emissions, fugitive emissions, as well as the combination of the two, were below EPA's acceptable thresholds.

This Risk Assessment was not developed with public input and was based on faulty and incomplete information.

VI. USEPA's risk analysis is based in significant part on a grand total of one trial burn/stack test and that test was flawed and problem-plagued

USEPA's so-called "fact sheet" entitled "Risk Assessment at Evoqua Water Technologies" issued June 2016 (www.epa.gov/az/evoqua-air-emissions-and-risk-assessment), the September 2016 USEPA Region IX "Revised Draft RCRA Facility Assessment Report" for the Evoqua facility" https://www.epa.gov/sites/production/files/2016-09/documents/azd982441263_draft_rfa_report_evoqua_water_technologies_llc_2016-09-27.pdf

make claims about stack emissions and the supposed risk from those emissions that are without basis in fact or reality.

Despite operating for a quarter of a century, there has been only one stack test in March 2006 and that was conducted by the facility, not USEPA. USEPA allowed the company to emit hazardous pollutants for 14 years without ever once requiring a test burn until 2006 – another example of pro-polluter bias by USEPA.

A big additional problem with USEPA's use of the results of the stack test in determining risk is that the company knew they were going to be tested and when it was to occur, so they were able to prepare – clearly this is not the same as would occur under normal operating conditions.

Despite knowing in advance when the test would occur, the test burn had many operational problems. Serious problems with the test burn/stack test are detailed in the “Performance Demonstration Test Report Prepared for Siemens Water Technologies, Corp., June 30, 2006, by Focus Environmental Inc. This report is incorporated into our comments. This report contained the following information on pages 15-17:

- Test team arrived 7 am March 28, 2006 – “Entire RF-2 unit experienced a shutdown at 7:56 am due to over-amperage of the ID fan.”
- March 29: “Glass probe liner broke...and sampling was immediately stopped.”
- March 30: “At 08:58 a weld on the nipple attached to the carbon feed chute used for spiking material injection was noticed to be cracked. Spiking was immediately stopped and the weld was repaired.”
- March 30: “PDT Run 3 was started at 11:50 on March 30, 2006. All sampling activities were placed on hold at 12:39 when it was noted that the organic surrogate mixture was not flowing correctly through the spiking system.”

There were thus at least four major problems including at least three shutdowns in just three days of tests. Despite these problems including at least three shutdowns, the PDT Report's Executive Summary (page 12) states that “Specific conclusions drawn from the PDT are as follows: The RF-2 system operated reliably during each PDT run, and was able to maintain operating conditions which were consistent with the target values stated in the PDT Plan. The test results are suitable for establishing operating parameter limits.”

These problems were never revealed to CRIT or the public in a transparent manner – this information to our knowledge was never reported in a USEPA fact sheet, report or verbal presentation to the public including CRIT tribal government or members. It is thus yet another example of improper bias in USEPA's regulatory and permitting role.

VII. USEPA falsely claimed it conducted the test burn and provided “oversight”:

The “Performance Demonstration Test” Report referenced above says in its “Test Implementation Summary” on page 14 the following which clearly documents that the company conducted the test and not EPA. It also proves that EPA staff members were present only for portions of the test:

“The PDT program was conducted under the overall direction of Siemens Water Technologies Corp. personnel. Mr. Monte McCue was the overall CPT Manager for Siemens Water Technologies Corp.. Mr. Willard (Drew) Bolyard of Siemens Water Technologies Corp. oversaw plant personnel and operations during the PDT. Ms. Mary

Blevins, Ms. Stacy Braye, Mr. Steven Arman, Mr. Robert Fitzgerald, Mr. Michael Svizzero, and Ms. Karen Scheuerman of USEPA were on-site to observe portions of the PDT.”

Despite the clear facts, USEPA continues to falsely claim in writing that EPA conducted the test burn. The very first statement in the USEPA’s June 2016 “fact sheet” entitled “Risk Assessment at Evoqua Water Technologies” makes the following completely false statement:

“EPA conducted a trial burn at the facility to find out amounts of chemicals coming out of the Evoqua facility’s smokestack.”

The clear fact is that USEPA never, ever conducted a test burn at the facility. This incorrect “fact sheet” is part of the USEPA’s administrative record for this permit process and completely misleads any member of the public who reads it if they don’t know the truth. We incorporate this “fact sheet” into our comments.

In their “Revised Draft RCRA Facility Assessment Report” (September 2016) “Evoqua tested the RF-2 unit under the oversight of EPA...” (page 16). The truth is that EPA did not properly oversee the test burn – as the PDT Report documents that EPA staff members were present only for portions of the test.

VIII. USEPA’S claims about “Typical Evoqua Stack Gas Composition” are without basis in fact due to the flawed test burn and the complete failure to monitor hazardous emissions other than during the problem-plagued and brief trial burn conducted by the company:

USEPA’s “fact sheet” www.epa.gov/az/evoqua-air-emissions-and-risk-assessment has a section entitled “Typical Evoqua Stack Gas Composition” which implies that EPA knows what the typical emissions are. The EPA’s “Revised Draft RCRA Facility Assessment Report” similarly uses the results from the problem-plagued test burn to assess facility performance. In fact, USEPA has no idea if that is correct. The facts are:

- EPA has never once in a quarter of a century conducted its own test burns at the facility
- Neither EPA or the facility has ever monitored hazardous emissions other than on during a three day test in 2006 when the company conducted its own problem-plagued trial burn
- There is not and never has been continuous monitoring of the stack for emissions of hazardous air pollutants.

USEPA’s conclusions about the risk from stack emissions are thus without basis in fact, and the reality is that USEPA has no idea of what are typical emissions or if those emissions are within regulatory limits under the Clean Air Act or other applicable laws.

IX. USEPA's claim that fugitive emissions are within regulatory levels has no basis in fact:

Fugitive emissions at the facility have never been monitored, rendering USEPA claims that fugitive emissions are below regulatory levels speculation at best and clearly misleading. To our knowledge, USEPA never clearly informed CRIT that there has never been any monitoring whatsoever of fugitive emissions.

X. Potential Violation of the Clean Air Act:

The Clean Air Act requires any major source of criteria or hazardous air pollutants to obtain a Title V Clean Air Act permit. According to USEPA's "Statement of Basis" (page 7) "The Facility's uncontrolled potential to emit criteria and HAP pollutants is below applicable major source thresholds, with the exception of sulfur dioxide (SO₂) and oxides of nitrogen (NO_x)."

USEPA claims about emissions levels are based on the completely flawed and problem-plagued test burn that occurred more than a decade ago and was the only such test in a quarter century at the facility. Using this test burn to exempt the facility from Title V requirements is improper.

XI. USEPA remained silent as the facility made false claims to tribal members and the general public about emissions:

This facility was sited on CRIT lands by Westates Carbon/Wheelabrator Technologies at a time when dozens of waste disposal companies and government agencies actively and strategically targeted tribal lands for hazardous waste, solid waste and radioactive waste disposal and treatment facilities in order to exploit tribal sovereignty and avoid having to get local, county and state permits.

It is a fact that USEPA knowingly remained silent as facility operators made false claims to tribal members about emissions. For example, a US Filter public document entitled "US Filter Westates Carbon Reactivation Facility Description" states that "The exhaust of the plant, via the stack, is basically 180 degree Fahrenheit steam." This statement is clearly not correct as a wide range of hazardous chemicals are emitted into the air from the stack. We attach and incorporate this company document into our comments.

At a tour of the facility given by the plant manager for the Mohave Elders and attended by Bradley Angel, Executive Director of Greenaction, the plant manager stated that the emissions were steam. The Mohave Elders and Greenaction demanded USEPA come to CRIT and provide a workshop on dioxin and its environmental and health impacts. Patrick Wilson of USEPA did then come to CRIT and make this presentation – and this was the very first time that tribal members ever heard about dioxin from EPA.

EPA's deafening silence for years about toxic emissions and their continued practice of failing to provide accurate information about toxic emissions and risk is a violation of trust responsibility and makes a mockery of a legitimate public participation and permit process.

XII. USEPA “Fact Sheets” (September and November 2016) that accompanied the draft permit decision are biased and misleading:

Both the September and November 2016 USEPA “fact sheets” entitled “Fact Sheet: Proposed Permit for the Evoqua Water Technologies LLC Facility Near Parker, Arizona” are extremely misleading, omit vital information relevant to a robust and informed public participation process, and completely taint the legitimacy of the permit process.

These “Fact Sheets” –as well as USEPA’s June 2016 “Community Information Fact Sheet for the Evoqua Water Technologies LLC Facility Near Parker, Arizona - omit even one word about hazardous emissions into the air and water. An uninformed person reading this would never know that there are hazardous emissions. They would never know that the federal government itself sends significant amounts of hazardous wastes to the facility or that USEPA never conducted an Environmental Impact Statement for the facility. These omissions misled the public and deprived the affected public of vital information, thus undermining the integrity of the public participation process.

The link to the November 2016 document is <https://www.epa.gov/sites/production/files/2016-11/documents/azd982441263-evoqua-proposed-permit-fs-english-revised-2016-11-10.pdf>

The June and September 2016 USEPA “fact sheets” are attached.

We attach and incorporate these three USEPA “fact sheets” into our comments.

XIII. USEPA falsely claims it did a risk assessment:

USEPA’s June 2016 2016 “fact sheet” entitled “Risk Assessment at Evoqua Water Technologies” makes the following completely false statement:

“Why did EPA do a Risk Assessment?

The Evoqua facility is regulated by EPA under the Resource Conservation and Recovery Act (RCRA) because it handles hazardous waste. A Risk Assessment is one way to make sure that the facility is operating safely.”

The fact is that USEPA never did a Risk Assessment and the EPA’s claim to the contrary is false and taints the permit process.

The USEPA document entitled “Evoqua Air Emissions and Risk Assessment” found at <https://www.epa.gov/az/evoqua-air-emissions-and-risk-assessment> and linked from <https://www.epa.gov/az/evoqua> which was posted in the fall of 2016 states:

“At EPA’s request, and as part of the permit process, Evoqua completed a [Human Health and Ecological Risk Assessment](#) in July 2007.”

There is no link to any USEPA Risk Assessment as none was performed. This false claim by USEPA, combined with countless other false and misleading claims made during the permit process and the facility’s regulatory history, once again tainted and made a mockery of the public’s right to an informed and impartial permit process.

XIV. USEPA failed to investigate tribal members’ testimony and information about possible elevated cancer rates in neighborhoods near the facility:

Over the last 15 years at least, tribal members repeatedly shared with USEPA their concerns and information about possible elevated rates of cancer among tribal members living in proximity to the facility. EPA never followed up or investigated this important information that is relevant to a permit decision.

XV. Inadequate Tribal Consultation with Colorado River Indian Tribes:

According to the USEPA’s Revised “Statement of Basis,” in August of 2014 EPA initiated formal Tribal consultation with respect to the RCRA Hazardous Waste Permit Application submitted to EPA for the Facility, which is operated by Evoqua on the Tribe’s land.”

The EPA should have initiated formal Tribal consultation with the CRIT before allowing the facility to operate on so-called interim status for decades, not waiting for over twenty years to commence the required consultation. This inexcusable delay, combined with many instances of false and misleading information being given to the CRIT by EPA and the withholding of key information from the CRIT, demonstrates bias and makes a mockery of meaningful and adequate tribal consultation.

Meaningful and adequate tribal consultation must be based on facts, not fiction. Unfortunately as these comments, and the administrative record, demonstrate, USEPA has continuously provided false, incomplete and misleading “information” to the Colorado River Indian Tribes including tribal government and other tribal members.

XVI. USEPA violated the National Historic Preservation Act and made a mockery of the NHPA process and federal trust responsibility:

The National Historic Preservation Act and its implementing regulations require USEPA, before issuing a permit, to adopt, when feasible, measures to mitigate potential adverse effects of the permitted activity on properties listed or eligible for listing in the National Register of Historic Places.

Despite the fact that the RCRA permit process began in 1995, USEPA allowed the facility to operate without a NHPA decision for two decades. EPA ignored the NHPA requirement for years and allowed the process to drag on for years despite being fully informed by tribal members since the mid-1990's about negative impacts on sacred and culturally significant sites.

The USEPA then conducted an NHPA Section 106 review of the potential impacts of issuance of a RCRA hazardous waste permit to the facility, and in June 2012 made a final determination that “no adverse effect” on historic properties would occur if a permit was issued. EPA made this determination despite extensive comments from the CRIT government including Chairman Daniel Eddy Jr., Mohave Elders of the Colorado River Indian Tribes and other tribal members that clearly and unequivocally documented that there would in fact be profound adverse effects – and despite EPA's acknowledging there were locations of traditional religious and cultural importance.

On September 10, 2003, Colorado River Indian Tribes Chairman Daniel Eddy Jr. wrote an official letter to USEPA to Karen Scheuermann, USEPA Region 9, regarding “Designated Area of Potential Effects for US Filter/Westates, Parker, AZ”.

The letter from Chairman Eddy, Jr. was an official communication from the tribal government and was extremely clear and specific in its view of the potential effects of this facility. We attach and incorporate this letter into our comments.

Chairman Eddy Jr.'s letter states in part:

“The cultural landscape in question comprises a significant core portion of traditional aboriginal territory for riverine Yuman and Numic speaking American Indian Groups. This area is very significant to these native peoples in cultural, historical, ecological, religious and cosmological terms. Review of past archaeology interpretations, elders recommendations from previous projects and oral stories from tribal members, helped institute the difficult decision to set boundaries on lands that hold traditional beliefs concerning tribal origins, cultural history, ceremonial activities and sacred sites. *While the US Filter/Westates facility was sited on tribal land in 1992, in a area set apart of industrial activity, it impacts other important aspects of a cultural landscape. The cultural landscape is not limited to air, water, and land.* The cultural importance of these environmental media must be taken into consideration in addition to cultural and spiritual effects... *(Emphasis added)*

According to the November 2016 “Revised Statement of Basis – Proposed Permit for Storage and Processing of RCRA-Regulated Hazardous Wastes,” USEPA determined there would allegedly be “no adverse effect” despite the fact that:

“EPA identified two sites within a one mile radius of the Facility (area of Potential Effects)...as potential historic properties under the NHPA. One is the Parker cemetery, a location where Navajo Code Talkers are interred. The second site that EPA considered consisted of all areas within the APE from where Black Peak, a mountain sacred to the members of the Native American community in the area, approximately 3 miles away, may be viewed or from where prayers might be directed. *EPA considered both locations to be areas of traditional religious and cultural importance.*”(Revised Statement of Basis pages 5-6) (*Emphasis added*).

But in a desperate and factually bankrupt attempt to justify the permit issuance that EPA has been trying to do for decades, and despite EPA acknowledging that areas of traditional religious and cultural importance could be impacted, USEPA justified their NHPA decision as follows:

“*EPA identified potential effects of Facility operations on historic properties, including visual and auditory impacts, and impacts stemming from the presence of chemicals at the Facility and in the Facility’s emissions.* However, because the Facility could continue treating non-hazardous spent carbon, whether or not a hazardous waste management permit is issued, EPA concluded that the permit decision will not significantly affect Facility operations. Thus, EPA has determined that issuing a permit solely for the management of RCRA hazardous waste at the Facility will have no adverse effect on nearby historic properties.” (Revised Statement of Basis, page 6) (*Emphasis added*)

Despite EPA identifying potential effects on historic properties of traditional religious and cultural importance including “impacts stemming from the presence of chemicals at the Facility and in the Facility’s emissions,” the EPA then totally ignored the impact of the presence and emissions of chemicals that they themselves acknowledged to exist. EPA’s rationale that the impact of the Facility on these sites would be the same even if hazardous wastes were not treated is without merit, as there would not be the presence of the wide range and potency of chemicals at the Facility or in the emissions if RCRA hazardous wastes were not treated. Emissions from treatment of hazardous and non-hazardous materials are not the same.

The EPA thus clearly ignored the specific comments and testimony from CRIT Chairman Daniel Eddy Jr. and the Mohave people about the impacts of toxic emissions on spiritual well-being, spirit pathways during cremations, prayers directed to sacred mountains, and the cultural landscape near the toxic waste facility.

The USEPA apparently believes it - and not the Mohave people, the Mohave Elders, and tribal leadership - is the authority on the Mohave religion and Mohave spiritual and cultural beliefs and practices. USEPA thus illegally and unethically violated the purpose and intent National Historic

Preservation Act and permits the desecration of profoundly sacred and culturally significant sites. This is environmental racism, pure and simple – and a violation of civil rights, environmental justice, and laws protecting sacred sites and religious freedom.

XVII. USEPA repeatedly failed to disclose that a wide range of federal agencies and federal facilities sends hazardous waste to the Evoqua facility at CRIT:

The USEPA September and November 2016 documents entitled “Fact Sheet: Proposed Permit for the Evoqua Water Technologies LLC Facility Near Parker, Arizona” state that “Annually, the Evoqua facility receives over 5,000 tons of spent carbon from 30-35 states across the United States.”

These “fact sheets” curiously and improperly fail to mention that the US government itself, including many federal agencies and federal facilities themselves send hazardous waste to the Evoqua facility.

According to manifests provided to Greenaction by the USEPA, federal agencies and federal facilities that sent hazardous wastes to the Evoqua facility include:

- Tooele Army Depot (Utah)
- US Department of Energy (Washington)
- US Army Garrison (Alabama)
- US Air Force (California)
- Rocky Mountain Arsenal (Colorado)
- US Army Corps of Engineers
- Jet Propulsion Laboratory/NASA (California)

During Greenaction’s many discussions with tribal council members over the years, not one council member told us that USEPA ever informed them that the federal government itself sent toxic wastes to the facility. All the tribal council members that Greenaction has spoken with stated that they had never been provided copies of hazardous waste manifests by USEPA.

Not only does USEPA’s failure to properly disclose this information taint the permit and tribal consultation processes, but it also may indicate why USEPA has been so biased in the permit process, why USEPA allowed the permit process to continue for decades, and why they now propose issuing a RCRA permit.

XVIII. Permit process violates, and permit issuance would violate, Executive Order 12898 and Title VI of the United States Civil Rights Act:

USEPA is in clear violation of Executive Order 12898 due to its improper actions and decisions in its regulatory and permitting role for the Evoqua facility. EPA has failed to properly address the disproportionately high and adverse human health and environmental effects of their actions

on the people of the Colorado River Indian Tribes and adjacent indigenous peoples. EPA's faulty regulatory and permitting role has increased the negative impacts, and issuance of a permit would also violate the Executive Order which states:

“Executive Order (E.O.) 12898 - Federal Actions to Address Environmental Justice in Minority Populations and Low-Income Populations - was issued by President William J. Clinton in 1994. Its purpose is to focus federal attention on the environmental and human health effects of federal actions on minority and low-income populations with the goal of achieving environmental protection for all communities.

The E.O. directs federal agencies to identify and address the disproportionately high and adverse human health or environmental effects of their actions on minority and low-income populations, to the greatest extent practicable and permitted by law. The order also directs each agency to develop a strategy for implementing environmental justice. The order is also intended to promote nondiscrimination in federal programs that affect human health and the environment, as well as provide minority and low-income communities access to public information and public participation.”

<https://www.epa.gov/laws-regulations/summary-executive-order-12898-federal-actions-address-environmental-justice>

USEPA is a recipient of federal funding and is thus subject to Title VI of the US Civil Rights Act and its implementing regulations. Title VI prohibits recipients of federal funding from taking actions that have a disparate and discriminatory effect on people based on race, color or national origin. EPA's actions, past, present and proposed, clearly have a prohibited impact.

Conclusion:

In conclusion, USEPA must deny the permit for the Evoqua facility or shut it down pending the conducting and conclusions of an unbiased, fact-based permit process that complies with all relevant laws, regulations and policies.

For health and justice,



Bradley Angel
Executive Director, Greenaction for Health and Environmental Justice



**UNITED STATES ENVIRONMENTAL PROTECTION AGENCY
REGION IX
75 Hawthorne Street
San Francisco, CA 94105**

July 30, 2009

SUBJECT: Key US EPA Messages for the Colorado River Indian Tribes (CRIT)
August 3, 2009 Council Meeting Regarding the Siemens Water
Technologies/CRIT Final Permit Application.

Status of Permit Application:

- 1) The US EPA is responsible under the Resource Conservation and Recovery Act (RCRA) for permitting carbon regeneration facilities that process RCRA regulated hazardous wastes on tribal lands;
- 2) The Siemens carbon regeneration facility is currently legally operating under “interim status” conditions as prescribed by RCRA. That interim status to continue regulated activities was triggered by the formal submittal of an initial Permit Application, Part A that was endorsed by the CRIT;
- 3) The US EPA remains respectful of the sovereignty of the CRIT and will continue to work closely with the CRIT Office of the Attorney General and Environmental Protection Office to address CRIT’s issues and concerns;
- 4) As owners of the land upon which Siemens is operating CRIT, along with Siemens, are held to be co-applicants under RCRA, responsible for placement, justification and merits of the project. The US EPA remains strictly neutral on such business concerns;
- 5) To date US EPA has not received a complete Final Part B Application from Siemens and the CRIT. It is a legal requirement that US EPA receive a complete application before it can act upon it. (CRIT signature on the Application is necessary for completeness);
- 6) At the May 18, 2009 CRIT Council Meeting, US EPA requested a decision by June 12, 2009, from the Council on whether it intended to sign the Final Part B Application;
- 7) To date CRIT has neither signed the Application nor in any way indicated its intention to do so. US EPA currently considers the Application incomplete;

- 8) Therefore, the US EPA considers it no longer appropriate for Siemens to continue operating under interim status conditions without a targeted date for resolution of the pending application status;
- 9) Accordingly, if US EPA does not receive a complete Final Part B Application from Siemens and the CRIT by September 1, 2009, it plans to issue a formal Notice of Deficiency (NOD) of the Application and proceed to denial of a final operating permit;
- 10) The CRIT will have the opportunity to formally comment upon and challenge any US EPA proposed or final permit decision concerning the Siemens facility; and
- 11) If US EPA does ultimately decide to deny the Permit Application it will assure and manage closure of the regulated units that process RCRA hazardous waste in such a manner that will allow Siemens to continue processing non-RCRA wastes. (Currently less than 20 percent of their input is RCRA regulated.).

Additional Issues and Messages:

- 1) Under RCRA US EPA may deny a permit for only three reasons:
 - a. An incomplete permit application,
 - b. Inability of US EPA to write a permit that is protective of human health and the environment, and
 - c. The facility construction is so deficient that it cannot meet US EPA permit conditions;
- 2) Though supplemental data and information will likely be further required to develop a permit, the current Final Part B Application appears technically sufficient to begin development of a final enforceable permit if the Application is made legally complete with the CRIT's signature;
- 3) The enhanced protections requested by the CRIT and negotiated by US EPA for this facility have been implemented, but are only voluntary until prescribed in a final permit. US EPA cannot assure compliance with non-permitted non-enforceable voluntary operating conditions;
- 4) In keeping with CRIT's expressed interest in enhancing human health and environmental protections at the facility beyond minimum requirements, US EPA directed Siemens to comply with appropriate portions of the Maximum Achievable Combustion Technology (MACT) rules of the Clean Air Act, to conduct a "trial burn" to help establish more protective operating conditions

and to create sufficient data for a robust Human Health and Ecological Risk Assessment (HHREA);

- 5) The CRIT Council requested that US EPA make a presentation of their analysis of the HHERA to help it in making a final signature decision. We met that request on May 18, 2009. Highlights of that analysis and presentation are as follows:
 - a. The “trial burn” identified and measured the concentration of chemicals that are released from the facility,
 - b. The primary potential pathway of concern for pollution from this facility is through the air,
 - c. The US EPA used local weather and census data along with computer based tools to model how and where those chemicals would distribute in the environment (the land, air and water) and who would be potentially impacted,
 - d. The US EPA used national data to analyze toxic effects of the released chemicals in the local environment,
 - e. The US EPA’s analysis of the HHERA indicated that the CRIT and Parker would not expect any adverse health impacts from normal operations at the facility if the tested operating conditions were incorporated in a Final Permit,
 - f. Even if permitted, Siemens will under normal operating conditions emit some regulated pollutants to the atmosphere. The HHERA and permit conditions however, will assure that the emissions remain health protective, and
 - g. Of the five similar carbon regeneration facilities in the nation processing regulated hazardous wastes, Siemens has the most stringent and protective air pollution control equipment, and is currently meeting the highest US EPA air protection standards.

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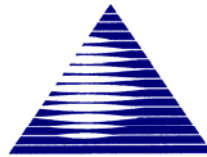
CARBON REACTIVATION FURNACE RF-2 PERFORMANCE DEMONSTRATION TEST REPORT

PREPARED FOR:

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**Revision: 0
June 30, 2006
Focus Project No. 010111**

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- C. Corrective Action Requests
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- F. Analytical Result Summaries
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- H. Data Validation Report

VOLUME II (on CD)

- I. Airtech, Inc. Stack Sampling Report (Includes particulate matter, M0040 Bag analytical data, and THC CEMS data)
- J. ESS, Spiking Report and Certificate of Composition for Spiking Materials
- K. CEMS Performance Specification Test Report
- L. Process Instrument Calibration Data

VOLUME III (on CD)

Feed and Process Data Packages

	File Name
A. Feed Ultimate Analysis	H6D040101 Carbon Ultimate.pdf
B. Feed Total Chlorine	H6D040102 Carbon Total Chlorine.pdf
C. Feed and Process Volatiles	H6D030205 Carbon & Process VOC.pdf
D. Feed and Process Semivolatiles	H6D030246 Carbon & Process SVOC.pdf
E. Feed and Process Metals	H6D040213 Carbon & Process Metals.pdf

Stack Gas Data Packages

	File Name
A. M5 Particle Size Distribution	142541 M5 PSD.pdf
B. M0030 VOST and First VOST Audit	H6D030169 M0030 VOST & 1 st VOST Audit.pdf
C. M0040 Total Volatile Organic Condensate	H6D030177 M0040 CON.pdf
D. M0061 Hexavalent Chromium	H6D030194 M0061 Hex Cr.pdf
E. M29 Metals	H6D030224 M29 Metals.pdf
F. M0010 Total Semivolatile and Nonvolatile Organics	H6D030231 M0010 TCO Grav.pdf
G. M0023A Dioxin and Furans	H6D030236 M0023A D-F.pdf
H. M0010 PCBs and PAHs	H6D030241 M0010 PCB PAH.pdf
I. M0010 SVOCs and OCPs	H6D030245 M0010 SVOC OCP.pdf
J. M26A Chlorine and Hydrogen Chloride	H6D040103 M26A HCl Cl.pdf
K. Second VOST Audit	H6D120117 2 nd VOST Audit.pdf

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ACRONYMS AND ABBREVIATIONS

acfm	Actual cubic feet per minute
APC	Air pollution control
ASTM	American Society for Testing and Materials
AWFCO	Automatic waste feed cutoff
B.P.	Boiling point
Btu	British thermal unit
CAR	Corrective Action Request
CAA	Clean Air Act
CARB	California Air Resources Board
CEM or CEMS	Continuous emission monitor or Continuous emission monitoring system
CFR	Code of Federal Regulations
cm	Centimeters
CO	Carbon monoxide
COPCs	Compounds of potential concern
CRIT	Colorado River Indian Tribes
cu. ft.	Cubic foot
CVAAS	Cold vapor atomic absorption spectroscopy
DC	Direct current
DOT	Department of Transportation
DQO	Data Quality Objective
DRE	Destruction and removal efficiency
dscf	Dry standard cubic foot
dscfm	Dry standard cubic feet per minute
dscm	Dry standard cubic meters
EPA	United States Environmental Protection Agency
FID	Flame ionization detector
ft	Feet
g	Gram
GC/FID	Gas chromatography/flame ionization detector
GC/MS	Gas chromatography/mass spectrometry
gpm	U.S. Gallons per minute
gr	Grain (equals 1/7000 pound)
GRAV	Gravimetric
HAP	Hazardous air pollutant
HCl	Hydrogen chloride
HPLC	High performance liquid chromatography
hr	Hour
HRGC/HRMS	High resolution gas chromatography/high resolution mass spectrometry
HWC MACT	Hazardous Waste Combustor Maximum Achievable Control Technology regulations
ICP	Inductively coupled plasma spectroscopy
in	Inch
in w.c.	Inches of water column (pressure measurement)
kg	Kilogram
L	Liter
lb	Pound
lpm	Liters per minute
m	Meter
mg	Milligram
ml	Milliliter
MTEC	Maximum theoretical emission concentration
NDIR	Non-dispersive infrared

ng	Nanogram
NVOC	Nonvolatile organic compound
P&ID	Piping and instrumentation diagram
PAH	Polyaromatic hydrocarbon
PCB	Polychlorinated biphenyl
PCDD/PCDF	Polychlorinated dibenzo-p-dioxins and polychlorinated dibenzo furans
PDT	Performance Demonstration Test
PDTP	Performance Demonstration Test Plan
PFD	Process flow diagram
PIC	Product of incomplete combustion
PLC	Programmable logic controller
POHC	Principal organic hazardous constituent
POTW	Publicly owned treatment works
ppm	Parts per million
ppmv	Parts per million by volume
ppmvd	Parts per million by volume, dry basis
psig	Pounds per square inch, gauge
QA	Quality assurance
QAPP	Quality Assurance Project Plan
QC	Quality control
RCRA	Resource Conservation and Recovery Act
RF	Reactivation Furnace
s	Second
scfm	Standard cubic feet per minute
SOP	Standard operating procedure
sq. ft.	Square feet
SQL	Sample quantitation limit
SVOC	Semivolatile organic compound
TCDD	Tetrachloro dibenzo-p-dioxin
TCO	Total chromatographable organics
TEQ	Toxicity equivalent (related to 2,3,7,8-TCDD)
THC	Total hydrocarbons
TIC	Tentatively identified compound
TOE	Total organic emissions
TSCA	Toxic Substances Control Act
ug	Microgram
VOA	Volatile organic analysis
VOC	Volatile organic compound
VOST	Volatile organic sampling train
WESP	Wet electrostatic precipitator
w.c.	Water column
XAD	Brand name for Amberlite XAD-2 adsorbent resin

1.0 EXECUTIVE SUMMARY

A Performance Demonstration Test (PDT) of the Carbon Reactivation Furnace RF-2 at the Siemens Water Technologies Corp. (formerly known as U.S. Filter Westates) Facility located in the Colorado River Indian Tribes (CRIT) Industrial Park near Parker, Arizona was conducted in March 2006.

The facility treats spent activated carbon that has been used by industry, state and federal government agencies, and municipalities for the removal of organic compounds from liquid and vapor phase process waste streams. Once the carbon has been used and is spent, it must be either disposed of or reactivated at a facility such as Siemens Water Technologies Corp.. A Carbon Reactivation Furnace (designated as RF-2) is used by Siemens Water Technologies Corp. to reactivate the spent carbon. Some of the carbon received at the Parker facility is designated as a hazardous waste under the Resource Conservation and Recovery Act (RCRA) regulations. Much of the carbon received at the facility is not a RCRA hazardous waste, as it is either not a characteristic or listed waste. The RF is not a hazardous waste incinerator. "Hazardous waste incinerator" is defined in 40 CFR Part 63, Subpart EEE as a "device defined as an incinerator in § 260.10 of this chapter and that burns hazardous waste at any time." (40 CFR 63.1201). "Incinerator" is defined in 40 CFR 260.10 as "any enclosed device that: (1) Uses controlled flame combustion and neither meets the criteria for classification as a boiler, sludge dryer or carbon regeneration unit, nor is listed as an industrial furnace; or (2) Meets the definition of infrared incinerator or plasma arc incinerator. (emphasis supplied)" The RF-2 unit does not qualify as an incinerator and instead is designated by Subpart X of the RCRA regulations as a Miscellaneous Unit. According to 40 CFR 264.601 of the Subpart X regulations, permit terms and provisions for a Miscellaneous Unit must include appropriate requirements of 40 CFR Subparts I through O and Subparts AA through CC, 40 CFR 270, 40 CFR 63 Subpart EEE, and 40 CFR 146.

Based on 40 CFR 264.601, Siemens Water Technologies Corp. tested the RF-2 unit to demonstrate performance and to establish operating parameter limits in accordance with the standards of 40 CFR 63 Subpart EEE. The emission standards of 40 CFR 63 Subpart EEE are more stringent than the RCRA hazardous waste incinerator emission standards of 40 CFR 264 Subpart O. The regulations at 40 CFR 63 Subpart EEE are often referred to as the Hazardous Waste Combustor Maximum Achievable Control Technology (HWC MACT) standards. This terminology will be used in this document.

The testing was conducted in accordance with the requirements of the HWC MACT standards and the approved PDT plan. The testing consisted of a Performance Demonstration Test of the RF-2 unit and a Continuous Emissions Monitoring Systems (CEMS) test. The CEMS testing was conducted just prior to the RF-2 PDT. The formal PDT was conducted on March 27 through March 30, 2006.

The carbon reactivation process consists of a multiple hearth reactivation furnace, a natural gas fired afterburner used to destroy organic contaminants released from the carbon, a wet quench, venturi scrubber, packed bed scrubber, and wet electrostatic precipitator.

The purpose of the PDT was to:

1. Demonstrate Compliance with Applicable USEPA Regulatory Performance Standards (Based on HWC MACT Standards for Existing Hazardous Waste Incinerators):
 - Demonstrate a DRE of greater than or equal to 99.99% for the selected principal organic hazardous constituents (POHCs) chlorobenzene and tetrachloroethene.
 - Demonstrate stack gas carbon monoxide concentration less than or equal to 100 ppmv, dry basis, corrected to 7% oxygen.
 - Demonstrate stack gas hydrocarbon concentration of less than or equal to 10 ppmv, as propane, dry basis, corrected to 7% oxygen.
 - Demonstrate a stack gas particulate concentration less than or equal to 34 mg/dscm (0.015 gr/dscf) corrected to 7% oxygen.
 - Demonstrate that the stack gas concentration of hydrogen chloride (HCl) and chlorine (Cl₂) are no greater than 77 ppmv, dry basis, corrected to 7% oxygen, expressed as HCl equivalents.
 - Demonstrate that the stack gas mercury concentration is less than or equal to 130 µg/dscm, corrected to 7% oxygen.
 - Demonstrate that the stack gas concentration of semivolatile metals (cadmium and lead, combined) is less than or equal to 240 µg/dscm, corrected to 7% oxygen.
 - Demonstrate that the stack gas concentration of low volatility metals (arsenic, beryllium, and chromium, combined) is less than or equal to 97 µg/dscm, corrected to 7% oxygen.
 - Demonstrate that the stack gas concentration of dioxins and furans does not exceed 0.40 ng/dscm, corrected to 7% oxygen, expressed as toxic equivalents of 2,3,7,8-TCDD (TEQ). This is the applicable standard since the gas temperature entering the first particulate matter control device is less than 400°F.
2. Establish Permit Operating Limits
 - Demonstrate maximum feed rate for spent activated carbon.
 - Demonstrate minimum afterburner gas temperature
 - Demonstrate maximum combustion gas velocity (or a suitable surrogate indicator)
 - Demonstrate maximum total chlorine/chloride feed rate
 - Establish a Maximum Theoretical Emission Concentration (MTEC) limit for mercury
 - Demonstrate system removal efficiency (SRE) for semivolatile and low volatility metals so feed rate limits can be developed by extrapolation from test results.
 - Establish appropriate operating limits for the air pollution control system components.

3. Gather Information for Use in a Site-Specific Risk Assessment
 - Measure emissions of metals, including hexavalent chromium
 - Measure emissions of specific volatile and semivolatile products of incomplete combustion (PICs)
 - Measure emissions of polychlorinated dibenzo-p-dioxins and polychlorinated dibenzofurans (PCDD/PCDF)
 - Measure emissions of polychlorinated biphenyls (PCBs)
 - Measure emissions of specific organochlorine pesticides
 - Measure emissions of total volatile, semivolatile, and nonvolatile organics
 - Determine the stack gas particle size distribution.

A summary of the PDT performance and emission results is presented in Table 1-1. A summary of the process operating conditions for each run is presented in Table 1-2.

The PDT results indicate that the RF-2 unit meets the applicable performance requirements. Specific conclusions drawn from the PDT are as follows:

- The RF-2 system operated reliably during each PDT run, and was able to maintain operating conditions which were consistent with the target values stated in the PDT Plan. The test results are suitable for establishing operating parameter limits.
- DRE requirements of 99.99% or greater were met for both POHCs (monochlorobenzene and tetrachloroethene). Minimum temperature limits and maximum flue gas flow rate limits can be appropriately established from the test results.
- PCDD/PCDF emission standards were met.
- Particulate matter emission standards were met.
- Metal emission standards were met for mercury, semivolatile metals, and low volatility metals. Maximum metal feed rates can be reliably determined using the test results.
- Stack gas CO and THC concentration standards were met in all test runs.
- Stack gas HCl/Cl₂ emission requirements were met. Maximum total chlorine and chloride feed rate limits can be appropriately established from the test results.
- Emissions data to support the estimates of risk in a site-specific multi-pathway human health and ecological risk assessment were gathered successfully.

Continued operation of the Siemens Water Technologies Corp. Carbon Reactivation Furnace RF-2 under the conditions established by the PDT will result in effective destruction of organic compounds, and control of emissions in accordance with the applicable performance requirements.

2.0 TEST PROGRAM SUMMARY

2.1 SUMMARY OF TEST PLAN AND OBJECTIVES

In order to accomplish the PDT objectives, (i.e., demonstrating that the unit will meet all applicable environmental performance standards) a single test condition representing “worst case” operations of minimum temperature, maximum combustion gas velocity (minimum residence time), and maximum spent activated carbon feed rate was performed. The test consisted of three replicate sampling runs.

A summary description of the planned testing conditions, analytical parameters, and sampling methods follows:

Test Condition 1 (“Worst-Case” Operations)

Sampling and monitoring protocols that were planned for the performance test are summarized as follows:

- Spent Activated Carbon Feed - total chlorine/chloride, elemental (C, H, N, O, S, moisture), volatile organics, semivolatile organics, and total metals (Al, Sb, As, Ba, Be, Cd, Cr, Co, Cu, Pb, Hg, Ni, Se, Ag, Tl, V, Zn)
- Makeup Water - volatile organics, semivolatile organics, and total metals (Al, Sb, As, Ba, Be, Cd, Cr, Co, Cu, Pb, Hg, Ni, Se, Ag, Tl, V, Zn)
- Caustic feed to APC - volatile organics, semivolatile organics, and total metals (Al, Sb, As, Ba, Be, Cd, Cr, Cu, Co, Pb, Hg, Ag, Tl, Se, Ni, V, Zn)
- Scrubber Blowdown - volatile organics, semivolatile organics, and total metals (Al, Sb, As, Ba, Be, Cd, Cr, Co, Cu, Pb, Hg, Ni, Se, Ag, Tl, V, Zn)
- Wastewater Discharge to POTW - volatile organics, semivolatile organics, and total metals (Al, Sb, As, Ba, Be, Cd, Cr, Co, Cu, Pb, Hg, Ni, Se, Ag, Tl, V, Zn)
- Stack gas particulate, HCl, and Cl₂ using EPA Method 26A
- Stack gas target volatile organics using VOST, SW-846 Method 0030
- Stack gas target semivolatile organics and organochlorine pesticides using SW-846 Method 0010
- Stack gas PAHs and PCBs using a separate SW-846 Method 0010 sampling train
- Stack gas PCDD/PCDF using SW-846 Method 0023A
- Stack gas total volatile organics using SW-846 Method 0040
- Stack gas total semivolatile and nonvolatile organics using SW-846 Method 0010
- Stack gas metals (Al, Sb, As, Ba, Be, Cd, total Cr, Co, Cu, Pb, Hg, Ni, Se, Ag, Tl, V, and Zn) using EPA Method 29
- Stack gas hexavalent chromium using SW-846 Method 0061
- Stack gas particle size distribution using a cascade impactor

- Stack gas CO and O₂ by permanently installed CEM according to the protocols in the Appendix to 40 CFR 63, Subpart EEE; Performance Specification 4B of 40 CFR 60, Appendix B.
- Stack gas total hydrocarbons (as propane) by temporary CEM according to EPA Method 25A and the protocols in the Appendix to 40 CFR 63, Subpart EEE.

Tables 2-1 and 2-2 present the planned PDT sampling and analytical protocol in greater detail. Figure 2-1 shows the location of sampling points in the RF-2 system.

2.2 DEVELOPMENT OF PERMIT LIMITS

Siemens Water Technologies Corp. is required to establish operating limits (applicable whenever hazardous waste is in the combustion chamber) in its permit to ensure that the RF-2 system complies with the applicable USEPA environmental performance standards at all times. Under the HWC MACT, the regulations establish a comprehensive list of regulated parameters at 40 CFR 63.1209 (j) through (p) which are used to ensure continuing regulatory compliance.

Considering the configuration of the RF-2 system and the characteristics of the spent activated carbon to be fed, Siemens Water Technologies Corp. anticipated establishing process operational limits on the following parameters, and operated the system accordingly during the PDT:

- Minimum afterburner gas temperature
- Maximum spent activated carbon feed rate
- Maximum total chlorine and chloride feed rate
- Maximum feed rate of mercury (based on MTEC)
- Maximum feed rate of semivolatile metals (total combined lead and cadmium)
- Maximum feed rate of low volatility metals (total combined arsenic, beryllium, and chromium)
- Minimum venturi scrubber pressure differential
- Minimum quench/venturi scrubber total liquid flow rate
- Minimum packed bed scrubber pH
- Minimum packed bed scrubber pressure differential
- Minimum packed bed scrubber liquid flow rate
- Minimum scrubber blowdown flow rate
- Minimum WESP secondary voltage
- Maximum stack gas flow rate (indicator of combustion gas velocity).

These operating limits have been established as described in the HWC MACT regulations and in the approved Performance Demonstration Test Plan, and are more fully described in Section 7.0 of this test report.

As part of EPA's approval of the PDT Plan, Siemens Water Technologies Corp. was also required to establish both a minimum and maximum temperature limit for Hearth #5 of the reactivation furnace. Since both a minimum and maximum temperature could not be demonstrated in the single test condition approved for the test, Siemens Water Technologies Corp. operated Hearth #5 at a maximum temperature during the PDT and will conduct a separate minimum temperature test outside of the formal PDT period.

2.3 TEST IMPLEMENTATION SUMMARY

Overall, the PDT was executed in substantial conformance with the approved protocols contained in the PDT Plan and Quality Assurance Project Plan (QAPP). This section presents an account of the PDT implementation.

The Performance Demonstration Test of the Siemens Water Technologies Corp. carbon reactivation furnace RF-2 located in the Colorado River Indian Tribes Industrial Park near Parker, Arizona was conducted during the week of March 27 - 31, 2006. Actual emissions sampling was conducted on March 28 through March 30. All planned testing for the PDT was completed.

All process operating conditions were within the operating envelope defined by the specifications provided in the PDT Plan. All sampling and analysis was performed as described in the PDT Plan and QAPP, with minor deviations as described in Section 2.3.2 below.

The PDT was conducted in compliance with the PDT Plan approved by the US Environmental Protection Agency (EPA) and CRIT. The PDT program was conducted under the overall direction of Siemens Water Technologies Corp. personnel. Mr. Monte McCue was the overall CPT Manager for Siemens Water Technologies Corp. Mr. Willard (Drew) Bolyard of Siemens Water Technologies Corp. oversaw plant personnel and operations during the PDT. Ms. Mary Blevins, Ms. Stacy Braye, Mr. Steven Arman, Mr. Robert Fitzgerald, Mr. Michael Svizzero, and Ms. Karen Scheuerman of USEPA were on-site to observe portions of the PDT. Mr. Hector Duran observed the PDT as a representative of CRIT. Mr. Marty Jones and Mr. Chase McLaughlin of Arcadis also observed the PDT as consultants to CRIT. Process operations were conducted by Siemens Water Technologies Corp. personnel, with the assistance of Mr. Karl Monninger of Chavond Barry Engineering. Mr. Anthony Eicher, of Focus Environmental, Inc. (Focus), coordinated and oversaw all technical aspects of the test program, and acted as the PDT

Manager. Mr. Eicher was also responsible for the preparation of this report, and provided overall QA/QC for the project. Ms. Teresa White, of Focus, acted as the on-site sample coordinator for the test. She also served as the Quality Assurance Officer for the PDT analytical activities, and performed data validation of the process sample and emissions results. Process samples were collected by Focus and Siemens Water Technologies Corp. personnel, under the direction of Focus. A number of process samples were provided as split samples to Ms. Kathy Baylor of EPA, who was on site to coordinate the collection and packaging of the split samples. All stack gas samples were collected by Airtech Environmental Services, Inc. (Airtech), under the direction of Mr. Pat Clark. Waste feed spiking services were provided by Engineered Spiking Solutions, Inc. (ESS), under the direction of Dr. William Schofield, with field spiking services provided by Mr. Scott Neal. PDT sample analyses were performed by the following laboratories:

1. Airtech conducted the analysis of stack gas particulate matter samples and provided on-site analytical services for the determination of total volatile organics. Airtech also operated a temporary CEM systems for THC during the PDT.
2. Severn-Trent Laboratories of Knoxville, Tennessee, under the direction of Dr. William Anderson, performed the analyses for all process and stack gas samples, with the exception of the stack gas particulate matter and particle size distribution.
3. MVA, Inc. of Atlanta, Georgia, conducted the stack gas particle size determination, under sub-contract to Severn-Trent Laboratories.

2.3.1 Test Run Chronology

The test team arrived on-site and set up equipment for the test on March 27, 2006. Coordination meetings were held between the test team members to ensure that all were familiar with the test protocols and that operators understood the desired test conditions.

During the initial meetings with the test team, a number of minor modifications to the test plan were discussed based on comments received from EPA after approval of the plan, and based on input from the other test team members based on observations during preliminary testing and subsequent sample analysis. The majority of these items have been documented through the use of Corrective Action Requests (CARs) as provided for in the approved Quality Assurance Project Plan (QAPP) and are discussed in detail in later section of this report. CARs were reviewed and approved by appropriate members of the team during the course of the PDT.

The test team arrived on site at or before 07:00 on March 28, 2006. The RF-2 system was near the target operating conditions when the team arrived. POHC spiking was started at 07:30 and spiking of the organic surrogate mixture and metals started at 07:50. The entire RF-2 unit experienced a shutdown at

07:56 due to over-amperage of the ID fan. All spiking was stopped immediately. The plant recovered quickly from the shutdown and spiking operations were re-started at 08:59. Preliminary stack gas flow traverses were conducted and final preparations were made for the beginning of testing.

PDT Run 1 was started at 12:10 on March 28, 2006.

PDT Run 1 was completed at 16:44 on March 28, 2006, without interruption. All stack gas sampling trains were successfully leak checked prior to the start of sampling, during port changes, and upon completion of sampling and were recovered once the run was complete.

On March 29, 2006, the testing crew arrived on-site at 08:00 and began setting up for PDT Run 2. Spiking operations were started at 08:58. Plant personnel made a number of adjustments to the furnace in order to maintain the stack gas flow rate near the desired conditions.

PDT Run 2 was started at 11:15 on March 29, 2006.

As the Method 0023A sampling train was being moved to the last traverse point in the first half of the run, the glass probe liner broke. The sampling team and regulatory observers noticed the break immediately when it occurred, and the sampling team shut down the sample pump. Since it was known when the break occurred and sampling was immediately stopped, it was decided to recover both parts of the broken probe liner, replace the probe, and continue sampling. All parties were aware of the situation and approved of the action taken.

PDT Run 2 was completed at 17:00 on March 29, 2006, without further sampling difficulties. All stack gas sampling trains were successfully leak checked prior to the start of sampling, during port changes, and upon completion of sampling and were recovered once the run was complete. There were no process interruptions during the run.

On March 30, 2006, the testing team arrived at or before 08:00 and began setting up for PDT Run 3. All process conditions were at their target values, and spiking started at 08:50.

At 08:58 a weld on the nipple attached to the carbon feed chute used for spiking material injection was noticed to be cracked. Spiking was immediately stopped and the weld was repaired. Spiking resumed at 10:13 on March 30, 2006.

PDT Run 3 was started at 11:50 on March 30, 2006.

All sampling activities were placed on hold at 12:39 when it was noted that the organic surrogate mixture was not flowing correctly through the spiking system. The other spiking systems continued to operate and process conditions were maintained while the problem with the organic surrogate mixture spiking system was identified and corrected.

Organic surrogate spiking was resumed at 14:43 and all sampling was resumed at 15:30 on March 30, 2006.

PDT Run 3 was completed at 19:16 on March 30, 2006. As the PSD sampling train was being recovered it was noted that the filter had gotten wet, thus potentially compromising the sample. Another PSD sample was collected as quickly as possible and finished at 19:59. Since all other samples had finished at 19:16, all parties involved in testing decided to designate 19:16 as the official run completion time. All stack gas sampling trains were successfully leak checked prior to the start of sampling, during port changes, and upon completion of sampling and were recovered once the run was complete. There were no process interruptions during the run.

On March 31, 2006 the test team dismantled all testing and spiking equipment, packaged samples for shipment to the laboratory, and departed the site. Sample packaging and shipping were handled by Focus and Airtech personnel.

2.3.2 Deviations from the Test Plan

Siemens Water Technologies Corp. conducted preliminary testing prior to the formal PDT in order to ensure that all process, spiking, sampling, and analytical systems and procedures were appropriate, and that the test team could identify and resolve any major issues prior to the formal PDT. During the preliminary testing and subsequent planning activities, several items were identified and corrective actions were initiated. These were documented through Corrective Action Requests (CARs) as provided for in the QAPP. Additionally, EPA provided Siemens Water Technologies Corp. with certain data submittal requests in the test plan approval letter, and also required Siemens Water Technologies Corp. to establish additional operating parameters (Hearth #5 minimum and maximum temperature) that were not addressed in the approved test plan. Additionally, conditions during the test dictated that several field directives be given; some of which warranted documentation through the CAR process.

A total of eight CARs were generated during the PDT and are shown in Appendix C. Additional verbal directives were given in the field and to the laboratory during the course of the PDT program. Each corrective action and verbal directive is discussed fully in Section 5.0, and is summarized below:

1. The selected laboratory for the performance test has a slightly different target analyte list compared to those presented in the original test plan. Revised target analyte lists were presented to EPA and were approved for use in the test. This is documented as CAR-001.
2. The original test plan calls for an organic surrogate mixture to be added to the spent activated carbon feed. That mixture was specified to contain 1,1,1-Trichloroethane, however the compound is not available because it is an ozone depleting substance. Methylene chloride was substituted for 1,1,1-trichloroethane. This is documented as CAR-002.
3. Based on observations made during preliminary testing, it was believed that the high stack gas moisture content and low particulate matter concentration would not be conducive to the use of a Cascade Impactor, which was originally planned for collection of particle size distribution data. Therefore, a Method 5 train, employing a smooth filter media was used to collect particulate matter samples, followed by scanning electron microscope examination of the particles to determine the particle size distribution. This is documented as CAR-003.
4. Prior to the test, the analytical laboratory expressed concern that analytical surrogate compounds placed onto the adsorbent resin in some of the sampling trains might be stripped off unless sampling is conducted at very low sampling rates. In order to address this concern, all semivolatile organic sampling trains were operated for a nominal sampling run time of 4 hours instead of the planned nominal sampling time of three hours. The same nominal volume of sample was collected over the four hour period that would have been collected in three hours. This represents a very conservative approach to the issue, and is documented as CAR-004.
5. EPA indicated that a minimum temperature limit must be established for Hearth #5 in the reactivation furnace. This condition was not anticipated, nor was it addressed in the Performance Demonstration Test Plan. After discussions with EPA, it was decided that a separate test will be conducted outside the formal PDT test period where a minimum Hearth #5 temperature will be maintained and the resulting reactivated carbon will be analyzed for organics. This is documented as CAR-005.
6. Several modifications to the target operating conditions and anticipated permit limits were made after approval of the Performance Demonstration Test Plan. Most of these changes were made as a result of preliminary testing. Additionally, EPA included with their test plan approval letter a table of information and process data that they wanted included in the test report. Revised operating condition targets and the list of data requested by EPA are documented as CAR-006.
7. During Run 2 of the PDT, the glass probe liner on the M0023A train was broken due to high winds swinging the sampling train as it was being moved from one traverse point to another. The stack sampling crew and regulatory observers noted the break and immediately stopped sampling. Upon investigation, it was found that both pieces of the broken probe liner could be retrieved and that the sampling train leak-checked from the break through the remainder of the train. All parties agreed that there was no impact on sample integrity, so the broken probe liner pieces were capped, taken to the recovery area and rinsed. The probe liner was replaced and the train was used to complete the sampling run. The rinse of the broken probe liner pieces was combined with the final train rinse to capture the entire sample. This is documented as CAR-007.

8. In order to maximize the stack gas flow rate (minimize the gas residence time) for the performance test, a source of additional air was needed beyond what is normally supplied by the combustion air fan. The access door on Hearth #1 was opened to allow additional air to be drawn into the system and to pass through the combustion and air pollution control portions of the system. This is documented as CAR-008.
9. Makeup water samples were planned to be collected only once, at the beginning of the test. Siemens Water Technologies Corp. personnel were concerned however, that the quality of the makeup water could change significantly over time, thus makeup water samples were collected at the beginning of each test run. This modification increased the number and frequency of makeup water samples.
10. In order to keep any water droplets and particulate matter from entering the M0040 sampling train, a glass wool plug was inserted into the sample probe. This was not described in the test plan, but was deemed to be a good operating practice for this train.
11. At the end of Run 1, the Test Manager noticed that the silica gel in the M0061 train was quite wet. The sampling team was directed to add an additional silica gel impinger to the M0061 train to prevent this situation from occurring again. A check of the moisture determination from the M0061 train used in Run 1 was compared to the moisture determinations from the other Run 1 trains, and found to be consistent. Thus there was no adverse impact on the Run 1 M0061 sample.
12. It was noted that Siemens Water Technologies Corp.'s installed stack gas flow rate monitor was not corresponding with the Pitot tube readings of the stack sampling team. Further investigation indicated that some type of fault in the stack gas flow rate monitor was being experienced, however it was not able to be corrected during the course of the PDT. All parties were informed of the situation, and a decision was made to complete the PDT and to use the average of the stack gas sampling train flow rate determinations from each run to set the maximum stack gas flow rate operating limit for the system. Siemens Water Technologies Corp. will need to correct the fault in the stack gas flow rate monitoring system in order to demonstrate continuing compliance with the operating limit.

All other testing and process operations were conducted in conformance with the approved PDT Plan and QAPP. EPA also requested that split samples of the process feed materials and effluents be provided. Additional sample volume was collected accordingly, and samples were split with EPA.

A few analytical quality control determinations showed non-conformances with the target data quality objectives. However, none of these non-conformances are deemed to have had a significant negative impact on the PDT results or conclusions. These items are discussed in Section 5.0 of the report and in the Data Validation Report in Appendix H.

3.0 PROCESS OPERATIONS

3.1 PROCESS OPERATING CONDITIONS

Key process operating parameters were continuously monitored and recorded during each test run by the process computer system. Process operating data were stored on magnetic disk at one-minute intervals during each test run. Appendix A presents complete printouts of the process operating data from each test run.

Manual logs were kept during the PDT to record the times when sampling runs were started, stopped, and/or interrupted. The PDT Manager's manual log is included in Appendix B. Tables 3-1 through 3-3 summarize key operating data collected during each PDT run.

Key process instruments were calibrated prior to the PDT. The CEM system underwent a Performance Specification Test prior to the PDT, and underwent daily calibration checks during the PDT. The Performance Specification Test and each daily calibration check showed the CEM system to be operating within specifications. A copy of the CEMS Performance Specification Test Report is included in Appendix K. Process instrument calibration data is presented in Appendix L.

3.2 FEED MATERIAL CHARACTERISTICS AND CONSTITUENT FEED RATES

The spent activated carbon feed to RF-2 was sampled at 15-minute intervals and composited during each PDT run. Makeup water samples were collected at the beginning of each run. Caustic used in the APC system was sampled once for the PDT program. Feed sampling logs, as well as other sampling information, are summarized in Appendix D. A list of samples is presented in Appendix E. Analyses of the feed samples, as well as summaries of all CPT analytical results are shown in Appendix F. Feed material physical/chemical characteristics are presented in Table 3-4. Constituent feed rate information (e.g., total chlorine/chloride, metals, and each POHC) is presented in Table 3-5. Table 3-6 presents volatile organic feed data. Semivolatile organic feed data are presented in Table 3-7. Example calculations are presented in Appendix G. (Note that the complete sampling report and full analytical data packages have been submitted as separate volumes.)

3.3 SPENT ACTIVATED CARBON FEED SPIKING

Monochlorobenzene and tetrachloroethene (perchloroethylene) were the designated POHCs, and were spiked onto the spent activated carbon feed in all PDT runs. Lead and chromium were spiked onto the spent activated carbon feed during each run to represent semivolatile, and low volatility metals, respectively. Additionally an organic surrogate mixture of methylene chloride, toluene, naphthalene, and ethylene glycol was added to the spent activated carbon to increase the organic loading and to provide a variety of compounds for the formation of a broad array of emission products. Spiking was conducted downstream of the feed sampling point, using metering pumps and mass flow meters, backed up by calibrated electronic scales. Spiking rates are summarized in Table 3-8. A complete spiking report is presented in Appendix J. The spiking report contains copies of all field data sheets, calibrations and spiking material composition certifications.

3.4 MAKEUP AND EFFLUENT CHARACTERISTICS

Makeup water and caustic solution are added to the scrubbing system. Effluent streams are the scrubber blowdown water and POTW discharge. Results of the makeup and effluent material analyses are summarized in Table 3-9. Summaries of all analyses are presented in Appendix F. Complete analytical data packages have been submitted as separate volumes.

4.0 COMPLIANCE RESULTS

Using the process operating data and analytical results from the PDT program, the performance of the Siemens Water Technologies Corp. Carbon Reactivation Furnace RF-2 system was determined and compared to the performance requirements specified for the facility. The PDT demonstrated the RF-2 unit's ability to meet all regulatory requirements. Table 4-1 presents performance results for each key parameter during the PDT, and compares the performance results with target criteria. Example calculations for each performance determination are shown in Appendix G.

Stack gas sampling was conducted by Airtech Environmental Services, Inc. Summaries of the sampling conditions are presented in each table of stack emission results. A complete report of Airtech's sampling results, including all field data sheets, calibration records, and calculations is presented in Appendix I. Example calculations for each PDT determination are presented in Appendix G. Analytical summaries are presented in Appendix F. Complete analytical data packages are presented in separate volumes.

4.1 POHC DESTRUCTION AND REMOVAL EFFICIENCY

Monochlorobenzene and tetrachloroethene were designated as the POHCs for the test. DRE results are summarized in Table 4-2. The PDT demonstrated that the RF-2 unit achieved a DRE of greater than 99.99% for each POHC in all runs.

4.2 DIOXIN AND FURAN EMISSIONS

Dioxin and furan sampling results and emission concentrations are presented in Tables 4-3 through 4-5. The data presented show the PCDD/PCDF emissions are in compliance with the HWC MACT standard of 0.40 ng TEQ/dscm corrected to 7% O₂ applicable to existing systems with a temperature at the entrance to the primary particulate matter control device of 400°F or less. [40 CFR 63.1203(a)(1)(ii)].

4.3 PARTICULATE EMISSIONS

Particulate matter sampling results and emission concentrations are shown in Tables 4-6 through 4-8. Particulate matter concentrations met the regulatory requirement for the PDT in all runs.

4.4 HYDROGEN CHLORIDE AND CHLORINE EMISSIONS

Tables 4-6 through 4-8 presents the results of HCl and Cl₂ emissions determinations during the PDT. HCl/Cl₂ emission concentrations were significantly below the performance criteria in all runs.

4.5 METALS EMISSIONS

Metal sampling and emissions results are presented in Tables 4-9 through 4-11. The results indicate that the system met the applicable emission standards for volatile metals (mercury), semivolatile metals (the sum of lead and cadmium emissions), and low volatility metals (the sum of arsenic, beryllium, and chromium emissions).

Further, data from the test were used to develop a system removal efficiency (SRE) for the low volatility metal group. These values are used along with the feed rates of spiked low volatility metal during the test to develop an extrapolated low volatility metals feed rate limit in accordance with 40 CFR 63.1209(n)(2)(ii) and the approved PDT Plan. The actual feed rate of mercury and semivolatile metals demonstrated during the test were used to establish feed rate limits for these metals, without extrapolation. Detailed information regarding the establishment of metals feed rate limits and other process operating limits is presented in Section 6.0 of the report.

4.6 STACK GAS OXYGEN, CARBON MONOXIDE, AND TOTAL HYDROCARBONS

Siemens Water Technologies Corp.'s CEM system was used to monitor the stack gas O₂, and CO concentrations during the PDT. A temporary CEM was operated by Airtech during the PDT for THC measurements. These CEM readings were used to demonstrate regulatory compliance and to make corrections to specific stack gas concentration values that are reported on a 7% O₂ corrected basis. Both the carbon monoxide and total hydrocarbon concentrations met the regulatory requirements in all test runs as indicated in Table 4-1. The CEM data are summarized with the process operating data in Tables 3-1 through 3-3, and in Appendix A. In addition, Airtech used CEM oxygen and carbon dioxide data to determine the stack gas molecular weight for use in emissions calculations. The oxygen and carbon dioxide data results are shown in the summary tables for each sampling train and are presented in Airtech's Stack Sampling Report in Appendix I.

5.0 QUALITY ASSURANCE/QUALITY CONTROL RESULTS

The PDT QAPP specifies procedures to be followed to assure the quality of data generated from the test program. Target data quality objectives (DQOs) and specific QA/QC procedures are presented in the QAPP for the following:

- Sample collection
- Sample analysis
- Process instrument calibration
- Stack sampling equipment calibration
- Laboratory analytical instrument calibration.

This section presents an overview of the QA/QC activities implemented during the PDT to ensure and assess the quality of the data gathered. This section also presents the QA/QC results for the PDT, and an assessment of the quality of the data gathered.

5.1 QA/QC ACTIVITIES AND IMPLEMENTATION

Siemens Water Technologies Corp. personnel were involved in all phases of project planning including the development of Data Quality Objectives (DQOs), the selection of sampling and analysis methods, the selection of contractors, and the development and review of project controlling documents. Primary references for the selection of methods and setting DQOs included:

- USEPA SW-846, Test Methods for Evaluating Solid Waste
- 40 CFR 266 Appendix IX and the Appendix to 40 CFR 63, Subpart EEE, Performance Specifications for Continuous Emission Monitoring Systems
- USEPA QAMS-005/80, Interim Guidelines and Specifications for Preparing Quality Assurance Project Plans
- EPA/625/6-89/023, Quality Assurance/Quality Control (QA/QC) Procedures for Hazardous Waste Incineration
- EPA/600/4-77-027b, Quality Assurance Handbook for Air Pollution Measurement Systems, Volume III, Stationary Source Specific Methods
- 40 CFR 60 Appendix A, Test Methods and Procedures, New Source Performance Standards
- 40 CFR 61 Appendix B, Test Methods.

5.1.1 QA Surveillance

Part of the overall program QA/QC is the coordination of process operations and sampling activities during the test. This coordination effort is intended to identify potential operating upsets or sampling problems in the field, and to institute corrective actions as required. These field actions include holding, stopping, and/or repeating test runs as needed to ensure the collection of adequate and representative data. A log is kept by the PDT Manager to document performance test activities and noteworthy occurrences that may be beneficial to the reconstruction of events or to the evaluation of PDT results. Appendix B contains a copy of the PDT Manager's manual log.

During the PDT, there were no process-related interruptions to sampling activities. There were two interruptions in sampling which occurred due to other causes.

During Run 2 as the Method 0023A sampling train was being moved to the last traverse point in the first half of the run, the glass probe liner broke. The sampling team and regulatory observers noticed the break immediately when it occurred, and the sampling team shut down the sample pump. Since it was known when the break occurred and sampling was immediately stopped, it was decided to recover both parts of the broken probe liner, replace the probe, and continue sampling. All parties were aware of the situation and approved of the action taken.

During Run 3, a problem developed with the organic surrogate mixture spiking system. All sampling was placed on hold while the problem was corrected. All process operations and other spiking activities continued without interruption. Once the organic surrogate mixture spiking system was returned to service, all sampling was resumed, and the run finished without further interruption.

No negative impact on sampling or analysis occurred as a result of these interruptions, nor were there any other occurrences noted that would impact the PDT results or conclusions.

Several items were identified throughout the course of the PDT program (including preliminary testing conducted by Siemens Water Technologies Corp. in preparation for the formal PDT) which could either be classified as nonconformances with the test methods or specifications of the project controlling documents, or as potential areas for improvement. Where modifications to the protocols or field activities were necessary, they were implemented through field directives and/or the issuance of a Corrective Action Request (CAR). Copies of each CAR are included in Appendix C. The sections below discuss the PDT activities and include a description of any QA/QC observations, procedural modifications, or CARs issued.

5.1.2 Sample Collection

Feed, effluent, and stack gas samples were collected and analyzed as part of the PDT program. Sampling QA/QC objectives are considered to be met if sampling activities follow the standard methods described in the PDT Plan and QAPP. During this test, sampling activities followed the prescribed procedures of the PDT Plan and QAPP, with the following exceptions:

1. Based on observations made during preliminary testing, it was believed that the high stack gas moisture content and low particulate matter concentration would not be conducive to the use of a Cascade Impactor, which was originally planned for collection of particle size distribution data. Therefore, a Method 5 train, employing a smooth filter media was used to collect particulate matter samples, followed by scanning electron microscope examination of the particles to determine the particle size distribution. This is documented as CAR-003.
2. Prior to the test, the analytical laboratory expressed concern that analytical surrogate compounds placed onto the adsorbent resin in some of the sampling trains might be stripped off unless sampling is conducted at very low sampling rates. In order to address this concern, all semivolatile organic sampling trains were operated for a nominal sampling run time of 4 hours instead of the planned nominal sampling time of three hours. The same nominal volume of sample was collected over the four hour period that would have been collected in three hours. This represents a very conservative approach to the issue, and is documented as CAR-004.
3. During Run 2 of the PDT, the glass probe liner on the M0023A train was broken due to high winds swinging the sampling train as it was being moved from one traverse point to another. The stack sampling crew and regulatory observers noted the break and immediately stopped sampling. Upon investigation, it was found that both pieces of the broken probe liner could be retrieved and that the sampling train leak-checked from the break through the remainder of the train. All parties agreed that there was no impact on sample integrity, so the broken probe liner pieces were capped, taken to the recovery area and rinsed. The probe liner was replaced and the train was used to complete the sampling run. The rinse of the broken probe liner pieces was combined with the final train rinse to capture the entire sample. This is documented as CAR-007.
4. Makeup water samples were collected at the beginning of each run rather than being collected only once at the beginning of the test program. This change was made based on plant personnel's recommendations and concerns that the makeup water quality could potentially change over time. This modification is viewed as an improvement to the original test protocol.
5. In order to keep any water droplets and particulate matter from entering the M0040 sampling train, a glass wool plug was inserted into the sample probe. This was not described in the test plan, but was deemed to be a good operating practice for this train.
6. At the end of Run 1, the Test Manager noticed that the silica gel in the M0061 train was quite wet. The sampling team was directed to add an additional silica gel impinger to the M0061 train to prevent this situation from occurring again. A check of the moisture determination from the M0061 train used in Run 1 was compared to the moisture determinations from the other Run 1 trains, and found to be consistent. Thus there was no adverse impact on the Run 1 M0061 sample.

7. EPA requested that split samples of the process feed materials and effluents be provided. Additional sample volume was collected accordingly, and samples were split with EPA.

Prior to the CPT, a database of all expected field samples was developed and cross-referenced with the analyses planned for each sample. A master list of samples generated from the database was used as a field QC checklist to help ensure that all samples were collected and shipped to the laboratory. Sample collection activities were recorded on log sheets, samples were labeled, packaged, and shipped to the analytical laboratory using traceability procedures described in the QAPP. Included with the samples were request-for-analysis forms specifying the required analyses for each sample. Copies of the process sample collection logs are included in Appendix D. Copies of the chain-of-custody records, and an index of sample numbers and identifications are included in the analytical data packages. Stack gas sample collection sheets are included with the full stack sampling report in Appendix I of this report. A review of the sample collection log sheets indicates that samples were collected as required, all applicable data were recorded, and sampling equipment conditions and operating parameters (particularly applicable to stack sampling activities) were within the requirements of the applicable methods.

5.1.3 Sample Analysis

Analytical data quality was determined through the analysis of blanks, duplicates, spiked samples, and reference materials, as prescribed by the QAPP. In large measure, the analytical data quality objectives for the PDT program were met. Section 5.2, below, and the data validation report in Appendix H, present more detailed results for each analytical data quality determination. Other observations and notes regarding sample analysis are provided in the next several paragraphs.

1. The selected laboratory for the performance test has a slightly different target analyte list compared to those presented in the original test plan. Revised target analyte lists were presented to EPA and were approved for use in the test. This is documented as CAR-001.
2. Several analytical results for the POHCs in the stack gas were above the upper calibration range of the analytical instrument. Since these analyses totally consume the sample, there was no opportunity to conduct a dilution and reanalyze the samples. The laboratory therefore reported estimated values. When this situation came to the attention of the PDT Manager and QA Manager, the laboratory was asked if anything could be done to qualify these estimates to ensure that they were valid. The laboratory set up an extended calibration curve for the affected compounds and requantified the samples as discussed in the case narrative of the VOST analytical data package. The requantified results were all less than the original reported results, therefore the original results are considered to be biased high. In order to be conservative in the use of these data, the original high emission values were used for calculating Destruction and Removal Efficiency, thus resulting in a conservatively low DRE.

5.1.4 Operations and Process Instrumentation

Process monitoring systems were calibrated prior to the PDT. Calibration data is presented in Appendix L. All process instrumentation met the performance criteria, and were deemed to produce reliable data, with one exception. While the stack gas flow rate monitoring system showed acceptable calibration results prior to the test, it was noted during the course of the PDT, that Siemens Water Technologies Corp.'s installed stack gas flow rate monitor was not corresponding with the Pitot tube readings of the stack sampling team. Further investigation indicated that some type of fault in the stack gas flow rate monitor was being experienced, however it was not able to be corrected during the course of the PDT. All parties were informed of the situation, and a decision was made to complete the PDT and to use the average of the stack gas sampling train flow rate determinations from each run to set the maximum stack gas flow rate operating limit for the system. Siemens Water Technologies Corp. will need to correct the fault in the stack gas flow rate monitoring system in order to demonstrate continuing compliance with the operating limit.

A CEMS Performance Specification Test was conducted prior to the PDT, and the emissions monitors met the applicable performance requirements. A CEMS Performance Specification Test Report is presented in Appendix K. Daily calibration of stack gas continuous emissions monitoring systems was conducted during the PDT. Each monitor met the calibration criteria during each day of testing.

The original test plan calls for an organic surrogate mixture to be added to the spent activated carbon feed. That mixture was specified to contain 1,1,1-Trichloroethane, however the compound is not available because it is an ozone depleting substance. Methylene chloride was substituted for 1,1,1-trichloroethane. This is documented as CAR-002.

Several modifications to the target operating conditions and anticipated permit limits were made after approval of the Performance Demonstration Test Plan. Most of these changes were made as a result of preliminary testing. Additionally, EPA included with their test plan approval letter a table of information and process data that they wanted included in the test report. Revised operating condition targets and the list of data requested by EPA are documented as CAR-006.

In order to maximize the stack gas flow rate (minimize the gas residence time) for the performance test, a source of additional air was needed beyond what is normally supplied by the combustion air fan. The access door on Hearth #1 was opened to allow additional air to be drawn into the system and to pass through the combustion and air pollution control portions of the system. This is documented as CAR-008.

5.1.5 Stack Sampling Equipment

All stack sampling equipment was calibrated according to the protocols given in the applicable sampling methods. Each sampling system passed the calibration criteria. Stack sampling equipment calibration records are included in the Stack Sampling Report in Appendix I, of this report.

5.1.6 Laboratory Analytical Instrumentation

QA/QC procedures, as specified by the analytical methods and summarized in the PDT Plan and QAPP, were conducted and documented during the test. Analytical instrument calibration records and all raw analytical data are presented in the analytical data packages, submitted as separate volumes. No calibration problems were identified by the laboratories.

5.2 AUDITS AND DATA VALIDATION

The following audits were provided for in the QAPP:

- Field audits
- Performance Evaluations
- Office Audits
- Laboratory Audits.

A field audit was used to ensure that work was performed in accordance with the various project controlling documents and associated standard operating procedures. This audit was conducted throughout the test by the PDT Manager through observation of process operations and sample collection. It is the opinion of the PDT Manager, based on field observations, that all work was performed in substantial compliance with the specifications contained in the PDT Plan and QAPP.

VOST audit samples (spiked Tenax resin) were provided by the regulatory agencies. An initial set of VOST audit tubes were received from EPA's contract laboratory and were analyzed with the samples from the PDT. These initial audit samples, however were received without proper documentation and preservation, and were thus deemed to be of suspect validity. EPA was informed of the issue and another set of VOST audit tubes were received from EPA's contract laboratory (this time with proper documentation and preservation). These audit samples were submitted to the laboratory for analysis, but the timing was such that they were not analyzed with the actual PDT samples. Results for all of the audit sample received are presented in Table 5-1. The test team participants do not know the true value of the audit samples, so the analytical results are reported here for review by the regulatory agencies.

The preparation of this report was conducted under the office QA/QC program in place at Focus. All records, correspondence, calculations, data, and reports are maintained in designated files for future reference. Reports, numerical tabulations, drawings, and calculations are checked for completeness and technical correctness, and documented prior to release in final form to the client.

Laboratory audits were provided for in the PDT Plan and the QAPP as an option to be exercised, if necessary, during the test program. No situations arose through the course of the test program which suggested the need for a laboratory audit.

Data validation consisted of a thorough check of all calculations involved in reducing sampling and analysis data. Subsequently, the data were compared to expected values and were investigated for consistency within and between test runs. For example, comparisons were made of stack gas flow rates, process operating temperatures, and sampling equipment operating conditions. Analytical data were reviewed to identify variations between duplicate measurements of the same parameter, either from multiple analyses of the same sample or from analyses between replicate test runs. Finally, QA/QC results were compared to the target data quality objectives defined in the QAPP and in the laboratory standard operating procedures (SOPs). During the project, 12,491 analytical data quality indicators were evaluated. Over 93 percent of the data quality objectives were completed and met. The data compare well within and between runs, and the measurements agree well with the expected values. The data are technically sound and are usable for their intended purpose. A data validation report is presented in Appendix H.

5.3 CALCULATIONS

Where applicable, the RF-2 system's performance and/or emissions were calculated using formulas presented in appropriate regulations. Other calculations followed generally accepted practice for thermal treatment process operations and performance test reporting. Many calculations were made using spreadsheets specifically designed by Focus for performance test data reduction and reporting, while other calculations were made by hand. Appendix G documents how all calculations were made for performance determination during this test program.

5.4 CONCLUSIONS

Overall, the PDT was executed in substantial conformance to the requirements and specifications of the project controlling documents. Any anomalies observed have been documented and corrective actions have been implemented as necessary. The impact of these anomalies has been thoroughly reviewed and assessed. In the judgment of the PDT Manager, those anomalies do not have a discernible negative impact on data quality or the utility of the data gathered to serve their intended purpose as defined in the PDT Plan and QAPP.

6.0 OPERATING PARAMETER LIMITS

The Siemens Water Technologies Corp. Carbon Reactivation Furnace RF-2 system demonstrated compliance with all applicable regulatory requirements during the PDT program. Operating parameter limits and associated automatic waste feed cutoff setpoints (as applicable) will be established as described in the approved PDT Plan and in the appropriate regulations of 40 CFR 63 Subpart EEE. Most operating parameter limits are based on demonstrations made during the PDT. For some parameters, such as maximum stack gas CO concentration, and minimum packed bed scrubber pressure differential, either regulation, guidance, or equipment manufacturer's recommendations (rather than the PDT demonstrated values) are used as the basis for the limit.

6.1 DEVELOPMENT OF OPERATING LIMITS

Limits on a number of operational control parameters must be maintained as an indication that the RF-2 system continues to operate in compliance with the applicable emission standards. Table 6-1 summarizes the discussion of the operational parameter limits for the RF-2 unit. To facilitate review, the operating parameters are grouped into the following categories:

- Group A1 parameters are continuously monitored and recorded, and are interlocked with the automatic waste feed cutoff system. Group A1 parameter limits are established from test operating data, and are used to ensure that system operating conditions are equal to or are more rigorous than those demonstrated during the test.
- Group A2 parameters are continuously monitored and recorded, and are interlocked with the automatic waste feed cutoff system. Group A2 parameter limits are established based on regulatory requirements rather than on the test operating conditions, e.g., the maximum stack CO concentration.
- Group B parameters are continuously monitored and recorded, but are not required to be interlocked with the automatic waste feed cutoff system. Operating records are required to ensure that established limits for these parameters are not exceeded. The Group B parameter limits are established based on the operation of the system during the test.
- Group C parameters are continuously monitored and recorded, but are not required to be interlocked with the automatic waste feed cutoff system. Group C parameter limits are based on manufacturer's recommendations, operational safety, and good operating practice considerations rather than on the test operating conditions, e.g., the minimum packed bed scrubber pressure differential.

6.2 SPECIFIC OPERATING PARAMETERS

Operating parameter limits for each of the control parameters have been established as specified in the HWC MACT regulations given in 40 CFR 63.1209 and the approved PDT plan. The following sections describe how each operating parameter limit has been established.

In addition to establishing specific operating limits, Siemens Water Technologies Corp. anticipates having limits on the types of waste that can be treated in RF-2. Since Siemens Water Technologies Corp. has demonstrated greater than 99.99% DRE during the PDT while treating chlorobenzene, a Class 1 (most thermally stable) compound, it is expected that Siemens Water Technologies Corp. will be permitted to treat all of the materials represented by the waste codes in the facility's most recent RCRA Part A permit application. Specific prohibitions are anticipated in the site's permit, for feed materials containing greater than 50 ppm of PCBs and those listed with the waste codes F020, F021, F022, F023, F026 or F027.

6.2.1 Parameters Demonstrated During the Test (Group A1 Limits)

Group A1 parameter limits are based on the results of the testing. The following operating parameters will be established as Group A1 parameters for the RF-2 system.

6.2.1.1 Maximum Spent Carbon Feed Rate

The PDT was conducted in order to demonstrate the maximum feed rate of spent carbon. The spent carbon feed rate is monitored on a continuous basis. The maximum allowable spent carbon feed rate has been established as a block hour average limit from the average of feed rates demonstrated during each of the three runs of the PDT.

6.2.1.2 Minimum Afterburner Temperature

The PDT was conducted at the minimum afterburner temperature with maximized combustion gas flow rate (minimum residence time), since these are the conditions least favorable for DRE. Organic emissions were also measured under these conditions for risk assessment purposes. Based on successful demonstration of DRE during the PDT, the minimum temperature limit has been established as an hourly rolling average equal to the average of the demonstrated test run average values.

6.2.1.3 Minimum and Maximum Hearth #5 Temperature

As part of EPA's approval of the PDT Plan, Siemens Water Technologies Corp. was required to establish both a minimum and maximum temperature limit for Hearth #5 of the reactivation furnace. Since both a minimum and maximum temperature could not be demonstrated in the single test condition approved for

the test, Siemens Water Technologies Corp. operated Hearth #5 at a maximum temperature during the PDT and will conduct a separate minimum temperature test outside of the formal PDT period.

The maximum Hearth #5 temperature limit has been established as an hourly rolling average equal to the average of the demonstrated test run averages.

6.2.1.4 Minimum Venturi Scrubber Differential Pressure

The performance test was conducted to demonstrate the minimum venturi scrubber differential pressure. Venturi scrubber differential pressure is monitored on a continuous basis. Based on successful demonstration of particulate and metals control during the performance test, the minimum venturi scrubber differential pressure limit has been established as the average of the hourly rolling average values demonstrated during each run of the performance test. The permit limit is also expected to be an hourly rolling average value.

6.2.1.5 Minimum Quench/Venturi Scrubber Recycle Liquid Flow Rate

The performance test was conducted to demonstrate the minimum quench/venturi scrubber recycle flow and maximum stack gas flow, thus establishing a *de facto* minimum liquid to gas ratio. Quench/Venturi scrubber flow and stack gas flow are both monitored on a continuous basis. Based on successful demonstration during the performance test, the minimum quench/venturi scrubber recycle liquid flow rate limit has been established based on the average of the hourly rolling average values demonstrated during each run of the performance test. This limit will be established as an hourly rolling average.

6.2.1.6 Minimum Packed Bed Scrubber pH

The performance test was conducted to demonstrate the minimum packed bed scrubber pH at maximum total chlorine/chloride feed rate. Scrubber pH is monitored on a continuous basis. Based on successful demonstration of HCl and Cl₂ control during the performance test, the minimum packed bed scrubber pH limit has been established as the average of the hourly rolling average pH values demonstrated during each run of the performance test. The permit limit will be administered as an hourly rolling average.

6.2.1.7 Minimum Packed Bed Scrubber Recycle Liquid Flow Rate

The performance test was conducted to demonstrate the minimum packed bed scrubber recycle flow rate and maximum stack gas flow, thus establishing a *de facto* minimum liquid to gas ratio. Packed bed scrubber recycle flow and stack gas flow are both monitored on a continuous basis. Based on successful demonstration of HCl and Cl₂ control during the performance test, the minimum packed bed scrubber recycle liquid flow rate limit has been established as the average of the hourly rolling average values demonstrated during each run of the performance test. This limit will also be administered on an hourly rolling average basis.

6.2.1.8 Minimum Scrubber Blowdown Flow Rate

The performance test demonstrated a minimum scrubber blowdown flow rate, in order to demonstrate worst case conditions for solids buildup in the scrubbing system. In order to conserve water, Siemens Water Technologies Corp. recycles most of the liquid from the air pollution control system. However, in order to prevent the buildup of dissolved solids in the recycled water, a certain amount of the water must be purged (or blown down) from the system. As water is purged from the system, fresh makeup water is added. The minimum scrubber blowdown flow rate limit has been based on the average of the hourly rolling average values demonstrated during each run of the performance test. This limit will be administered as an hourly rolling average.

6.2.1.9 Minimum WESP Secondary Voltage

Although the HWC MACT regulations do not require any indicator of performance in an electrically enhanced emissions control device, Siemens Water Technologies Corp. believes that it is appropriate to establish a performance indicator. Accordingly, WESP secondary voltage (expressed as KVDC) is used as the indicator of continuing WESP performance. The minimum value has been established as the average of the minimum hourly rolling average secondary voltage values demonstrated during each run of the performance test. The secondary voltage limit will be based on an hourly rolling average.

6.2.1.10 Maximum Combustion Gas Velocity (Stack Gas Flow Rate)

The stack gas flow rate (expressed as actual cubic feet per minute) is used as the indicator of combustion gas velocity. The maximum stack gas flow rate was planned to be established from the mean of the maximum hourly rolling average stack gas flow rates measured by Siemens Water Technologies Corp.'s stack gas flow rate monitor during each run of the performance test. As stated in earlier sections of this report, the stack gas flow rate monitor experienced difficulties during the PDT such that the measurements were not reliable. Each isokinetic sampling system used for stack gas emissions measurements during the PDT also included the measurement of stack gas flow rate. Thus, the average stack gas flow rate determinations for each run, derived from the stack gas sampling systems, has been used to establish a maximum stack gas flow rate limit. The maximum stack gas flow rate limit will be administered as an hourly rolling average.

6.2.2 Group A2 Parameters

6.2.2.1 Maximum Stack Gas CO Concentration

The maximum hourly rolling average stack gas CO concentration was maintained at or below 100 ppmv corrected to 7% oxygen (dry basis) during the test. An operating parameter limit for maximum stack gas

carbon monoxide concentration of 100 ppmv hourly rolling average corrected to 7% oxygen will be established.

6.2.2.2 Fugitive Emissions Control

The HWC MACT regulations require controlling combustion system leaks. By design (no open feed systems), the combustion chamber constitutes a sealed system. There are no locations for combustion system leaks to occur. Therefore, the RF-2 system is in compliance with 40 CFR 63.1206(c)(5)(i)(A).

6.2.3 Group B Parameters

6.2.3.1 Maximum Total Chlorine/Chloride Feed Rate

During the PDT, Siemens Water Technologies Corp. maximized the feed rate of total chlorine/chloride through the spiking of tetrachloroethene and other chlorinated organic compounds. Since the HCl and Cl₂ emissions measured during the PDT were less than the applicable standard, the limit for total chlorine/chloride feed rate has been set as a 12-hour rolling average, equal to the average of the average total chlorine/chloride feed rate during the three runs of the PDT. Total chlorine/chloride includes the native chlorine/chloride in the spent activated carbon feed plus the spiked chlorine/chloride. Records of feed analyses, and the calculated 12-hour rolling average total chlorine/chloride feed rate values will be maintained to demonstrate compliance with the chlorine/chloride feed rate limit.

6.2.3.2 Maximum Mercury Feed Rate

Due to the low amounts of mercury expected in the spent activated carbon, Siemens Water Technologies Corp. has elected to comply with the mercury standard by calculating and complying with a 12-hour rolling average Maximum Theoretical Emission Concentration (MTEC), conservatively assuming no mercury removal across the APC system. The MTEC is complied with as a maximum mercury feed rate limit. This limit has been calculated from the performance test data by using the stack gas flow rate and oxygen concentration, and the maximum allowable stack gas mercury concentration based on the HWC MACT regulations. The feed rate limit is determined assuming that all mercury is emitted, and is complied with as a maximum 12-hour rolling average mercury feed rate limit.

6.2.3.3 Maximum Semivolatile Metals Feed Rate

Siemens Water Technologies Corp. demonstrated compliance with the semivolatile metal emission standard while spiking lead during the test. Therefore, the permitted feed rate limit for semivolatile metals (total cadmium plus lead) has been set as a 12-hour rolling average value equal to the average semivolatile metal feed rate demonstrated during the three runs of the PDT. Records of feed analyses, and the calculated 12-hour rolling average semivolatile metal feed rate values will be maintained to demonstrate compliance with the semivolatile metal feed rate limit.

6.2.3.4 Maximum Low Volatility Metals Feed Rate

Siemens Water Technologies Corp. demonstrated compliance with the low volatility metal emission standard while spiking chromium during the test. The emissions measured during the test were significantly lower than the allowable limit. Therefore, the permitted feed rate limit for low volatility metals (total arsenic, plus beryllium, plus chromium) will be set as a 12-hour rolling average extrapolated upward to the HWC MACT standard based on the average low volatility metal feed rate and the average low volatility metal System removal Efficiency (SRE) during the three runs of the CPT. Extrapolation has been conducted as described in the approved PDT Plan. Records of feed analyses, and the calculated 12-hour rolling average low volatility metal feed rate values will be maintained to demonstrate compliance with the low volatility metal feed rate limit.

6.2.4 Group C3 Parameters

Group C parameter limits are based on manufacturer's recommendations, operational safety and good operating practice considerations. The following parameters are proposed as Group C parameters.

6.2.4.1 Minimum Packed bed Scrubber Pressure Differential

The minimum packed bed scrubber pressure differential is based on past operating experience. This limit has been established as an hourly rolling average limit.

6.3 EXTRAPOLATION OF METALS FEED RATE LIMITS

Siemens Water Technologies Corp. spiked lead and chromium into RF-2 during the PDT. Lead and chromium are representative of the semivolatile and low volatility metal groups, respectively. Since the lead emissions were very close to the applicable standard during the PDT, Siemens Water Technologies Corp. has established the maximum semivolatile metal feed rate as the average feed rate that was demonstrated during the three runs of the PDT. The emissions of low volatility metals however, were substantially below the standard during the PDT, thus Siemens Water Technologies Corp. has extrapolated the test results upward to establish a low volatility metals feed rate limit. PDT data has been used to calculate a system removal efficiency (SRE) for chromium, which can then be applied to the LVM metal volatility group. System removal efficiency is shown in Table 6-2, and was calculated using the following equation:

$$SRE_i = \left[1 - \frac{\dot{m}_{i,out}}{\dot{m}_{i,in}} \right] \times 100\%$$

where:

$\dot{m}_{i,in}$ = mass feed rate of metal i.

$\dot{m}_{i,out}$ = mass emission rate of metal i.

SRE_i = demonstrated system removal efficiency of metal i.

The demonstrated system removal efficiency for chromium can be used to establish a mass feed rate limit for low volatility metals using the following equation:

$$\dot{m}_{g,in,max} = \frac{\dot{m}_{g,out,MACT}}{\left(1 - \frac{SRE_i}{100}\right)}$$

where:

$\dot{m}_{g,in,max}$ = maximum allowable mass feed rate of metal group g

$\dot{m}_{g,out,MACT}$ = maximum allowable mass emission rate of metal group g based on the MTEC analysis

SRE_i = demonstrated system removal efficiency of metal i designated to be the metal representative of metal group g.

7.0 EMISSIONS DATA TO SUPPORT THE SITE SPECIFIC RISK ASSESSMENT

Siemens Water Technologies Corp. collected emissions data to support the site specific risk assessment under “worst-case” conditions rather than conducting a separate “risk burn” under less aggressive “typical” conditions. Siemens Water Technologies Corp. therefore believes that the emissions presented represent conservative values which are higher than during typical operation. The following section presents the emission data and discusses interpretation of the data where appropriate.

7.1 DETECTION LIMITS

Method detection limits (MDLs) were determined for each of the stack gas analyses conducted. MDLs were determined statistically for non-isotope dilution methods following the requirements of 40 CFR Part 136, Appendix B. MDLs for isotope dilution methods were determined following the promulgated method requirements. Isotope dilution method MDLs were calculated based on 2.5 times the background noise. All reported MDLs, including condensate analyses, are matrix specific and reflect any dilutions, splits, or concentrations applied during the extraction or analysis of the samples. As such, laboratory-supplied MDL's for these stack gas analyses appear to meet the definition of sample quantitation limit (SQL) referenced in several sources of risk assessment guidance.

7.2 METALS

EPA Method 29 was used to sample stack gas multiple-metals emissions during the PDT. Metals emission data were collected in addition to the metals feed rate data, and are presented with the compliance data in Section 4.0. Emission results for the multiple-metals trains are repeated here in Tables 7-1 through 7-3. Mercury speciation data for the risk assessment are presented in Table 7-4.

A separate SW-846 Method 0061 sampling train was operated during each run of the PDT to determine the emission of hexavalent chromium. Sampling conditions and emission results for hexavalent chromium are presented in Tables 7-5 through 7-7.

7.3 HYDROGEN CHLORIDE AND CHLORINE

HCl and Cl₂ emissions were determined using EPA Method 26A during the PDT and are presented with the compliance results in Section 4.0. They are repeated here in Tables 7-8 through 7-10.

7.4 PARTICLE SIZE DISTRIBUTION

Particle size distribution data were collected using EPA Method 5 followed by scanning electron microscope evaluation of the particles collected on the filters. Particle size distribution results are presented in Table 7-11.

7.5 SPECIATED VOLATILE ORGANICS

Stack gas volatile organic samples were collected using SW-846 Method 0030, and analyzed for a list of target analytes, as specified in the PDT Plan, as well as for tentatively identified compounds (TICs). Sampling conditions and results are presented in Tables 7-12 through 7-14.

7.6 SPECIATED SEMIVOLATILE ORGANICS

An SW-846 Method 0010 sampling train was used to sample the stack gases for a list of target semivolatile organics, as specified in the PDT Plan, as well as for tentatively identified compounds (TICs). The sampling conditions and results are summarized in Tables 7-15 through 7-17.

7.7 TOTAL VOLATILE ORGANICS, SEMIVOLATILE ORGANICS, AND NONVOLATILE ORGANICS

Determination of these emissions was conducted according to the procedures presented in EPA/600/R-96/036, and are reported in three fractions:

- 1 Total volatile organics, expressed as total mass of C₁ through C₇ n-alkanes (Tables 7-18 through 7-20).
- 2 Total chromatographable organics (TCO), representing compounds with a boiling point range of 100°C to 300°C (Tables 7-21 through 7-23).
- 3 Total nonvolatile organics (GRAV), representing compounds with a boiling point above 300°C (Tables 7-21 through 7-23).

7.8 DIOXINS AND FURANS

Stack gases were sampled using SW-846 Method 0023A for PCDD/PCDF emissions during each PDT run. Analyses were performed to identify the total mass of the tetra- through octa-chlorinated PCDD and

PCDF congeners, as well as the mass of each individual 2,3,7,8-substituted PCDD and PCDF congener. In order to evaluate the potential risk posed by emissions of a variety of PCDD/PCDF compounds, each 2,3,7,8-substituted isomer is assigned a "toxic equivalence factor" which is used to equate the toxicity of that compound to the toxicity of 2,3,7,8-TCDD. A summary of the sampling conditions and emission results is provided with the compliance results in Section 4.0, and are repeated here as Tables 7-24 through 7-26. Analytical results for each of the 2,3,7,8-substituted PCDD and PCDF isomers, and their corresponding emissions, expressed as 2,3,7,8-TCDD toxic equivalents are presented in Tables 7-27 through 7-29.

7.9 SPECIATED PAHS

Polyaromatic hydrocarbons were analyzed on the same sampling train used for speciated semivolatile organic compound determinations. Analyses for PAHs followed CARB Method 429. Sampling conditions and emission results are presented in Tables 7-30 through 7-32.

7.10 POLYCHLORINATED BIPHENYLS (PCBS)

PCBs were analyzed on the same sampling train used for speciated semivolatile organic compound determinations. Analyses for PCBs followed EPA Method 1668. Sampling conditions and emission results are presented in Tables 7-33 through 7-35.

7.11 ORGANOCHLORINE PESTICIDES

Organochlorine pesticide compounds were sampled using SW-846 Method 0010. Sampling conditions and emission results are presented in Tables 7-36 through 7-38.

TABLES

Analytical Notation Legend

Notation	Meaning
B	Method blank contamination. The associated method blank contains the analyte at a reportable level.
C	Co-eluting isomer
COL	Greater than 40% RPD between primary and confirmatory column. Reported lower value.
E	Estimated – Exceeds calibration range
J	Estimated result. Result is less than the reporting limit.
M	Result measured against nearest internal standard, assuming a response factor of 1.
N	Estimated. Tentatively identified compound.
NA	Not analyzed or Not applicable
ND or U	Not detected
Q	Estimated maximum possible concentration (EMPC)

Table 1-1. Regulatory Compliance Performance and Emissions Summary

Parameter	Units	Test Objective	Run 1	Run 2	Run 3	Test Average
DRE - Chlorobenzene	%	> 99.99	> 99.9914	> 99.9970	99.9940	> 99.9941
DRE - Tetrachloroethene	%	> 99.99	> 99.9951	> 99.9982	> 99.9976	> 99.9970
Stack gas filterable particulate matter concentration (b)	mg/dscm	< 34	21	10	18	16
	(gr/dscf)	< 0.015	0.0090	0.0046	0.0079	0.0072
Stack gas PCDD/PCDF (b)	ng TEQ/dscm	< 0.40	0.065	0.052	0.062	0.060
Stack gas mercury (b)	ug/dscm	< 130	< 6.1	< 5.8	< 7.5	< 6.5
Stack gas semivolatile metals (Cd + Pb) concentration (b)	ug/dscm	< 240	210	130	360	230
Stack gas low volatility metals (As + Be + Cr) concentration (b)	ug/dscm	< 97	< 35	< 12	< 21	< 23
Stack gas HCl/Cl ₂ (b)	ppmv as HCl	< 77	5.4	3.2	3.0	3.9
Stack gas carbon monoxide concentration (b)	ppmv	< 100	11.5	10.4	15.6	12.5
Stack gas total hydrocarbon concentration (b)	ppmv, as propane	< 10	< 0.6	< 0.6	< 0.6	< 0.6
Stack gas oxygen concentration	vol%, dry	NA	9.8	8.9	9.3	9.3

- (a) Stack gas THC and O₂ data were obtained using Airtech's temporary CEMS.
- (b) Corrected to 7% oxygen, dry basis.

Note: Compliance with regulatory standards is based on the arithmetic average of the three test runs, except for DRE, where each run must meet the specified criteria [see 40 CFR 63.1206(b)(12)(ii)]. All values are reported to two significant figures.

Table 1-2. Summary of Process Operating Conditions ^a

Parameter	Units	PDT	Actual			
		Target	Run 1	Run 2	Run 3	Average
Spent carbon feed rate (1-min avg)	lb/hr	3000	3071	3022	3053	3049
Total chlorine/chloride feed rate	lb/hr	75 – 80	59.5	62.0	58.6	60.0
Mercury feed rate	lb/hr	3.0E-04	4.0E-05	4.2E-05	7.0E-05	5.1E-05
Total semivolatile metals feed rate (Cd+Pb)	lb/hr	1.1E-01	1.0E-01	1.0E-01	1.0E-01	1.0E-01
Total low volatility metals feed rate (As+Be+Cr)	lb/hr	3.9E-01	3.6E-01	3.8E-01	3.7E-01	3.7E-01
Monochlorobenzene feed rate	lb/hr	33 – 37	34.8	35.0	35.0	35.0
Tetrachloroethene feed rate	lb/hr	33 – 37	35.0	35.0	34.8	35.0
Organic surrogate mixture feed rate	lb/hr	40 – 42	40.9	40.9	40.7	40.8
Hearth #5 temperature	°F	1650	1650	1650	1650	1650
Afterburner temperature	°F	1750	1763	1767	1751	1760
Venturi scrubber pressure differential	in w.c.	≥ 15	19.2	17.7	18.0	18.3
Quench/venturi scrubber total liquid flow rate	gpm	70 – 75	74.6	77.0	73.2	74.9
Packed bed scrubber pH	pH	≥ 4	4.82	4.62	3.68	4.37
Packed bed scrubber liquid flow rate	gpm	≥ 60	63.6	63.1	62.9	63.2
Wet scrubber bowdown flow rate	gpm	60	59.8	57.2	56.9	58.0
WESP secondary voltage	kVDC	≥ 14	24.3	22.1	21.7	22.7
Stack gas flow rate	acfm	9,000	11,297	8,506	8,846	9,550
Stack gas carbon monoxide ^b	ppmv	≤ 100	11.5	10.4	15.6	12.5
Stack gas total hydrocarbons (as propane) ^c	ppmv	≤ 10	< 0.6	< 0.6	< 0.6	< 0.6
Stack gas oxygen ^d	vol %	NA	10.1	9.2	9.4	9.6

Note: HRA = Hourly rolling average.

(a) All values are averages. All but constituent feed rates and stack gas flow rates are taken from control room instruments. Spiking rates have been added to spent activated carbon feed rates, since spiking occurred downstream of the spent activated carbon mass feed rate measurement system. Stack gas flow rates are the average from all isokinetic sampling trains from each run. Stack gas flow monitor was not working properly during the test.

(b) 60-minute rolling average, corrected to 7% O₂, dry basis.

(c) Corrected to 7% O₂, dry basis.

(d) Dry basis.

Table 2-1. Summary of Planned Sampling Locations, Equipment, and Methods

Location ^a	Sample Name (Number)	Access	Equipment	Sample Size	General Procedure/Frequency	Reference Method ^b
1	Spent Activated Carbon (1-Volatiles) (1-Semivolatiles) (1 – Metals) (1 - Properties) (1-Archive)	Conveyor	Teflon scoop 4L glass jug, 250 ml jar (VOA) 1L glass bottles with teflon lined lids	1 scoop per grab; 250 ml volatiles 1L semivolatiles 1L properties 1L metals 1L archive	Collect a grab sample at each 15-minute interval during each test run. Grab samples will be combined in a glass jug to build run composite. Collect four 1-liter samples and one 250 ml VOA jar of the homogenized composite at the end of the test run.	SW-846, Vol. II, Chapter 9, Section 9.3
2	Makeup water (2-Volatiles) (1-Semivolatiles) (1 – Metals) (1-Archive)	Tap	40 ml vials; 4L glass jug, 1L glass bottles with teflon lined lids	40 ml VOA 1L semivolatiles 1L metals 1L archive	Collect one pair of 40 ml VOA vials at the beginning of the test; Fill 4L bottle at beginning of test. Fill three 1-liter samples from the 4L bottle.	SW-846, Vol. II, Chapter 9, Section 9.2
3	Caustic (2-Volatiles) (1-Semivolatiles) (1 – Metals) (1-Archive)	Tap	40 ml vials; 4L glass jug, 1L glass bottles with teflon lined lids	40 ml VOA 1L semivolatiles 1L metals 1L archive	Collect one pair of 40 ml VOA vials at the beginning of the test; Fill 4L bottle at beginning of test. Fill three 1-liter samples from the 4L bottle.	SW-846, Vol. II, Chapter 9, Section 9.2
4	Scrubber Blowdown (2-Volatiles) (1-Semivolatiles) (1 – Metals) (1-Archive)	Tap	40 ml vials; 4L glass jug, 1L glass bottles with teflon lined lids	40 ml VOA ~200 ml per grab; 1L semivolatiles 1L metals 1L archive	Collect one pair of 40 ml VOA vials at each 30 minute interval; Collect a ~200 ml grab sample at each 30-minute interval during each test run. Grab samples will be combined in a glass jug to build run composite. Collect three 1-liter samples of the homogenized composite at the end of the test run.	SW-846, Vol. II, Chapter 9, Section 9.2

Table 2-1. Summary of Planned Sampling Locations, Equipment, and Methods

Location ^a	Sample Name (Number)	Access	Equipment	Sample Size	General Procedure/Frequency	Reference Method ^b
5	POTW Discharge (2-Volatiles) (1-Semivolatiles) (1 – Metals) (1-Archive)	Tap	40 ml vials; 4L glass jug, 1L glass bottles with teflon lined lids	40 ml VOA ~200 ml per grab; 1L semivolatiles 1L metals 1L archive	Collect one pair of 40 ml VOA vials at each 30 minute interval; Collect a ~200 ml grab sample at each 30-minute interval during each test run. Grab samples will be combined in a glass jug to build run composite. Collect three 1-liter samples of the homogenized composite at the end of the test run.	SW-846, Vol. II, Chapter 9, Section 9.2
Stack (6)	Stack gas M29	Port	EPA Method 29 multiple metals sampling train	Minimum 120 minutes ^{c,d}	Collect integrated sample for metals and moisture. Measure stack gas velocity, pressure, and temperature. Collect bag samples or use CEM for oxygen and carbon dioxide.	EPA Methods 1 through 5, and 29.
Stack (6)	Stack gas M0061	Port	SW-846 Method 0061 hexavalent chromium sampling train	Minimum 120 minutes ^{c,d}	Collect integrated samples for hexavalent chromium and moisture. Measure stack gas velocity, pressure, and temperature. Collect bag samples or use CEM for oxygen and carbon dioxide.	EPA Methods 1 through 5; SW846-0061
Stack (6)	Stack gas M26A	Port	EPA Method 26A sampling train	Minimum 120 minutes ^{c,d}	Collect integrated sample for particulate, hydrogen chloride, and chlorine. Measure stack gas velocity, pressure, and temperature. Collect bag samples or use CEM for oxygen and carbon dioxide.	EPA Methods 1 through 5, and 26A
Stack (6)	Stack gas M0010-SV	Port	SW-846 Method 0010 sampling train	Minimum 3 dry standard cubic meters ^{c,d}	Collect integrated sample for semivolatile organics, organochlorine pesticides, and moisture. Measure stack gas velocity, pressure, and temperature. Collect bag samples or use CEM for oxygen and carbon dioxide.	EPA Methods 1 through 5; SW846-0010.

Table 2-1. Summary of Planned Sampling Locations, Equipment, and Methods

Location ^a	Sample Name (Number)	Access	Equipment	Sample Size	General Procedure/Frequency	Reference Method ^b
Stack (6)	Stack gas M0010-P	Port	Combined SW-846 Method 0010, EPA CARB Method 429 sampling train	Minimum 3 dry standard cubic meters ^{c,d}	Collect integrated sample for PAHs, PCBs, and moisture. Measure stack gas velocity, pressure, and temperature. Collect bag samples or use CEM for oxygen and carbon dioxide.	EPA Methods 1 through 5; SW846-0010; CARB Method 429.
Stack (6)	Stack gas M0010-TOE	Port	SW-846 Method 0010 sampling train	Minimum 3 dry standard cubic meters ^{c,d}	Collect integrated samples for total semivolatile organics, total nonvolatile organics, and moisture. Measure stack gas velocity, pressure, and temperature. Collect bag samples or use CEM for oxygen and carbon dioxide.	EPA Methods 1 through 5; SW846-0010; EPA TOE Guidance
Stack (6)	Stack gas M0023A	Port	SW-846 Method 0023A sampling train	Minimum 3 hours and 2.5 dry standard cubic meters ^{c,d}	Collect integrated sample for PCDD/PCDFs, and moisture. Measure stack gas velocity, pressure, and temperature. Collect bag samples or use CEM for oxygen and carbon dioxide.	EPA Methods 1 through 5; SW846-0023A.
Stack (6)	Stack gas M0030	Port	SW-846 Method 0030 volatile organic sampling train	4 tube pairs per run; 40 minutes per tube pair. Up to 20 liters of stack gas per tube pair	Collect four pairs of sorbent tubes and stack gas condensate for volatile organics during each run.	SW846-0030 (VOST)
Stack (6)	Stack gas M0040	Port	SW-846 Method 0040 sampling train	25 – 50 liters	Collect representative sample through a heated sample probe and filter; through a condenser and into a Tedlar bag. Transport dried sample and condensate to GC/FID.	EPA Methods 1 through 5; SW846-0040; EPA TOE Guidance.
Stack (6)	Stack gas PSD	Port	Cascade impactor	As required	Collect particle size distribution samples on multiple substrates	Cascade impactor mfr. instructions
Stack (6)	Stack gas CEMS	Port	Temporary CEMS THC	Continuous	Continuously monitor stack gas for total hydrocarbons during each run	EPA Method 25A

Table 2-1. Summary of Planned Sampling Locations, Equipment, and Methods

Location ^a	Sample Name (Number)	Access	Equipment	Sample Size	General Procedure/Frequency	Reference Method ^b
Stack (7)	Stack gas CEMS	Port	Installed CEMS CO	Continuous	Continuously monitor stack gas carbon monoxide during each run.	40 CFR 63 Subpart EEE Appendix; PS 4B
Stack (7)	Stack gas CEMS	Port	Installed CEMS O ₂	Continuous	Continuously monitor stack gas oxygen during each run.	40 CFR 63 Subpart EEE Appendix; PS 4B

- a Refer to Figure 2-1.
- b “SW846” refers to Test Methods for Evaluating Solid Waste, Third Edition, November 1986, and Updates.
 “EPA Method” refers to New Source Performance Standards, Test Methods and Procedures, Appendix A, 40 CFR 60.
 “CARB” refers to California Air Resources Board Methods.
 “PS 4B” refers to Performance Specification 4B, 40 CFR 60.
- c The exact volume of gas sampled will depend on the isokinetic sampling rate.
- d Isokinetic sampling trains include:
- Collecting one set of bag samples (or using CEM) for oxygen and carbon dioxide analysis to determine stack gas molecular weight (EPA Method 3)
 - Performing stack gas velocity, pressure, and temperature profile measurement for each sampling location (EPA Method 2)
 - Determining the moisture content of the stack gas for each sampling train (EPA Method 4)

Table 2-2. Summary of Planned Performance Test Analytical Procedures and Methods

Sample Name	Analysis	Samples per Run	Total Field Samples for Analysis	Preparation Method (See Note 1)	Analytical Method (See Note 1)
Spent Activated Carbon	Volatile Organics	1	3	Purge & Trap (SW846-5035)	GC/MS (SW846-8260)
	Organics	1	3	Solvent extraction (SW846-3542)	GC/MS (SW846-8270)
	Chloride	1	3	SW846-5050	Ion chromatography (SW846-9056)
	Total metals	1	3	Acid digestion (SW846-3050)	ICP (SW846-6020) & CVAAS (SW846-7470 for Hg)
Semivolatile	Elemental	1	3	NA	(ASTM D5373) with (ASTM D3176) as an alternate
Makeup Water	Volatile Organics	1	3	Purge & Trap (SW846-5035)	GC/MS (SW846-8260)
	Organics	1	3	Solvent extraction (SW846-3542)	GC/MS (SW846-8270)
	Total metals	1	3	Acid digestion (SW846-3020)	ICP (SW846-6020) & CVAAS (SW846-7470 for Hg)
Caustic	Volatile Organics	1	3	Purge & Trap (SW846-5035)	GC/MS (SW846-8260)
	Organics	1	3	Solvent extraction (SW846-3542)	GC/MS (SW846-8270)
	Total metals	1	3	Acid digestion (SW846-3020)	ICP (SW846-6020) & CVAAS (SW846-7470 for Hg)
Scrubber Blowdown	Volatile Organics	1	3	Purge & Trap (SW846-5035)	GC/MS (SW846-8260)
	Organics	1	3	Solvent extraction (SW846-3542)	GC/MS (SW846-8270)
	Total metals	1	3	Acid digestion (SW846-3020)	ICP (SW846-6020) & CVAAS (SW846-7470 for Hg)

Semivolatile

Table 2-2. Summary of Planned Performance Test Analytical Procedures and Methods

Sample Name	Analysis	Samples per Run	Total Field Samples for Analysis	Preparation Method (See Note 1)	Analytical Method (See Note 1)
POTW Discharge	Volatile Organics	1	3	Purge & Trap (SW846-5035)	GC/MS (SW846-8260)
	Organics	1	3	Solvent extraction (SW846-3542)	GC/MS (SW846-8270)
	Total metals	1	3	Acid digestion (SW846-3020)	ICP (SW846-6020) & CVAAS (SW846-7470 for Hg)
Stack gas M0030 Semivolatile	VOCs + TICs (tenax + tenax/charcoal tubes) (Note 2)	(Note 3)	(Note 3)	Thermal desorption, trap (SW846-5041A)	GC/MS (SW846-8260)
	VOCs + TICs (condensate) (Note 2)	1	3	Purge and trap	GC/MS (SW846-8260)
Stack gas M0040	Total VOCs	1	3	Purge and trap for condensate Direct injection for gas	GC/FID (Guidance for Total Organics, App. A and E)
Stack gas M0010-SV (low res analysis)	Semivolatile Organics & TICs (Note 4)	1	3	Solvent extraction (SW846-3542)	GC/MS (SW846-8270)
	OCP (Note 5)	1	3	Solvent extraction (SW846-3542)	GC (SW-846-8081)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Velocity	NA	NA	NA	Pitot tube (EPA Method 2)
	Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA	Orsat or CEM (EPA Method 3)

Table 2-2. Summary of Planned Performance Test Analytical Procedures and Methods

Sample Name	Analysis	Samples per Run	Total Field Samples for Analysis	Preparation Method (See Note 1)	Analytical Method (See Note 1)
Stack gas M0010-P (high res analysis)	PCB (Note 7)	1	3	Solvent extraction (SW846-3542)	GC/MS (EPA Method 1668)
	PAH (Note 8)	1	3	Solvent extraction (CARB 429)	GC/MS (CARB 429)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Velocity	NA	NA	NA	Pitot tube (EPA Method 2)
	Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA	Orsat or CEM (EPA Method 3)
Stack gas M0010-TOE	Total SVOCs	1	3	Solvent extraction (SW846-3542)	TOC GC/FID (Guidance for Total Organics, Appendix C)
	Total NVOCs	1	3	Solvent extraction (SW846-3542)	Gravimetric Method (Guidance for Total Organics, Appendix D)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Velocity	NA	NA	NA	Pitot tube (EPA Method 2)
	Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA	Orsat or CEM (EPA Method 3)
Stack gas M0023A	PCDD/PDCF	1	3	Solvent extraction (SW846-3500)	GC/MS (SW-846 Method 8290)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Velocity	NA	NA	NA	Pitot tube (EPA Method 2)
		Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA

Table 2-2. Summary of Planned Performance Test Analytical Procedures and Methods

Sample Name	Analysis	Samples per Run	Total Field Samples for Analysis	Preparation Method (See Note 1)	Analytical Method (See Note 1)
Stack gas M29	Metals (Note 9)	1	3	Acid digestion (SW846-3050)	ICP (SW846-6020) & CVAAS (SW846-7470 for Hg)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Velocity	NA	NA	NA	Pitot tube (EPA Method 2)
	Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA	Orsat or CEM (EPA Method 3)
Stack gas M0061	Hexavalent chromium	1	3	NA	Ion chromatography, post-column reactor (SW846-7199)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Velocity	NA	NA	NA	Pitot tube (EPA Method 2)
	Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA	Orsat or CEM (EPA Method 3)
Stack gas M26A	Hydrogen chloride/Chlorine	1	3	NA	Ion chromatography (SW846-9057)
	Particulate	1	1	NA	Gravimetric (EPA Method 5)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Velocity	NA	NA	NA	Pitot tube (EPA Method 2)
	Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA	Orsat or CEM (EPA Method 3)
Stack gas M00023A	PCDD/PCDF	1	3	Solvent extraction (SW846-8290)	GC/MS (SW846-8290; & SW846-0023A)
	Moisture	1	3	NA	Gravimetric (EPA Method 4)
	Temperature	1	3	NA	Thermocouple (EPA Method 2)
	Flow rate	NA	NA	NA	Pitot tube (EPA Method 2)
	Oxygen, Carbon dioxide	(Note 6)	(Note 6)	NA	Orsat or CEM (EPA Method 3)
Stack gas PSD	Particle size distribution	NA	NA	NA	Cascade impactor manufacturer's instructions

Table 2-2. Summary of Planned Performance Test Analytical Procedures and Methods

Sample Name	Analysis	Samples per Run	Total Field Samples for Analysis	Preparation Method (See Note 1)	Analytical Method (See Note 1)
Stack gas temporary CEMS	Total hydrocarbons	(Note 10)	(Note 10)	NA	Extractive Analyzers, EPA Method 25A
Stack gas Installed CEMs	Carbon Monoxide	(Note 10)	(Note 10)	NA	Extractive Analyzers, 40CFR 63 Appendix
	Oxygen	(Note 10)	(Note 10)	NA	Extractive Gas Analyzers, 40 CFR 63 Appendix

Note 1: "ASTM" refers to American Society for Testing and Materials, Annual Book of ASTM Standards, Annual Series.

"SW846" refers to Test Methods for Evaluating Solid Waste, Third Edition, November 1986, and updates.

"EPA Methods" (Methods 1 through 5 and 23) refer to New Source Performance Standards, Test Methods and Procedures,, App. A, 40CFR 60.

"CARB" refers to California Air Resources Board methodology adopted January 27, 1987.

"Guidance for Total Organics" refers to EPA/600/R-96/036, March, 1996.

Note 2: Volatile Target Compounds as listed in this Test Plan, plus tentatively identified compounds.

Note 3: During each sampling run, 4 pairs of VOST tubes (8 samples) will be collected, but only 3 pairs (6 samples) will be analyzed. The extra tube pair provides a contingency in case of breakage or other event that could require analysis of the extra tube pair. Analysis of each tube in each tube pair will be conducted separately.

Note 4: Semivolatile Target Compounds as listed in this Test Plan, plus tentatively identified compounds.

Note 5: Organochlorinated pesticide (OCP) target compounds as listed in this Test Plan.

Note 6: One set of gas bag samples collected during each stack traverse for Orsat analysis, or CEM.

Note 7: Polychlorinated Biphenyl (PCB) target compounds target compounds as listed in the Plan

Note:8 Polycyclic Aromatic Hydrocarbon (PAH) target compounds as listed in this Plan

Note 9: Metal Target Compounds as listed in this Test Plan.

Note 10: Installed CEMs sampling and analysis is continuous during each run.

Table 3-1. Process Operating Data Summary - Run 1^a

Parameter	Units	No. of Readings	Mean	Minimum	Maximum	Std. Dev.
Spent carbon feed rate (1-min avg)	lb/hr	274	3071	0	3555	706
Hearth #5 temperature	°F	274	1650	1649	1650	0.4
Afterburner temperature	°F	274	1763	1762	1764	0.5
Venturi scrubber pressure differential	in w.c.	274	19.2	17.3	19.9	0.8
Quench/venturi scrubber total liquid flow rate	gpm	274	74.6	74.3	74.8	0.1
Packed bed scrubber pH	pH	274	4.82	4.42	5.22	0.2
Packed bed scrubber liquid flow rate	gpm	274	63.6	63.2	63.9	0.2
Wet scrubber bowdown flow rate	gpm	274	59.8	58.0	61.8	1.0
WESP secondary voltage	kVDC	274	24.3	24.2	24.5	0.1
Stack gas flow rate	acfm	274	8626	8182	8894	204
Stack gas carbon monoxide ^b	ppmv	274	11.5	9.8	12.7	0.8
Stack gas oxygen (1-min avg) ^c	vol %	274	10.1	9.0	11.1	0.4

- a All values are taken from process instrument logs presented in Appendix A, and are 60-minute rolling averages, except as noted.
- b 60-minute rolling average, corrected to 7% O₂, dry basis.
- c Dry basis.

Table 3-2. Process Operating Data Summary - Run 2^a

Parameter	Units	No. of Readings	Mean	Minimum	Maximum	Std. Dev.
Spent carbon feed rate (1-min avg)	lb/hr	345	3022	47	3583	573
Hearth #5 temperature	°F	345	1650	1648	1652	0.6
Afterburner temperature	°F	345	1767	1765	1770	1.3
Venturi scrubber pressure differential	in w.c.	345	17.7	16.5	18.7	0.6
Quench/venturi scrubber total liquid flow rate	gpm	345	77.0	76.7	77.7	0.4
Packed bed scrubber pH	pH	345	4.62	4.23	4.98	0.2
Packed bed scrubber liquid flow rate	gpm	345	63.1	62.9	63.2	0.1
Wet scrubber bowdown flow rate	gpm	345	57.2	56.6	58.6	0.4
WESP secondary voltage	kVDC	345	22.1	21.8	22.3	0.1
Stack gas flow rate	acfm	345	7101	6935	7415	128
Stack gas carbon monoxide ^b	ppmv	345	10.4	8.3	12.9	1.3
Stack gas oxygen (1-min avg) ^c	vol %	345	9.2	8.6	10.7	0.4

- a All values are taken from process instrument logs presented in Appendix A, and are 60-minute rolling averages, except as noted.
- b 60-minute rolling average, corrected to 7% O₂, dry basis.
- c Dry basis.

Table 3-3. Process Operating Data Summary - Run 3^a

Parameter	Units	No. of Readings	Mean	Minimum	Maximum	Std. Dev.
Spent carbon feed rate (1-min avg)	lb/hr	275	3053	109	4211	744
Hearth #5 temperature	°F	275	1650	1648	1652	0.8
Afterburner temperature	°F	275	1751	1750	1754	0.6
Venturi scrubber pressure differential	in w.c.	275	18.0	17.3	19.2	0.5
Quench/venturi scrubber total liquid flow rate	gpm	275	73.2	72.4	75.9	0.7
Packed bed scrubber pH	pH	275	3.68	3.46	4.16	0.2
Packed bed scrubber liquid flow rate	gpm	275	62.9	62.7	63.9	0.2
Wet scrubber bowdown flow rate	gpm	275	56.9	55.4	58.5	0.7
WESP secondary voltage	kVDC	275	21.7	21.3	22.8	0.4
Stack gas flow rate	acfm	275	7049	6832	7380	109
Stack gas carbon monoxide ^b	ppmv	275	15.6	12.0	19.5	1.7
Stack gas oxygen (1-min avg) ^c	vol %	275	9.4	7.6	10.9	0.6

- a All values are taken from process instrument logs presented in Appendix A, and are 60-minute rolling averages, except as noted.
- b 60-minute rolling average, corrected to 7% O₂, dry basis.
- c Dry basis.

Table 3-4. Feed Material Physical/Chemical Characteristics

Characteristics	Units	Spent Activated Carbon			
		Run 1	Run 2	Run 3	Average
Carbon content	wt%	61.3	67.6	60.2	63.0
Hydrogen content ^a	wt%	4.1	2.9	3.9	3.6
Oxygen content ^a	wt%	33.9	28.8	35.2	32.6
Nitrogen content	wt%	< 0.5	< 0.5	< 0.5	< 0.5
Sulfur content	wt%	< 0.2	< 0.2	< 0.2	< 0.2

(a) Hydrogen and oxygen content includes moisture. Oxygen determined by difference. Oxygen could not be analyzed due to a matrix interference.

Table 3-5. Feed Composition and Constituent Feed Rates (Chloride, Metals, POHCs)

Stream Name	Feed Rate (lb/hr)			
	Run 1	Run 2	Run 3	Average
Spent Activated Carbon	3071	3022	3053	3049
Monochlorobenzene Spike	34.82	35.05	35.05	34.97
Tetrachloroethene Spike	35.05	35.03	34.85	34.98
Lead Spike	19.83	20.15	19.88	19.95
Chrome Spike	19.83	20.15	19.88	19.95
Organic Surrogate Mixture Spike	40.87	40.88	40.73	40.83

Table 3-5. Feed Composition and Constituent Feed Rates (Chloride, Metals, POHCs), continued

		Analytical Result								
Properties/Constituents	Units	Spent Activated Carbon			Monochlorobenzene Spike			Tetrachloroethene Spike		
		Run 1	Run 2	Run 3	Run 1	Run 2	Run 3	Run 1	Run 2	Run 3
Chlorine/chloride	mg/kg	3860 J	4740 J	3650 J	315548	315548	315548	855199	855199	855199
Metals										
Aluminum	mg/kg	4.33E+02	8.32E+02	7.85E+02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Antimony	mg/kg	6.00E+00 ND	6.00E+00 ND	6.00E+00 ND	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Arsenic	mg/kg	1.40E+00 B	1.40E+00 B	1.60E+00 B	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Barium	mg/kg	2.11E+01	3.50E+01	3.73E+01	0.00E+00	0.00E+01	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Beryllium	mg/kg	2.20E-01 B	4.20E-01 B	5.40E-01 B	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cadmium	mg/kg	1.60E-01 B	1.40E-01 B	2.40E-01 B	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Chromium	mg/kg	3.70E+00	5.90E+00	5.70E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cobalt	mg/kg	1.60E+00 B	1.80E+00 B	2.00E+00 B	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Copper	mg/kg	1.11E+01	1.74E+01	1.24E+01	0.00E+01	0.00E+01	0.00E+01	0.00E+00	0.00E+00	0.00E+00
Lead	mg/kg	7.50E-01 B	8.80E-01 B	1.10E+00 B	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Manganese	mg/kg	2.78E+02	2.70E+02	1.79E+02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mercury	mg/kg	1.30E-02 B	1.40E-02 B	2.30E-02 B	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nickel	mg/kg	9.50E+00	5.08E+01	2.89E+01	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Selenium	mg/kg	6.10E-01 B	5.50E-01 B	4.80E-01 B	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Silver	mg/kg	3.00E+00 ND	3.00E+00 ND	3.00E+00 ND	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Thallium	mg/kg	3.50E+00 ND	3.50E+00 ND	3.50E+00 ND	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Vanadium	mg/kg	2.70E+00	2.90E+00	6.20E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Zinc	mg/kg	1.44E+01 J	1.68E+01 J	1.68E+01 J	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
POHCs										
Monochlorobenzene	mg/kg	0	0	0	999976	999976	999976	0	0	0
Tetrachloroethene	mg/kg	0	0	0	0	0	0	999740	999740	999740

		Analytical Result								
Properties/Constituents	Units	Lead Spike			Chrome Spike			Organic Surrogate Mixture Spike		
		Run 1	Run 2	Run 3	Run 1	Run 2	Run 3	Run 1	Run 2	Run 3
Chlorine/chloride	mg/kg	0	0	0	0	0	0	162966	162966	162966
Metals										
Aluminum	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Antimony	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Arsenic	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Barium	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Beryllium	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cadmium	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Chromium	mg/kg	0.00E+00	0.00E+00	0.00E+00	1.75E+04	1.75E+04	1.75E+04	0.00E+00	0.00E+00	0.00E+00
Cobalt	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Copper	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Lead	mg/kg	5.00E+03	5.00E+03	5.00E+03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Manganese	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mercury	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nickel	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Selenium	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Silver	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Thallium	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Vanadium	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Zinc	mg/kg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
POHCs										
Monochlorobenzene	mg/kg	0	0	0	0	0	0	0	0	0
Tetrachloroethene	mg/kg	0	0	0	0	0	0	0	0	0

Table 3-5. Feed Composition and Constituent Feed Rates (Chloride, Metals, POHCs), continued

	Resultant Feed Rates (lb/hr)											
	Spent Activated Carbon				Monochlorobenzene Spike				Tetrachloroethene Spike			
	Run 1	Run 2	Run 3	Average	Run 1	Run 2	Run 3	Average	Run 1	Run 2	Run 3	Average
Chlorine/chloride	1.19E+01	1.43E+01	1.11E+01	1.24E+01	1.10E+01	1.11E+01	1.11E+01	1.10E+01	3.00E+01	3.00E+01	2.98E+01	2.99E+01
Metals												
Aluminum	1.33E+00	2.51E+00	2.40E+00	2.08E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Antimony	< 1.84E-02	< 1.81E-02	< 1.83E-02	1.83E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Arsenic	4.30E-03	4.23E-03	4.88E-03	4.47E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Barium	6.48E-02	1.06E-01	1.14E-01	9.48E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Beryllium	6.76E-04	1.27E-03	1.65E-03	1.20E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cadmium	4.91E-04	4.23E-04	7.33E-04	5.49E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Chromium	1.14E-02	1.78E-02	1.74E-02	1.55E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cobalt	4.91E-03	5.44E-03	6.11E-03	5.49E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Copper	3.41E-02	5.26E-02	3.79E-02	4.15E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Lead	2.30E-03	2.66E-03	3.36E-03	2.77E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Manganese	8.54E-01	8.16E-01	5.46E-01	7.39E-01	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mercury	3.99E-05	4.23E-05	7.02E-05	5.08E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nickel	2.92E-02	1.54E-01	8.82E-02	9.03E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Selenium	1.87E-03	1.66E-03	1.47E-03	1.67E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Silver	< 9.21E-03	< 9.07E-03	< 9.16E-03	9.15E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Thallium	< 1.07E-02	< 1.06E-02	< 1.07E-02	1.07E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Vanadium	8.29E-03	8.76E-03	1.89E-02	1.20E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Zinc	4.42E-02	5.08E-02	5.13E-02	4.88E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
POHCs												
Monochlorobenzene	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.48E+01	3.50E+01	3.50E+01	3.50E+01	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Tetrachloroethene	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.50E+01	3.50E+01	3.48E+01	3.50E+01

	Resultant Feed Rates (lb/hr)											
	Lead Spike				Chrome Spike				Organic Surrogate Mixture Spike			
	Run 1	Run 2	Run 3	Average	Run 1	Run 2	Run 3	Average	Run 1	Run 2	Run 3	Average
Chlorine/chloride	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	6.66E+00	6.66E+00	6.64E+00	6.65E+00
Metals												
Aluminum	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Antimony	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Arsenic	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Barium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Beryllium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cadmium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Chromium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	3.48E-01	3.53E-01	3.48E-01	3.50E-01	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cobalt	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Copper	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Lead	9.91E-02	1.01E-01	9.94E-02	9.97E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Manganese	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mercury	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nickel	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Selenium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Silver	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Thallium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Vanadium	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Zinc	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
POHCs												
Monochlorobenzene	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Tetrachloroethene	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00

Table 3-5. Feed Composition and Constituent Feed Rates (Chloride, Metals, POHCs), continued

Resultant Feed Rates (lb/hr)				
	Grand Total			
	Run 1	Run 2	Run 3	Average
Chlorine/chloride	5.95E+01	6.20E+01	5.86E+01	6.00E+01
Metals				
Aluminum	1.33E+00	2.51E+00	2.40E+00	2.08E+00
Antimony	1.84E-02	1.81E-02	1.83E-02	1.83E-02
Arsenic	4.30E-03	4.23E-03	4.88E-03	4.47E-03
Barium	6.48E-02	1.06E-01	1.14E-01	9.48E-02
Beryllium	6.76E-04	1.27E-03	1.65E-03	1.20E-03
Cadmium	4.91E-04	4.23E-04	7.33E-04	5.49E-04
Chromium	3.59E-01	3.71E-01	3.66E-01	3.65E-01
Cobalt	4.91E-03	5.44E-03	6.11E-03	5.49E-03
Copper	3.41E-02	5.26E-02	3.79E-02	4.15E-02
Lead	1.01E-01	1.03E-01	1.03E-01	1.03E-01
Manganese	8.54E-01	8.16E-01	5.46E-01	7.39E-01
Mercury	3.99E-05	4.23E-05	7.02E-05	5.08E-05
Nickel	2.92E-02	1.54E-01	8.82E-02	9.03E-02
Selenium	1.87E-03	1.66E-03	1.47E-03	1.67E-03
Silver	9.21E-03	9.07E-03	9.16E-03	9.15E-03
Thallium	1.07E-02	1.06E-02	1.07E-02	1.07E-02
Vanadium	8.29E-03	8.76E-03	1.89E-02	1.20E-02
Zinc	4.42E-02	5.08E-02	5.13E-02	4.88E-02
POHCs				
Monochlorobenzene	3.48E+01	3.50E+01	3.50E+01	3.50E+01
Tetrachloroethene	3.50E+01	3.50E+01	3.48E+01	3.50E+01
Metal Volatility Groups				
SVM	1.02E-01	1.04E-01	1.03E-01	1.03E-01
LVM	3.64E-01	3.77E-01	3.72E-01	3.71E-01

Note: If not detected, metals, ash, and chlorine are considered to be present at their detection limit, for purposes of determining constituent feed rate.

Table 3-6. Waste Feed Volatile Organic Compound Concentration

Constituent	Units	Spent Activated Carbon Feed			
		Run 1	Run 2	Run 3	Average
Acetone	ug/kg	3.50E+03	3.60E+03	2.40E+03	3.17E+03
Acrylonitrile	ug/kg	< 3.80E+03	< 3.80E+03	< 3.80E+03	< 3.80E+03
Benzene	ug/kg	3.80E+03	1.70E+03	1.00E+03	2.17E+03
Bromobenzene	ug/kg	< 2.60E+02	< 2.60E+02	< 2.60E+02	< 2.60E+02
Bromochloromethane	ug/kg	< 1.70E+02	< 1.70E+02	< 1.70E+02	< 1.70E+02
Bromodichloromethane	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
Bromoform	ug/kg	< 2.10E+02	< 2.10E+02	< 2.10E+02	< 2.10E+02
Bromomethane	ug/kg	7.40E+02	7.50E+02	< 1.70E+02	< 5.53E+02
2-Butanone (MEK)	ug/kg	1.40E+04	3.20E+03	1.20E+03	6.13E+03
n-Butylbenzene	ug/kg	< 3.80E+02	< 3.80E+02	< 3.80E+02	< 3.80E+02
sec-Butylbenzene	ug/kg	< 3.80E+02	< 3.80E+02	< 3.80E+02	< 3.80E+02
tert-Butylbenzene	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
Carbon disulfide	ug/kg	< 1.50E+02	< 1.50E+02	< 1.50E+02	< 1.50E+02
Carbon tetrachloride	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
Chlorobenzene	ug/kg	< 1.30E+02	< 1.30E+02	< 1.30E+02	< 1.30E+02
Chlorodibromomethane	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
Chloroethane	ug/kg	< 2.80E+02	< 2.80E+02	< 2.80E+02	< 2.80E+02
Chloroform	ug/kg	1.90E+03	1.30E+03	1.10E+03	1.43E+03
Chloromethane	ug/kg	< 1.00E+03	2.30E+03	< 1.00E+03	< 1.43E+03
2-Chlorotoluene	ug/kg	< 3.00E+02	< 3.00E+02	< 3.00E+02	< 3.00E+02
4-Chlorotoluene	ug/kg	< 3.00E+02	< 3.00E+02	< 3.00E+02	< 3.00E+02
1,2-Dibromo-3-chloropropane	ug/kg	< 1.40E+02	< 1.40E+02	< 1.40E+02	< 1.40E+02
1,2-Dibromoethane	ug/kg	< 1.80E+02	< 1.80E+02	< 1.80E+02	< 1.80E+02
Dibromomethane	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
1,2-Dichlorobenzene	ug/kg	< 3.20E+02	< 3.20E+02	< 3.20E+02	< 3.20E+02
1,3-Dichlorobenzene	ug/kg	< 3.30E+02	< 3.30E+02	< 3.30E+02	< 3.30E+02
1,4-Dichlorobenzene	ug/kg	< 3.30E+02	< 3.30E+02	< 3.30E+02	< 3.30E+02
Dichlorodifluoromethane	ug/kg	< 1.60E+02	< 1.60E+02	< 1.60E+02	< 1.60E+02
1,1-Dichloroethane	ug/kg	1.50E+02	3.60E+02	2.60E+02	2.57E+02
1,2-Dichloroethane	ug/kg	6.00E+02	1.50E+02	2.10E+02	3.20E+02
cis-1,2-Dichloroethene	ug/kg	3.20E+02	1.70E+02	1.50E+02	2.13E+02
trans-1,2-Dichloroethene	ug/kg	< 1.90E+02	< 1.90E+02	< 1.90E+02	< 1.90E+02
1,1-Dichloroethene	ug/kg	5.00E+02	6.70E+02	8.40E+02	6.70E+02
1,2-Dichloropropane	ug/kg	< 1.80E+02	< 1.80E+02	< 1.80E+02	< 1.80E+02
1,3-Dichloropropane	ug/kg	< 2.20E+02	< 2.20E+02	< 2.20E+02	< 2.20E+02
2,2-Dichloropropane	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
cis-1,3-Dichloropropene	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
trans-1,3-Dichloropropene	ug/kg	< 1.50E+02	< 1.50E+02	< 1.50E+02	< 1.50E+02
1,1-Dichloropropene	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
Ethylbenzene	ug/kg	< 2.40E+02	< 2.40E+02	< 2.40E+02	< 2.40E+02
Hexachlorobutadiene	ug/kg	< 5.50E+02	< 5.50E+02	< 5.50E+02	< 5.50E+02
2-Hexanone	ug/kg	< 8.00E+02	< 8.00E+02	< 8.00E+02	< 8.00E+02
Iodomethane	ug/kg	5.50E+02	5.50E+02	5.50E+02	5.50E+02
Isopropylbenzene	ug/kg	< 2.80E+02	< 2.80E+02	< 2.80E+02	< 2.80E+02
p-Isopropyltoluene	ug/kg	< 4.20E+02	< 4.20E+02	< 4.20E+02	< 4.20E+02
Methylene chloride	ug/kg	< 4.20E+02	< 4.20E+02	< 4.20E+02	< 4.20E+02
4-Methyl-2-pentanone	ug/kg	< 8.00E+02	< 8.00E+02	< 8.00E+02	< 8.00E+02
Naphthalene	ug/kg	< 2.40E+02	< 2.40E+02	6.00E+02	< 3.60E+02
n-Propylbenzene	ug/kg	< 3.60E+02	< 3.60E+02	< 3.60E+02	< 3.60E+02
Styrene	ug/kg	< 2.40E+02	< 2.40E+02	< 2.40E+02	< 2.40E+02
1,1,1,2-Tetrachloroethane	ug/kg	< 1.60E+02	< 1.60E+02	< 1.60E+02	< 1.60E+02
1,1,1,2,2-Tetrachloroethane	ug/kg	< 2.10E+02	< 2.10E+02	< 2.10E+02	< 2.10E+02
Tetrachloroethene	ug/kg	1.60E+03	2.30E+03	1.10E+03	1.67E+03
Tetrahydrofuran	ug/kg	2.70E+03	1.10E+03	< 1.00E+03	< 1.60E+03
Toluene	ug/kg	3.20E+02	7.70E+02	2.10E+02	4.33E+02
1,2,3-Trichlorobenzene	ug/kg	< 3.60E+02	< 3.60E+02	< 3.60E+02	< 3.60E+02
1,2,4-Trichlorobenzene	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
1,1,1-Trichloroethane	ug/kg	5.60E+03	1.40E+04	1.10E+04	1.02E+04
1,1,2-Trichloroethane	ug/kg	< 1.80E+02	< 1.80E+02	< 1.80E+02	< 1.80E+02
Trichloroethene	ug/kg	4.30E+04	3.20E+04	2.00E+04	3.17E+04
Trichlorofluoromethane	ug/kg	< 3.20E+02	< 3.20E+02	< 3.20E+02	< 3.20E+02
1,2,3-Trichloropropane	ug/kg	< 2.70E+02	< 2.70E+02	< 2.70E+02	< 2.70E+02
1,1,2-Trichloro-1,2,2-trifluoroethane	ug/kg	1.70E+03	1.60E+03	1.10E+03	1.47E+03
1,2,4-Trimethylbenzene	ug/kg	< 3.20E+02	< 3.20E+02	< 3.20E+02	< 3.20E+02
1,2,5-Trimethylbenzene	ug/kg	< 3.10E+02	< 3.10E+02	< 3.10E+02	< 3.10E+02
Vinyl acetate	ug/kg	< 6.00E+02	< 6.00E+02	< 6.00E+02	< 6.00E+02
Vinyl chloride	ug/kg	< 1.40E+02	< 1.40E+02	< 1.40E+02	< 1.40E+02
m- & p- Xylene	ug/kg	< 4.80E+02	< 4.80E+02	< 4.80E+02	< 4.80E+02
o-Xylene	ug/kg	< 2.10E+02	< 2.10E+02	< 2.10E+02	< 2.10E+02
Total xylenes	ug/kg	< 7.00E+02	< 7.00E+02	< 7.00E+02	< 7.00E+02

Table 3-7. Waste Feed Semivolatile Organic Compound Concentration

Constituent	Units	Spent Activated Carbon Feed			
		Run 1	Run 2	Run 3	Average
Acenaphthene	ug/kg	5.70E+02	5.60E+02	7.80E+02	6.37E+02
Acenaphthylene	ug/kg	1.30E+03	1.20E+03	1.60E+03	1.37E+03
Aniline	ug/kg	< 1.60E+02	< 1.60E+02	< 1.60E+02	< 1.60E+02
Anthracene	ug/kg	2.00E+02	2.40E+02	2.40E+02	2.27E+02
Benz(a)anthracene	ug/kg	< 1.00E+02	< 1.00E+02	< 1.00E+02	< 1.00E+02
Benzidine	ug/kg	< 4.20E+03	< 4.20E+03	< 4.20E+03	< 4.20E+03
Benzo(b)fluoranthene	ug/kg	< 2.60E+02	< 2.60E+02	< 2.60E+02	< 2.60E+02
Benzo(k)fluoranthene	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
Benzoic acid	ug/kg	< 8.50E+02	< 8.50E+02	< 8.50E+02	< 8.50E+02
Benzo(g,h,i)perylene	ug/kg	< 1.00E+02	< 1.00E+02	< 1.00E+02	< 1.00E+02
Benzo(a)pyrene	ug/kg	< 2.00E+02	< 2.00E+02	< 2.00E+02	< 2.00E+02
Benzyl alcohol	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
bis(2-Chloroethoxy)methane	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
bis(2-Chloroethyl)ether	ug/kg	< 9.50E+01	< 9.50E+01	< 9.50E+01	< 9.50E+01
bis(2-Ethylhexyl)phthalate	ug/kg	< 3.20E+02	< 3.20E+02	4.10E+02	< 3.50E+02
4-Bromophenyl-phenylether	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
Butyl benzyl phthalate	ug/kg	< 1.40E+02	< 1.40E+02	< 1.40E+02	< 1.40E+02
Carbazole	ug/kg	< 1.40E+02	< 1.40E+02	< 1.40E+02	< 1.40E+02
4-Chloroaniline	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
4-Chloro-3-Methylphenol	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
2-Chloronaphthalene	ug/kg	< 9.50E+01	< 9.50E+01	< 9.50E+01	< 9.50E+01
2-Chlorophenol	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
4-Chlorophenyl-phenylether	ug/kg	< 1.30E+02	< 1.30E+02	< 1.30E+02	< 1.30E+02
Chrysene	ug/kg	< 1.00E+02	< 1.00E+02	< 1.00E+02	< 1.00E+02
Dibenz(a,h)anthracene	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
Dibenzofuran	ug/kg	< 1.10E+02	< 1.10E+02	< 1.10E+02	< 1.10E+02
Di-n-butylphthalate	ug/kg	< 1.60E+02	< 1.60E+02	< 1.60E+02	< 1.60E+02
1,2-Dichlorobenzene	ug/kg	2.60E+04	2.30E+04	2.70E+04	2.53E+04
1,3-Dichlorobenzene	ug/kg	< 8.50E+01	< 8.50E+01	< 8.50E+01	< 8.50E+01
1,4-Dichlorobenzene	ug/kg	1.90E+03	1.70E+03	2.10E+03	1.90E+03
3,3'-Dichlorobenzidine	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
2,4-Dichlorophenol	ug/kg	< 9.50E+01	< 9.50E+01	< 9.50E+01	< 9.50E+01
Diethylphthalate	ug/kg	< 8.50E+01	< 8.50E+01	< 8.50E+01	< 8.50E+01
2,4-Dimethylphenol	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
Dimethylphthalate	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
1,3-Dinitrobenzene	ug/kg	< 9.50E+01	< 9.50E+01	< 9.50E+01	< 9.50E+01
4,6-Dinitro-2-methylphenol	ug/kg	< 8.50E+02	< 8.50E+02	< 8.50E+02	< 8.50E+02
2,4-Dinitrophenol	ug/kg	< 8.00E+02	< 8.00E+02	< 8.00E+02	< 8.00E+02
2,4-Dinitrotoluene	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
2,6-Dinitrotoluene	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
Di-n-octyl phthalate	ug/kg	< 1.50E+02	< 1.50E+02	< 1.50E+02	< 1.50E+02
Diphenylamine	ug/kg	< 1.50E+02	< 1.50E+02	< 1.50E+02	< 1.50E+02
1,2-Diphenylhydrazine	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
Fluoranthene	ug/kg	1.40E+02	1.60E+02	1.30E+02	1.43E+02
Fluorene	ug/kg	7.30E+02	7.10E+02	1.00E+03	8.13E+02
Hexachlorobenzene	ug/kg	< 9.00E+01	< 9.00E+01	< 9.00E+01	< 9.00E+01
Hexachlorobutadiene	ug/kg	< 8.50E+01	< 8.50E+01	< 8.50E+01	< 8.50E+01
Hexachlorocyclopentadiene	ug/kg	< 8.50E+02	< 8.50E+02	< 8.50E+02	< 8.50E+02
Hexachloroethane	ug/kg	< 1.10E+02	< 1.10E+02	< 1.10E+02	< 1.10E+02
Indeno(1,2,3-c,d)pyrene	ug/kg	< 9.00E+01	< 9.00E+01	< 9.00E+01	< 9.00E+01
Isophorone	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
2-Methylnaphthalene	ug/kg	7.70E+03	7.60E+03	1.10E+04	8.77E+03
2-Methylphenol	ug/kg	< 1.00E+02	< 1.00E+02	< 1.00E+02	< 1.00E+02
3 & 4-Methylphenol	ug/kg	< 2.20E+02	3.10E+02	< 2.20E+02	< 2.50E+02
Naphthalene	ug/kg	6.50E+03	5.90E+03	8.70E+03	7.03E+03
2-Nitroaniline	ug/kg	< 1.60E+02	< 1.60E+02	< 1.60E+02	< 1.60E+02
3-Nitroaniline	ug/kg	< 9.50E+01	< 9.50E+01	< 9.50E+01	< 9.50E+01
4-Nitroaniline	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
Nitrobenzene	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
2-Nitrophenol	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
4-Nitrophenol	ug/kg	< 8.50E+02	< 8.50E+02	< 8.50E+02	< 8.50E+02
N-Nitrosodimethylamine	ug/kg	< 8.50E+01	< 8.50E+01	< 8.50E+01	< 8.50E+01
N-Nitrosodiphenylamine	ug/kg	< 1.20E+02	< 1.20E+02	< 1.20E+02	< 1.20E+02
N-Nitroso-di-n-propylamine	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
Pentachlorophenol	ug/kg	< 8.50E+02	< 8.50E+02	< 8.50E+02	< 8.50E+02
Phenanthrene	ug/kg	9.20E+02	1.00E+03	1.10E+03	1.01E+03
Phenol	ug/kg	2.00E+03	7.10E+02	4.50E+02	1.05E+03
2,2'-oxybis(1-Chloropropane)	ug/kg	< 8.50E+01	< 8.50E+01	< 8.50E+01	< 8.50E+01
Pyrene	ug/kg	2.10E+02	2.50E+02	2.20E+02	2.27E+02
Pyridine	ug/kg	< 8.50E+01	< 8.50E+01	< 8.50E+01	< 8.50E+01
1,2,4-Trichlorobenzene	ug/kg	2.00E+03	2.00E+03	3.00E+03	2.33E+03
2,4,5-Trichlorophenol	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02
2,4,6-Trichlorophenol	ug/kg	< 3.40E+02	< 3.40E+02	< 3.40E+02	< 3.40E+02

Table 3-8. Summary of Spiking Materials and Rates

Run 1						
Constituent	Compound	Constituent	Spike Material wt % Constituent	Spike Material Feed Rate (lb/hr)	Constituent Feed Rate (lb/hr)	Constituent Feed Rate (g/hr)
Lead	Pb(NO ₃) ₂	Pb	0.4998%	19.83	9.91E-02	4.50E+01
Chromium	Cr(NO ₃) ₃ · 9H ₂ O	Cr	1.753%	19.83	3.48E-01	1.58E+02
Monochlorobenzene	C ₆ H ₅ Cl	C ₆ H ₅ Cl	99.9976%	34.82	34.82	1.58E+04
Tetrachloroethene	C ₂ Cl ₄	C ₂ Cl ₄	99.974%	35.05	35.04	1.59E+04
Organic Surrogate Mixture						
Methylene chloride	CH ₂ Cl ₂	CH ₂ Cl ₂	19.51%	40.87	7.97	3.62E+03
Ethylene glycol	C ₂ H ₆ O ₂	C ₂ H ₆ O ₂	19.51%	40.87	7.97	3.62E+03
Toluene	C ₆ H ₅ CH ₃	C ₆ H ₅ CH ₃	41.44%	40.87	16.94	7.68E+03
Naphthalene	C ₁₀ H ₈	C ₁₀ H ₈	19.50%	40.87	7.97	3.62E+03

Run 2						
Constituent	Compound	Constituent	Spike Material wt % Constituent	Spike Material Feed Rate (lb/hr)	Constituent Feed Rate (lb/hr)	Constituent Feed Rate (g/hr)
Lead	Pb(NO ₃) ₂	Pb	0.4998%	20.15	1.01E-01	4.57E+01
Chromium	Cr(NO ₃) ₃ · 9H ₂ O	Cr	1.753%	20.15	3.53E-01	1.60E+02
Monochlorobenzene	C ₆ H ₅ Cl	C ₆ H ₅ Cl	99.9976%	35.05	35.05	1.59E+04
Tetrachloroethene	C ₂ Cl ₄	C ₂ Cl ₄	99.974%	35.03	35.02	1.59E+04
Organic Surrogate Mixture						
Methylene chloride	CH ₂ Cl ₂	CH ₂ Cl ₂	19.51%	40.88	7.98	3.62E+03
Ethylene glycol	C ₂ H ₆ O ₂	C ₂ H ₆ O ₂	19.51%	40.88	7.98	3.62E+03
Toluene	C ₆ H ₅ CH ₃	C ₆ H ₅ CH ₃	41.44%	40.88	16.94	7.68E+03
Naphthalene	C ₁₀ H ₈	C ₁₀ H ₈	19.50%	40.88	7.97	3.62E+03

Run 3						
Constituent	Compound	Constituent	Spike Material wt % Constituent	Spike Material Feed Rate (lb/hr)	Constituent Feed Rate (lb/hr)	Constituent Feed Rate (g/hr)
Lead	Pb(NO ₃) ₂	Pb	0.4998%	19.88	9.94E-02	4.51E+01
Chromium	Cr(NO ₃) ₃ · 9H ₂ O	Cr	1.753%	19.88	3.48E-01	1.58E+02
Monochlorobenzene	C ₆ H ₅ Cl	C ₆ H ₅ Cl	99.9976%	35.05	35.05	1.59E+04
Tetrachloroethene	C ₂ Cl ₄	C ₂ Cl ₄	99.974%	34.86	34.85	1.58E+04
Organic Surrogate Mixture						
Methylene chloride	CH ₂ Cl ₂	CH ₂ Cl ₂	19.51%	40.73	7.95	3.60E+03
Ethylene glycol	C ₂ H ₆ O ₂	C ₂ H ₆ O ₂	19.51%	40.73	7.95	3.60E+03
Toluene	C ₆ H ₅ CH ₃	C ₆ H ₅ CH ₃	41.44%	40.73	16.88	7.66E+03
Naphthalene	C ₁₀ H ₈	C ₁₀ H ₈	19.50%	40.73	7.94	3.60E+03

Table 3-9. Makeup Water, Caustic, and Scrubber Purge POHC Concentration

Constituent	Makeup Water (ug/L)				Caustic (ug/L)				Scrubber Blowdown (ug/L)				POTW Discharge (ug/L)			
	Run 1	Run 2	Run 3	Average	Run 1	Run 2	Run 3	Average	Run 1	Run 2	Run 3	Average	Run 1	Run 2	Run 3	Average
Metals																
Aluminum	< 1.10E+02	< 1.10E+02	< 1.10E+02	< 1.10E+02	< 4.40E+02	NA	NA	< 4.40E+02	1.37E+04	1.17E+04	1.76E+04	1.43E+04	1.14E+02	< 1.10E+02	1.48E+02	< 1.24E+02
Antimony	< 1.40E+01	< 1.40E+01	< 1.40E+01	< 1.40E+01	< 5.60E+01	NA	NA	< 5.60E+01	< 1.40E+01	< 1.40E+01	1.77E+01	< 1.52E+01	< 1.40E+01	< 1.40E+01	< 1.40E+01	< 1.40E+01
Arsenic	< 5.10E+00	5.90E+00	< 5.10E+00	< 5.37E+00	< 2.04E+01	NA	NA	< 2.04E+01	3.67E+01	2.61E+01	3.93E+01	3.40E+01	1.37E+01	1.26E+01	1.19E+01	1.27E+01
Barium	5.12E+01	5.19E+01	4.92E+01	5.08E+01	3.63E+02	NA	NA	3.63E+02	8.74E+02	7.66E+02	1.13E+03	9.23E+02	2.47E+02	2.26E+02	2.38E+02	2.37E+02
Beryllium	< 1.80E+00	< 1.80E+00	< 1.80E+00	< 1.80E+00	< 7.20E+00	NA	NA	< 7.20E+00	3.80E+00	3.70E+00	5.40E+00	4.30E+00	< 1.80E+00	< 1.80E+00	< 1.80E+00	< 1.80E+00
Cadmium	< 8.20E-01	< 8.20E-01	< 8.20E-01	< 8.20E-01	< 3.30E+00	NA	NA	< 3.30E+00	1.13E+01	1.17E+01	1.37E+01	1.22E+01	< 8.20E-01	< 8.20E-01	2.40E+00	< 1.35E+00
Chromium	< 3.90E+00	< 3.90E+00	< 3.90E+00	< 3.90E+00	3.64E+02	NA	NA	3.64E+02	1.72E+03	1.75E+03	2.90E+03	2.12E+03	2.46E+01	1.30E+01	2.51E+01	2.09E+01
Cobalt	< 2.20E+00	< 2.20E+00	< 2.20E+00	< 2.20E+00	< 8.80E+00	NA	NA	< 8.80E+00	3.15E+01	2.64E+01	4.05E+01	3.28E+01	< 2.20E+00	< 2.20E+00	< 2.20E+00	< 2.20E+00
Copper	< 7.00E+00	< 7.00E+00	< 7.00E+00	< 7.00E+00	< 2.80E+01	NA	NA	< 2.80E+01	1.78E+03	9.65E+02	6.69E+02	1.14E+03	< 7.00E+00	< 7.00E+00	< 7.00E+00	< 7.00E+00
Lead	< 3.70E+00	< 3.70E+00	< 3.70E+00	< 3.70E+00	9.75E+01	NA	NA	9.75E+01	7.21E+02	5.92E+02	1.51E+03	9.41E+02	< 3.70E+00	< 3.70E+00	< 3.70E+00	< 3.70E+00
Manganese	1.54E+01	1.85E+01	1.40E+01	1.60E+01	7.48E+01	NA	NA	7.48E+01	3.38E+03	3.10E+03	4.32E+03	3.60E+03	1.15E+02	6.12E+01	8.59E+01	8.74E+01
Mercury	< 6.00E-02	< 6.00E-02	< 6.00E-02	< 6.00E-02	3.50E+00	NA	NA	3.50E+00	3.50E-01	4.20E-01	4.50E-01	4.07E-01	< 6.00E-02	< 6.00E-02	< 6.00E-02	< 6.00E-02
Nickel	< 3.80E+00	< 3.80E+00	< 3.80E+00	< 3.80E+00	1.50E+02	NA	NA	1.50E+02	4.33E+02	3.97E+02	4.05E+02	4.12E+02	< 3.80E+00	< 3.80E+00	4.60E+00	< 4.13E+00
Selenium	< 4.30E+00	< 4.30E+00	< 4.30E+00	< 4.30E+00	< 1.72E+01	NA	NA	< 1.72E+01	1.19E+01	8.60E+00	1.21E+01	1.09E+01	1.10E+01	1.00E+01	9.00E+00	1.00E+01
Silver	< 9.70E+00	< 9.70E+00	< 9.70E+00	< 9.70E+00	5.30E+01	NA	NA	5.30E+01	< 9.70E+00	< 9.70E+00	< 9.70E+00	< 9.70E+00	< 9.70E+00	< 9.70E+00	< 9.70E+00	< 9.70E+00
Thallium	< 1.00E+01	< 1.00E+01	< 1.00E+01	< 1.00E+01	< 4.00E+01	NA	NA	< 4.00E+01	< 1.00E+01	< 1.00E+01	< 1.00E+01	< 1.00E+01	< 1.00E+01	< 1.00E+01	< 1.00E+01	< 1.00E+01
Vanadium	< 5.00E+00	< 5.00E+00	< 5.00E+00	< 5.00E+00	< 2.00E+01	NA	NA	< 2.00E+01	8.43E+01	5.81E+01	1.09E+02	8.38E+01	2.56E+01	1.66E+01	2.10E+01	2.11E+01
Zinc	< 3.80E+00	< 3.80E+00	< 3.80E+00	< 3.80E+00	2.04E+02	NA	NA	2.04E+02	7.65E+02	5.64E+02	6.45E+02	6.58E+02	< 3.80E+00	< 3.80E+00	< 3.80E+00	< 3.80E+00
Volatile Organics																
Acetone	4.40E+00	3.80E+00	4.50E+00	4.23E+00	4.50E+00	NA	NA	4.50E+00	ND	4.10E+00	3.60E+00	3.85E+00	3.70E+00	3.70E+00	4.80E+00	4.07E+00
Bromobenzene	ND	ND	ND	ND	1.80E-01	NA	NA	1.80E-01	ND	ND	ND	ND	ND	ND	ND	ND
Bromodichloromethane	3.20E+00	4.10E+00	2.50E+00	3.27E+00	8.60E-01	NA	NA	8.60E-01	ND	ND	ND	ND	ND	8.90E-01	1.00E+00	9.45E-01
Bromoform	4.00E+01	3.20E+01	2.80E+01	3.33E+01	2.80E+00	NA	NA	ND	9.90E-01	9.20E-01	1.00E+00	9.70E-01	2.00E+00	2.00E+00	2.10E+00	2.03E+00
Carbon disulfide	ND	ND	ND	ND	ND	NA	NA	ND	ND	ND	ND	ND	ND	ND	ND	ND
Chlorodibromomethane	1.30E+01	1.30E+01	8.90E+00	1.16E+01	1.00E+00	NA	NA	1.00E+00	9.20E-01	8.70E-01	8.90E-01	8.93E-01	1.40E+00	1.30E+00	1.40E+00	1.37E+00
Chloroform	5.60E-01	6.40E-01	6.20E-01	6.07E-01	1.70E-01	NA	NA	1.70E-01	ND	ND	ND	ND	1.40E-01	1.50E-01	1.40E-01	1.43E-01
1,2-Dichloroethane	ND	1.30E-01	1.20E-01	1.25E-01	1.30E-01	NA	NA	1.30E-01	ND	ND	ND	ND	ND	ND	ND	ND
Iodomethane	ND	ND	ND	ND	ND	NA	NA	ND	5.50E-01	ND	ND	5.50E-01	ND	ND	ND	ND
Methylene chloride	5.50E-01	2.40E+00	2.00E+00	1.65E+00	5.30E-01	NA	NA	ND	ND	2.30E+00	8.40E-01	1.57E+00	3.60E-01	2.00E+00	6.50E-01	1.00E+00
Tetrachloroethene	3.30E-01	3.10E-01	4.50E-01	3.63E-01	2.40E-01	NA	NA	2.40E-01	ND	ND	ND	ND	1.30E-01	ND	ND	1.30E-01
Toluene	ND	4.10E-01	3.10E-01	3.60E-01	ND	NA	NA	ND	ND	4.10E-01	ND	4.10E-01	ND	4.30E-01	1.20E-01	2.75E-01
Semivolatile Organics																
bis(2-ethylhexyl)phthalate	ND	ND	ND	ND	4.10E+01	NA	NA	ND	ND	ND	ND	ND	ND	ND	ND	ND

Note: Only detected organics shown on this table.

Table 4-1. Regulatory Compliance Summary

Parameter	Units	Test Objective	Run 1	Run 2	Run 3	Test Average
DRE - Chlorobenzene	%	> 99.99	> 99.9914	> 99.9970	99.9940	> 99.9941
DRE - Tetrachloroethene	%	> 99.99	> 99.9951	> 99.9982	> 99.9976	> 99.9970
Stack gas filterable particulate matter concentration (b)	mg/dscm	< 34	21	10	18	16
	(gr/dscf)	< 0.015	0.0090	0.0046	0.0079	0.0072
Stack gas PCDD/PCDF (b)	ng TEQ/dscm	< 0.40	0.065	0.052	0.062	0.060
Stack gas mercury (b)	ug/dscm	< 130	< 6.1	< 5.8	< 7.5	< 6.5
Stack gas semivolatile metals (Cd + Pb) concentration (b)	ug/dscm	< 240	210	130	360	230
Stack gas low volatility metals (As + Be + Cr) concentration (b)	ug/dscm	< 97	< 35	< 12	< 21	< 23
Stack gas HCl/Cl ₂ (b)	ppmv as HCl	< 77	5.4	3.2	3.0	3.9
Stack gas carbon monoxide concentration (b)	ppmv	< 100	11.5	10.4	15.6	12.5
Stack gas total hydrocarbon concentration (b)	ppmv, as propane	< 10	< 0.6	< 0.6	< 0.6	< 0.6
Stack gas oxygen concentration	vol%, dry	NA	9.8	8.9	9.3	9.3

(a) Stack gas THC and O₂ data were obtained using Airtech's temporary CEMS.

(b) Corrected to 7% oxygen, dry basis.

Note: Compliance with regulatory standards is based on the arithmetic average of the three test runs, except for DRE, where each run must meet the specified criteria [see 40 CFR 63.1206(b)(12)(ii)]. All values are reported to two significant figures.

Table 4-2. POHC Feed Rates, Emissions Rates, and DREs

Parameter	Units	Test Results			
		Run 1	Run 2	Run 3	Average
Monochlorobenzene feed rate	lb/hr	34.81	35.05	35.05	34.97
Tetrachloroethene feed rate	lb/hr	35.04	35.02	34.84	34.97
Monochlorobenzene emission rate	lb/hr	< 2.99E-03	< 1.05E-03	2.09E-03	< 2.04E-03
Tetrachloroethene emission rate	lb/hr	< 1.73E-03	< 6.26E-04	< 8.35E-04	< 1.06E-03
Monochlorobenzene DRE	%	> 99.9914	> 99.9970	99.9940	> 99.9941
Tetrachloroethene DRE	%	> 99.9951	> 99.9982	> 99.9976	> 99.9970

Table 4-3. PCDD/PCDF Emission Summary – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	5,290
	acfm	11,760
Stack gas temperature	°F	176
Stack gas velocity	ft/min	3,744
Stack gas sample volume	dscf	139,210
	dscm	3,943
Isokinetic	%	101.2
Stack gas moisture content	vol%	45.2
Stack gas carbon dioxide	vol %, dry	6.4
Stack gas oxygen	vol %, dry	9.8
PCDD/PCDF		
Total PCDD/PCDF	pg/sample	< 12288
Stack gas PCDD/PCDF concentration	ng/dscm	< 3.12E+00
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 3.90E+00
PCDD/PCDF emission rate	g/s	< 7.78E-09
PCDD/PCDF Toxic Equivalents as 2,3,7,8-TCDD		
Stack gas PCDD/PCDF concentration	ng/dscm	< 5.23E-02
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 6.53E-02
PCDD/PCDF emission rate	g/s	< 1.30E-10

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-4. PCDD/PCDF Emission Summary – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	3,780
	acfm	8,320
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,646
Stack gas sample volume	dscf	119.220
	dscm	3.376
Isokinetic	%	100.9
Stack gas moisture content	vol%	44.4
Stack gas carbon dioxide	vol %, dry	7.2
Stack gas oxygen	vol %, dry	8.9
PCDD/PCDF		
Total PCDD/PCDF	pg/sample	< 7223.8
Stack gas PCDD/PCDF concentration	ng/dscm	< 2.12E+00
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 2.45E+00
PCDD/PCDF emission rate	g/s	< 3.78E-09
PCDD/PCDF Toxic Equivalents as 2,3,7,8-TCDD		
Stack gas PCDD/PCDF concentration	ng/dscm	< 4.52E-02
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 5.23E-02
PCDD/PCDF emission rate	g/s	< 8.07E-11

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-5. PCDD/PCDF Emission Summary – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	4,040
	acfm	8,850
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,820
Stack gas sample volume	dscf	126.180
	dscm	3.573
Isokinetic	%	99.9
Stack gas moisture content	vol%	44.5
Stack gas carbon dioxide	vol %, dry	7.1
Stack gas oxygen	vol %, dry	9.3
PCDD/PCDF		
Total PCDD/PCDF	pg/sample	< 9067.1
Stack gas PCDD/PCDF concentration	ng/dscm	< 2.49E+00
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 2.98E+00
PCDD/PCDF emission rate	g/s	< 4.75E-09
PCDD/PCDF Toxic Equivalents as 2,3,7,8-TCDD		
Stack gas PCDD/PCDF concentration	ng/dscm	< 5.23E-02
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 6.25E-02
PCDD/PCDF emission rate	g/s	< 9.96E-11

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-6. Particulate Matter, Hydrogen Chloride, and Chlorine Emissions Summary – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	5,030
	acfm	11,320
	dscm/min	142.45
Stack gas temperature	°F	175
Stack gas velocity	ft/min	3,606
Stack gas sample volume	dscf	72.660
	dscm	2.058
Isokinetic	%	93.7
Stack gas moisture content	vol %	45.9
Stack gas carbon dioxide content	vol %, dry	6.3
Stack gas oxygen content	vol %, dry	9.6
Hydrogen chloride and chlorine		
HCl collected	mg	11.8
Cl ₂ collected	mg	1.95
Stack gas HCl concentration	mg/dscm	5.73E+00
	mg/dscm @7% O ₂	7.04E+00
Stack gas HCl emission rate	lb/h	1.08E-01
	kg/h	4.90E-02
	g/s	1.36E-02
Stack gas Cl ₂ concentration	mg/dscm	9.48E-01
	mg/dscm @7% O ₂	1.16E+00
Stack gas Cl ₂ emission rate	lb/h	1.79E-02
	kg/h	8.10E-03
	g/s	2.25E-03
Stack gas HCl+Cl ₂ concentration expressed as HCl equivalents	ppmv, dry	4.42E+00
	ppmv, dry @7% O ₂	5.43E+00
Particulate		
Particulate matter collected	mg	34.3
Particulate concentration	gr/dscf	7.29E-03
	gr/dscf @ 7% O ₂	8.95E-03
	mg/dscm	1.67E+01
	mg/dscm @ 7% O ₂	2.05E+01
Particulate emission rate	lb/h	3.14E-01
	kg/h	1.42E-01
	g/s	3.96E-02

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-7. Particulate Matter, Hydrogen Chloride, and Chlorine Emissions Summary – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	3,850
	acfm	8,580
	dscm/min	109.03
Stack gas temperature	°F	174
Stack gas velocity	ft/min	2,730
Stack gas sample volume	dscf	74.990
	dscm	2.124
Isokinetic	%	96.0
Stack gas moisture content	vol %	45.1
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	8.9
Hydrogen chloride and chlorine		
HCl collected	mg	6.95
Cl ₂ collected	mg	2.01
Stack gas HCl concentration	mg/dscm	3.27E+00
	mg/dscm @7% O ₂	3.79E+00
Stack gas HCl emission rate	lb/h	4.72E-02
	kg/h	2.14E-02
	g/s	5.95E-03
Stack gas Cl ₂ concentration	mg/dscm	9.46E-01
	mg/dscm @7% O ₂	1.10E+00
Stack gas Cl ₂ emission rate	lb/h	1.37E-02
	kg/h	6.19E-03
	g/s	1.72E-03
Stack gas HCl+Cl ₂ concentration expressed as HCl equivalents	ppmv, dry	2.80E+00
	ppmv, dry @7% O ₂	3.24E+00
Particulate		
Particulate matter collected	mg	19.4
Particulate concentration	gr/dscf	3.99E-03
	gr/dscf @ 7% O ₂	4.62E-03
	mg/dscm	9.13E+00
	mg/dscm @ 7% O ₂	1.06E+01
Particulate emission rate	lb/h	1.32E-01
	kg/h	5.98E-02
	g/s	1.66E-02

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-8. Particulate Matter, Hydrogen Chloride, and Chlorine Emissions Summary – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	4,090
	acfm	8,970
	dscm/min	115.83
Stack gas temperature	°F	174
Stack gas velocity	ft/min	2,856
Stack gas sample volume	dscf	79.290
	dscm	2.246
Isokinetic	%	95.7
Stack gas moisture content	vol %	44.8
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	9.3
Hydrogen chloride and chlorine		
HCl collected	mg	6.49
Cl ₂ collected	mg	1.94
Stack gas HCl concentration	mg/dscm	2.89E+00
	mg/dscm @7% O ₂	3.46E+00
Stack gas HCl emission rate	lb/h	4.43E-02
	kg/h	2.01E-02
	g/s	5.58E-03
Stack gas Cl ₂ concentration	mg/dscm	8.64E-01
	mg/dscm @7% O ₂	1.03E+00
Stack gas Cl ₂ emission rate	lb/h	1.32E-02
	kg/h	6.00E-03
	g/s	1.67E-03
Stack gas HCl+Cl ₂ concentration expressed as HCl equivalents	ppmv, dry	2.49E+00
	ppmv, dry @7% O ₂	2.98E+00
Particulate		
Particulate matter collected	mg	33.6
Particulate concentration	gr/dscf	6.54E-03
	gr/dscf @ 7% O ₂	7.83E-03
	mg/dscm	1.50E+01
	mg/dscm @ 7% O ₂	1.79E+01
Particulate emission rate	lb/h	2.29E-01
	kg/h	1.04E-01
	g/s	2.89E-02

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-9. Metals Emission Summary – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	4,970
	acfm	11,260
	dscm/min	140.75
Stack gas temperature	°F	176
Stack gas velocity	ft/min	3,582
Stack gas sample volume	dscf	76,790
	dscm	2,175
Isokinetic	%	98.2
Stack gas moisture content	vol %	46.2
Stack gas carbon dioxide content	vol %, dry	6.3
Stack gas oxygen content	vol %, dry	9.6
Aluminum		
Metal collected	ug	132.3
Metal concentration	ug/dscm	6.08E+01
	ug/dscm @ 7% O ₂	7.47E+01
Metal emission rate	lb/h	1.13E-03
	g/s	1.43E-04
Antimony		
Metal collected	ug	< 5.3
Metal concentration	ug/dscm	< 2.44E+00
	ug/dscm @ 7% O ₂	< 2.99E+00
Metal emission rate	lb/h	< 4.54E-05
	g/s	< 5.72E-06
Arsenic		
Metal collected	ug	< 5.9
Metal concentration	ug/dscm	< 2.73E+00
	ug/dscm @ 7% O ₂	< 3.35E+00
Metal emission rate	lb/h	< 5.08E-05
	g/s	< 6.40E-06
Barium		
Metal collected	ug	10.2
Metal concentration	ug/dscm	4.69E+00
	ug/dscm @ 7% O ₂	5.76E+00
Metal emission rate	lb/h	8.73E-05
	g/s	1.10E-05
Beryllium		
Metal collected	ug	< 0.4
Metal concentration	ug/dscm	< 1.75E-01
	ug/dscm @ 7% O ₂	< 2.15E-01
Metal emission rate	lb/h	< 3.25E-06
	g/s	< 4.10E-07
Cadmium		
Metal collected	ug	12.1
Metal concentration	ug/dscm	5.56E+00
	ug/dscm @ 7% O ₂	6.83E+00
Metal emission rate	lb/h	1.04E-04
	g/s	1.31E-05
Chromium		
Metal collected	ug	56.0
Metal concentration	ug/dscm	2.58E+01
	ug/dscm @ 7% O ₂	3.16E+01
Metal emission rate	lb/h	4.79E-04
	g/s	6.04E-05
Cobalt		
Metal collected	ug	< 1.1
Metal concentration	ug/dscm	< 5.15E-01
	ug/dscm @ 7% O ₂	< 6.32E-01
Metal emission rate	lb/h	< 9.59E-06
	g/s	< 1.21E-06
Copper		
Metal collected	ug	167.1
Metal concentration	ug/dscm	7.68E+01
	ug/dscm @ 7% O ₂	9.44E+01
Metal emission rate	lb/h	1.43E-03
	g/s	1.80E-04
Lead		
Metal collected	ug	356.8
Metal concentration	ug/dscm	1.64E+02
	ug/dscm @ 7% O ₂	2.01E+02
Metal emission rate	lb/h	3.05E-03
	g/s	3.85E-04
Manganese		
Metal collected	ug	65.8
Metal concentration	ug/dscm	3.03E+01
	ug/dscm @ 7% O ₂	3.72E+01
Metal emission rate	lb/h	5.63E-04
	g/s	7.10E-05
Mercury		
Metal collected	ug	< 10.8
Metal concentration	ug/dscm	< 4.98E+00
	ug/dscm @ 7% O ₂	< 6.11E+00
Metal emission rate	lb/h	< 9.26E-05
	g/s	< 1.17E-05
Nickel		
Metal collected	ug	12.0
Metal concentration	ug/dscm	5.52E+00
	ug/dscm @ 7% O ₂	6.78E+00
Metal emission rate	lb/h	1.03E-04
	g/s	1.29E-05
Selenium		
Metal collected	ug	4.5
Metal concentration	ug/dscm	2.07E+00
	ug/dscm @ 7% O ₂	2.54E+00
Metal emission rate	lb/h	3.85E-05
	g/s	4.85E-06
Silver		
Metal collected	ug	2.6
Metal concentration	ug/dscm	1.20E+00
	ug/dscm @ 7% O ₂	1.47E+00
Metal emission rate	lb/h	2.23E-05
	g/s	2.80E-06
Thallium		
Metal collected	ug	< 11.0
Metal concentration	ug/dscm	< 5.06E+00
	ug/dscm @ 7% O ₂	< 6.21E+00
Metal emission rate	lb/h	< 9.42E-05
	g/s	< 1.19E-05
Vanadium		
Metal collected	ug	< 3.0
Metal concentration	ug/dscm	< 1.38E+00
	ug/dscm @ 7% O ₂	< 1.69E+00
Metal emission rate	lb/h	< 2.57E-05
	g/s	< 3.24E-06
Zinc		
Metal collected	ug	218.4
Metal concentration	ug/dscm	1.00E+02
	ug/dscm @ 7% O ₂	1.23E+02
Metal emission rate	lb/h	1.87E-03
	g/s	2.36E-04

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-10. Metals Emission Summary – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	3,860
	acfm	8,600
	dscm/min	109.32
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,736
Stack gas sample volume	dscf	79,370
	dscm	2,248
Isokinetic	%	102.9
Stack gas moisture content	vol %	45.1
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	8.9
Aluminum		
Metal collected	ug	123.2
Metal concentration	ug/dscm	5.48E+01
	ug/dscm @ 7% O ₂	6.34E+01
Metal emission rate	lb/h	7.93E-04
	g/s	9.99E-05
Antimony		
Metal collected	ug	< 4.8
Metal concentration	ug/dscm	< 2.14E+00
	ug/dscm @ 7% O ₂	< 2.47E+00
Metal emission rate	lb/h	< 3.09E-05
	g/s	< 3.89E-06
Arsenic		
Metal collected	ug	< 2.7
Metal concentration	ug/dscm	< 1.21E+00
	ug/dscm @ 7% O ₂	< 1.41E+00
Metal emission rate	lb/h	< 1.76E-05
	g/s	< 2.21E-06
Barium		
Metal collected	ug	9.0
Metal concentration	ug/dscm	4.00E+00
	ug/dscm @ 7% O ₂	4.63E+00
Metal emission rate	lb/h	5.79E-05
	g/s	7.30E-06
Beryllium		
Metal collected	ug	< 0.4 ND
Metal concentration	ug/dscm	< 1.60E-01 ND
	ug/dscm @ 7% O ₂	< 1.85E-01 ND
Metal emission rate	lb/h	< 2.32E-06 ND
	g/s	< 2.92E-07 ND
Cadmium		
Metal collected	ug	7.9
Metal concentration	ug/dscm	3.51E+00
	ug/dscm @ 7% O ₂	4.07E+00
Metal emission rate	lb/h	5.08E-05
	g/s	6.40E-06
Chromium		
Metal collected	ug	20.2
Metal concentration	ug/dscm	8.99E+00
	ug/dscm @ 7% O ₂	1.04E+01
Metal emission rate	lb/h	1.30E-04
	g/s	1.64E-05
Cobalt		
Metal collected	ug	< 1.0 ND
Metal concentration	ug/dscm	< 4.45E-01 ND
	ug/dscm @ 7% O ₂	< 5.15E-01 ND
Metal emission rate	lb/h	< 6.43E-06 ND
	g/s	< 8.11E-07 ND
Copper		
Metal collected	ug	108.1
Metal concentration	ug/dscm	4.81E+01
	ug/dscm @ 7% O ₂	5.56E+01
Metal emission rate	lb/h	6.95E-04
	g/s	8.76E-05
Lead		
Metal collected	ug	250.4
Metal concentration	ug/dscm	1.11E+02
	ug/dscm @ 7% O ₂	1.29E+02
Metal emission rate	lb/h	1.61E-03
	g/s	2.03E-04
Manganese		
Metal collected	ug	42.0
Metal concentration	ug/dscm	1.87E+01
	ug/dscm @ 7% O ₂	2.16E+01
Metal emission rate	lb/h	2.70E-04
	g/s	3.40E-05
Mercury		
Metal collected	ug	< 11.3
Metal concentration	ug/dscm	< 5.02E+00
	ug/dscm @ 7% O ₂	< 5.81E+00
Metal emission rate	lb/h	< 7.26E-05
	g/s	< 9.15E-06
Nickel		
Metal collected	ug	11.4
Metal concentration	ug/dscm	5.07E+00
	ug/dscm @ 7% O ₂	5.87E+00
Metal emission rate	lb/h	7.33E-05
	g/s	9.24E-06
Selenium		
Metal collected	ug	4.0
Metal concentration	ug/dscm	1.78E+00
	ug/dscm @ 7% O ₂	2.06E+00
Metal emission rate	lb/h	2.57E-05
	g/s	3.24E-06
Silver		
Metal collected	ug	5.7
Metal concentration	ug/dscm	2.54E+00
	ug/dscm @ 7% O ₂	2.93E+00
Metal emission rate	lb/h	3.67E-05
	g/s	4.62E-06
Thallium		
Metal collected	ug	< 10.6
Metal concentration	ug/dscm	< 4.72E+00
	ug/dscm @ 7% O ₂	< 5.46E+00
Metal emission rate	lb/h	< 6.82E-05
	g/s	< 8.59E-06
Vanadium		
Metal collected	ug	< 1.6
Metal concentration	ug/dscm	< 7.12E-01
	ug/dscm @ 7% O ₂	< 8.24E-01
Metal emission rate	lb/h	< 1.03E-05
	g/s	< 1.30E-06
Zinc		
Metal collected	ug	136.2
Metal concentration	ug/dscm	6.06E+01
	ug/dscm @ 7% O ₂	7.01E+01
Metal emission rate	lb/h	8.76E-04
	g/s	1.10E-04

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 4-11. Metals Emission Summary – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	4,000
	acfm	8,920
	dscm/min	113.28
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,838
Stack gas sample volume	dscf	82,610
	dscm	2,340
Isokinetic	%	103.2
Stack gas moisture content	vol %	45.5
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	9.3
Aluminum		
Metal collected	ug	125.2
Metal concentration	ug/dscm	5.35E+01
	ug/dscm @ 7% O ₂	6.40E+01
Metal emission rate	lb/h	8.02E-04
	g/s	1.01E-04
Antimony		
Metal collected	ug	< 4.9
Metal concentration	ug/dscm	< 2.09E+00
	ug/dscm @ 7% O ₂	< 2.51E+00
Metal emission rate	lb/h	< 3.14E-05
	g/s	< 3.95E-06
Arsenic		
Metal collected	ug	< 3.7
Metal concentration	ug/dscm	< 1.59E+00
	ug/dscm @ 7% O ₂	< 1.91E+00
Metal emission rate	lb/h	< 2.39E-05
	g/s	< 3.01E-06
Barium		
Metal collected	ug	10.8
Metal concentration	ug/dscm	4.62E+00
	ug/dscm @ 7% O ₂	5.52E+00
Metal emission rate	lb/h	6.92E-05
	g/s	8.72E-06
Beryllium		
Metal collected	ug	< 0.4 ND
Metal concentration	ug/dscm	< 1.54E-01 ND
	ug/dscm @ 7% O ₂	< 1.84E-01 ND
Metal emission rate	lb/h	< 2.31E-06 ND
	g/s	< 2.91E-07 ND
Cadmium		
Metal collected	ug	9.7
Metal concentration	ug/dscm	4.15E+00
	ug/dscm @ 7% O ₂	4.97E+00
Metal emission rate	lb/h	6.22E-05
	g/s	7.84E-06
Chromium		
Metal collected	ug	36.5
Metal concentration	ug/dscm	1.56E+01
	ug/dscm @ 7% O ₂	1.87E+01
Metal emission rate	lb/h	2.34E-04
	g/s	2.95E-05
Cobalt		
Metal collected	ug	< 1.0 ND
Metal concentration	ug/dscm	< 4.27E-01 ND
	ug/dscm @ 7% O ₂	< 5.11E-01 ND
Metal emission rate	lb/h	< 6.40E-06 ND
	g/s	< 8.07E-07 ND
Copper		
Metal collected	ug	112.4
Metal concentration	ug/dscm	4.80E+01
	ug/dscm @ 7% O ₂	5.75E+01
Metal emission rate	lb/h	7.20E-04
	g/s	9.07E-05
Lead		
Metal collected	ug	694.2
Metal concentration	ug/dscm	2.97E+02
	ug/dscm @ 7% O ₂	3.55E+02
Metal emission rate	lb/h	4.45E-03
	g/s	5.60E-04
Manganese		
Metal collected	ug	41.4
Metal concentration	ug/dscm	1.77E+01
	ug/dscm @ 7% O ₂	2.12E+01
Metal emission rate	lb/h	2.65E-04
	g/s	3.34E-05
Mercury		
Metal collected	ug	< 14.7
Metal concentration	ug/dscm	< 6.28E+00
	ug/dscm @ 7% O ₂	< 7.52E+00
Metal emission rate	lb/h	< 9.42E-05
	g/s	< 1.19E-05
Nickel		
Metal collected	ug	9.4
Metal concentration	ug/dscm	4.02E+00
	ug/dscm @ 7% O ₂	4.81E+00
Metal emission rate	lb/h	6.02E-05
	g/s	7.59E-06
Selenium		
Metal collected	ug	3.9
Metal concentration	ug/dscm	1.68E+00
	ug/dscm @ 7% O ₂	2.02E+00
Metal emission rate	lb/h	2.52E-05
	g/s	3.18E-06
Silver		
Metal collected	ug	< 1.9 ND
Metal concentration	ug/dscm	< 8.29E-01 ND
	ug/dscm @ 7% O ₂	< 9.92E-01 ND
Metal emission rate	lb/h	< 1.24E-05 ND
	g/s	< 1.57E-06 ND
Thallium		
Metal collected	ug	< 10.7
Metal concentration	ug/dscm	< 4.57E+00
	ug/dscm @ 7% O ₂	< 5.47E+00
Metal emission rate	lb/h	< 6.85E-05
	g/s	< 8.64E-06
Vanadium		
Metal collected	ug	< 2.0
Metal concentration	ug/dscm	< 8.55E-01
	ug/dscm @ 7% O ₂	< 1.02E+00
Metal emission rate	lb/h	< 1.28E-05
	g/s	< 1.61E-06
Zinc		
Metal collected	ug	133.3
Metal concentration	ug/dscm	5.70E+01
	ug/dscm @ 7% O ₂	6.82E+01
Metal emission rate	lb/h	8.54E-04
	g/s	1.08E-04

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 5-1. VOST Audit Sample Results

Compound	Units	Original Audit Samples (No Ice)						Final Audit Samples (Ice)		
		#1	#2	#3	#4	#5	#6	#1	#2	#3
Acetone	ug	0.31	0.39	0.39	0.26	0.18	ND	0.22 B	0.24 B	0.17 B
Benzene	ug	0.054	0.058	0.057	0.058	0.063	0.059	0.064	0.069	0.068
2-Butanone	ug	0.082 J	0.091 J	0.084 J	0.068 J	0.046 J	ND	0.044 J	0.053 J	ND
Carbon Disulfide	ug	0.015	0.016	0.016	0.016	0.015	0.016	0.017	0.018	0.018
Carbon Tetrachloride	ug	0.041	0.046	0.045	0.046	0.047	0.049	0.049	0.053	0.052
Chlorobenzene	ug	ND	ND	0.0013 J	0.0016 J	0.0029 J	0.0044 J	ND	ND	ND
Chloroform	ug	0.065	0.074	0.069	0.072	0.076	0.074	0.078	0.086	0.089
Methylene Chloride	ug	0.075	0.077	0.072	0.075	0.076	0.075	0.099	0.12	0.12
Tetrachloroethene	ug	0.14	0.16	0.16	0.16	0.14	0.16	0.15	0.15	0.14
Tetrahydrofuran	ug	ND	ND	ND	ND	0.034 J	ND	ND	0.036 J	0.054 J
Toluene	ug	0.0032 J	0.0035 J	0.0033 J	0.0033 J	0.003 J	0.0034 J	0.0036 J	0.0034 J	0.0032 J

Table 6-1. Proposed Operating Parameter Limits

Control Parameters ^a	Anticipated Permit Limit	Comments ^b
GROUP A1 PARAMETERS		
Maximum spent carbon feed rate (lb/hr)	3049	Block hour AWFCO
Minimum afterburner temperature (°F)	1760	Hourly rolling average AWFCO
Maximum hearth #5 temperature (°F)	1650	Hourly rolling average AWFCO
Minimum hearth #5 temperature (°F)	TBD	Hourly rolling average AWFCO
Minimum venturi scrubber pressure differential (in. w.c.)	18	Hourly rolling average AWFCO
Minimum quench/venturi scrubber total liquid flow rate (gpm)	75	Hourly rolling average AWFCO
Minimum packed bed scrubber pH	4.4	Hourly rolling average AWFCO
Minimum packed bed scrubber liquid flow rate (gpm)	63	Hourly rolling average AWFCO
Minimum wet scrubber blowdown flow rate (gpm)	58	Hourly rolling average AWFCO
Minimum WESP secondary voltage (kVDC)	22	Hourly rolling average AWFCO
Maximum stack gas flow rate acfm	9,550	Hourly rolling average AWFCO
GROUP A2 PARAMETERS		
Maximum stack gas carbon monoxide (ppmvd, @7% oxygen) ^c	100	Hourly rolling average AWFCO
GROUP B PARAMETERS		
Allowable hazardous constituents	All except dioxin wastes and TSCA PCBs	Class 1 POHC demonstrated
Maximum total chlorine and chloride feed rate (lb/hr)	60	12-hour rolling average
Maximum mercury feed rate (lb/hr)	1.8E-03	12-hour rolling average
Maximum semivolatile metal (Cd + Pb) feed rate (lb/hr)	1.0E-01	12-hour rolling average
Maximum low volatility metal (As + Be + Cr) feed rate (lb/hr)	1.5E+00	12-hour rolling average
GROUP C PARAMETERS		
Minimum packed bed scrubber pressure differential (in. w.c.)	0.1	Hourly rolling average

(a) Group A1 parameters are continuously monitored and recorded, and are interlocked with the automatic waste feed cutoff system. The values for the Group A1 parameters are based on the performance demonstration test operating conditions.

Group A2 parameters are continuously monitored and recorded, and are interlocked with the automatic waste feed cutoff system. The values for the Group A2 parameters are based on regulatory standards or good operating practice rather than performance demonstration test operating conditions.

Group B parameters are continuously monitored and recorded, but are not interlocked with the automatic waste feed cutoff system. Values for the group B parameters are based on the performance demonstration test operating conditions.

Group C parameters are continuously monitoring and recording, but are not interlocked with the automatic waste feed cutoff system. The values for the Group C parameters are based on manufacturer's specifications and/or operational and safety considerations rather than performance demonstration test operating conditions.

(b) AWFCO = Automatic waste feed cutoff.

(c) AWFCO interlock will not be active during the daily CEM calibration period.

Table 6-2. Metals System Removal Efficiency

Run 1

Metal	Feed Rate (lb/hr)	Feed Rate (g/hr)	Emission Rate (lb/hr)	Emission Rate (g/hr)	SRE (%)
Chromium	3.59E-01	1.63E+02	4.79E-04	2.17E-01	99.87%

Run 2

Metal	Feed Rate (lb/hr)	Feed Rate (g/hr)	Emission Rate (lb/hr)	Emission Rate (g/hr)	SRE (%)
Chromium	3.71E-01	1.68E+02	1.30E-04	5.90E-02	99.96%

Run 3

Metal	Feed Rate (lb/hr)	Feed Rate (g/hr)	Emission Rate (lb/hr)	Emission Rate (g/hr)	SRE (%)
Chromium	3.66E-01	1.66E+02	2.34E-04	1.06E-01	99.94%

Table 7-1. Metals Emission Summary – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	4,970
	acfm	11,260
	dscm/min	140.75
Stack gas temperature	°F	176
Stack gas velocity	ft/min	3,582
Stack gas sample volume	dscf	76,790
	dscm	2,175
Isokinetic	%	98.2
Stack gas moisture content	vol %	46.2
Stack gas carbon dioxide content	vol %, dry	6.3
Stack gas oxygen content	vol %, dry	9.6
Aluminum		
Metal collected	ug	132.3
Metal concentration	ug/dscm	6.08E+01
	ug/dscm @ 7% O ₂	7.47E+01
Metal emission rate	lb/h	1.13E-03
	g/s	1.43E-04
Antimony		
Metal collected	ug	< 5.3
Metal concentration	ug/dscm	< 2.44E+00
	ug/dscm @ 7% O ₂	< 2.99E+00
Metal emission rate	lb/h	< 4.54E-05
	g/s	< 5.72E-06
Arsenic		
Metal collected	ug	< 5.9
Metal concentration	ug/dscm	< 2.73E+00
	ug/dscm @ 7% O ₂	< 3.35E+00
Metal emission rate	lb/h	< 5.08E-05
	g/s	< 6.40E-06
Barium		
Metal collected	ug	10.2
Metal concentration	ug/dscm	4.69E+00
	ug/dscm @ 7% O ₂	5.76E+00
Metal emission rate	lb/h	8.73E-05
	g/s	1.10E-05
Beryllium		
Metal collected	ug	< 0.4
Metal concentration	ug/dscm	< 1.75E-01
	ug/dscm @ 7% O ₂	< 2.15E-01
Metal emission rate	lb/h	< 3.25E-06
	g/s	< 4.10E-07
Cadmium		
Metal collected	ug	12.1
Metal concentration	ug/dscm	5.56E+00
	ug/dscm @ 7% O ₂	6.83E+00
Metal emission rate	lb/h	1.04E-04
	g/s	1.31E-05
Chromium		
Metal collected	ug	56.0
Metal concentration	ug/dscm	2.58E+01
	ug/dscm @ 7% O ₂	3.16E+01
Metal emission rate	lb/h	4.79E-04
	g/s	6.04E-05
Cobalt		
Metal collected	ug	< 1.1
Metal concentration	ug/dscm	< 5.15E-01
	ug/dscm @ 7% O ₂	< 6.32E-01
Metal emission rate	lb/h	< 9.59E-06
	g/s	< 1.21E-06
Copper		
Metal collected	ug	167.1
Metal concentration	ug/dscm	7.68E+01
	ug/dscm @ 7% O ₂	9.44E+01
Metal emission rate	lb/h	1.43E-03
	g/s	1.80E-04
Lead		
Metal collected	ug	356.8
Metal concentration	ug/dscm	1.64E+02
	ug/dscm @ 7% O ₂	2.01E+02
Metal emission rate	lb/h	3.05E-03
	g/s	3.85E-04
Manganese		
Metal collected	ug	65.8
Metal concentration	ug/dscm	3.03E+01
	ug/dscm @ 7% O ₂	3.72E+01
Metal emission rate	lb/h	5.63E-04
	g/s	7.10E-05
Mercury		
Metal collected	ug	< 10.8
Metal concentration	ug/dscm	< 4.98E+00
	ug/dscm @ 7% O ₂	< 6.11E+00
Metal emission rate	lb/h	< 9.26E-05
	g/s	< 1.17E-05
Nickel		
Metal collected	ug	12.0
Metal concentration	ug/dscm	5.52E+00
	ug/dscm @ 7% O ₂	6.78E+00
Metal emission rate	lb/h	1.03E-04
	g/s	1.29E-05
Selenium		
Metal collected	ug	4.5
Metal concentration	ug/dscm	2.07E+00
	ug/dscm @ 7% O ₂	2.54E+00
Metal emission rate	lb/h	3.85E-05
	g/s	4.85E-06
Silver		
Metal collected	ug	2.6
Metal concentration	ug/dscm	1.20E+00
	ug/dscm @ 7% O ₂	1.47E+00
Metal emission rate	lb/h	2.23E-05
	g/s	2.80E-06
Thallium		
Metal collected	ug	< 11.0
Metal concentration	ug/dscm	< 5.06E+00
	ug/dscm @ 7% O ₂	< 6.21E+00
Metal emission rate	lb/h	< 9.42E-05
	g/s	< 1.19E-05
Vanadium		
Metal collected	ug	< 3.0
Metal concentration	ug/dscm	< 1.38E+00
	ug/dscm @ 7% O ₂	< 1.69E+00
Metal emission rate	lb/h	< 2.57E-05
	g/s	< 3.24E-06
Zinc		
Metal collected	ug	218.4
Metal concentration	ug/dscm	1.00E+02
	ug/dscm @ 7% O ₂	1.23E+02
Metal emission rate	lb/h	1.87E-03
	g/s	2.36E-04

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-2. Metals Emission Summary – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	3,860
	acfm	8,600
	dscm/min	109.32
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,736
Stack gas sample volume	dscf	79,370
	dscm	2,248
Isokinetic	%	102.9
Stack gas moisture content	vol %	45.1
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	8.9
Aluminum		
Metal collected	ug	123.2
Metal concentration	ug/dscm	5.48E+01
	ug/dscm @ 7% O ₂	6.34E+01
Metal emission rate	lb/h	7.93E-04
	g/s	9.99E-05
Antimony		
Metal collected	ug	< 4.8
Metal concentration	ug/dscm	< 2.14E+00
	ug/dscm @ 7% O ₂	< 2.47E+00
Metal emission rate	lb/h	< 3.09E-05
	g/s	< 3.89E-06
Arsenic		
Metal collected	ug	< 2.7
Metal concentration	ug/dscm	< 1.21E+00
	ug/dscm @ 7% O ₂	< 1.41E+00
Metal emission rate	lb/h	< 1.76E-05
	g/s	< 2.21E-06
Barium		
Metal collected	ug	9.0
Metal concentration	ug/dscm	4.00E+00
	ug/dscm @ 7% O ₂	4.63E+00
Metal emission rate	lb/h	5.79E-05
	g/s	7.30E-06
Beryllium		
Metal collected	ug	< 0.4 ND
Metal concentration	ug/dscm	< 1.60E-01 ND
	ug/dscm @ 7% O ₂	< 1.85E-01 ND
Metal emission rate	lb/h	< 2.32E-06 ND
	g/s	< 2.92E-07 ND
Cadmium		
Metal collected	ug	7.9
Metal concentration	ug/dscm	3.51E+00
	ug/dscm @ 7% O ₂	4.07E+00
Metal emission rate	lb/h	5.08E-05
	g/s	6.40E-06
Chromium		
Metal collected	ug	20.2
Metal concentration	ug/dscm	8.99E+00
	ug/dscm @ 7% O ₂	1.04E+01
Metal emission rate	lb/h	1.30E-04
	g/s	1.64E-05
Cobalt		
Metal collected	ug	< 1.0 ND
Metal concentration	ug/dscm	< 4.45E-01 ND
	ug/dscm @ 7% O ₂	< 5.15E-01 ND
Metal emission rate	lb/h	< 6.43E-06 ND
	g/s	< 8.11E-07 ND
Copper		
Metal collected	ug	108.1
Metal concentration	ug/dscm	4.81E+01
	ug/dscm @ 7% O ₂	5.56E+01
Metal emission rate	lb/h	6.95E-04
	g/s	8.76E-05
Lead		
Metal collected	ug	250.4
Metal concentration	ug/dscm	1.11E+02
	ug/dscm @ 7% O ₂	1.29E+02
Metal emission rate	lb/h	1.61E-03
	g/s	2.03E-04
Manganese		
Metal collected	ug	42.0
Metal concentration	ug/dscm	1.87E+01
	ug/dscm @ 7% O ₂	2.16E+01
Metal emission rate	lb/h	2.70E-04
	g/s	3.40E-05
Mercury		
Metal collected	ug	< 11.3
Metal concentration	ug/dscm	< 5.02E+00
	ug/dscm @ 7% O ₂	< 5.81E+00
Metal emission rate	lb/h	< 7.26E-05
	g/s	< 9.15E-06
Nickel		
Metal collected	ug	11.4
Metal concentration	ug/dscm	5.07E+00
	ug/dscm @ 7% O ₂	5.87E+00
Metal emission rate	lb/h	7.33E-05
	g/s	9.24E-06
Selenium		
Metal collected	ug	4.0
Metal concentration	ug/dscm	1.78E+00
	ug/dscm @ 7% O ₂	2.06E+00
Metal emission rate	lb/h	2.57E-05
	g/s	3.24E-06
Silver		
Metal collected	ug	5.7
Metal concentration	ug/dscm	2.54E+00
	ug/dscm @ 7% O ₂	2.93E+00
Metal emission rate	lb/h	3.67E-05
	g/s	4.62E-06
Thallium		
Metal collected	ug	< 10.6
Metal concentration	ug/dscm	< 4.72E+00
	ug/dscm @ 7% O ₂	< 5.46E+00
Metal emission rate	lb/h	< 6.82E-05
	g/s	< 8.59E-06
Vanadium		
Metal collected	ug	< 1.6
Metal concentration	ug/dscm	< 7.12E-01
	ug/dscm @ 7% O ₂	< 8.24E-01
Metal emission rate	lb/h	< 1.03E-05
	g/s	< 1.30E-06
Zinc		
Metal collected	ug	136.2
Metal concentration	ug/dscm	6.06E+01
	ug/dscm @ 7% O ₂	7.01E+01
Metal emission rate	lb/h	8.76E-04
	g/s	1.10E-04

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-3. Metals Emission Summary – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	4,000
	acfm	8,920
	dscm/min	113.28
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,838
Stack gas sample volume	dscf	82,610
	dscm	2,340
Isokinetic	%	103.2
Stack gas moisture content	vol %	45.5
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	9.3
Aluminum		
Metal collected	ug	125.2
Metal concentration	ug/dscm	5.35E+01
	ug/dscm @ 7% O ₂	6.40E+01
Metal emission rate	lb/h	8.02E-04
	g/s	1.01E-04
Antimony		
Metal collected	ug	< 4.9
Metal concentration	ug/dscm	< 2.09E+00
	ug/dscm @ 7% O ₂	< 2.51E+00
Metal emission rate	lb/h	< 3.14E-05
	g/s	< 3.95E-06
Arsenic		
Metal collected	ug	< 3.7
Metal concentration	ug/dscm	< 1.59E+00
	ug/dscm @ 7% O ₂	< 1.91E+00
Metal emission rate	lb/h	< 2.39E-05
	g/s	< 3.01E-06
Barium		
Metal collected	ug	10.8
Metal concentration	ug/dscm	4.62E+00
	ug/dscm @ 7% O ₂	5.52E+00
Metal emission rate	lb/h	6.92E-05
	g/s	8.72E-06
Beryllium		
Metal collected	ug	< 0.4 ND
Metal concentration	ug/dscm	< 1.54E-01 ND
	ug/dscm @ 7% O ₂	< 1.84E-01 ND
Metal emission rate	lb/h	< 2.31E-06 ND
	g/s	< 2.91E-07 ND
Cadmium		
Metal collected	ug	9.7
Metal concentration	ug/dscm	4.15E+00
	ug/dscm @ 7% O ₂	4.97E+00
Metal emission rate	lb/h	6.22E-05
	g/s	7.84E-06
Chromium		
Metal collected	ug	36.5
Metal concentration	ug/dscm	1.56E+01
	ug/dscm @ 7% O ₂	1.87E+01
Metal emission rate	lb/h	2.34E-04
	g/s	2.95E-05
Cobalt		
Metal collected	ug	< 1.0 ND
Metal concentration	ug/dscm	< 4.27E-01 ND
	ug/dscm @ 7% O ₂	< 5.11E-01 ND
Metal emission rate	lb/h	< 6.40E-06 ND
	g/s	< 8.07E-07 ND
Copper		
Metal collected	ug	112.4
Metal concentration	ug/dscm	4.80E+01
	ug/dscm @ 7% O ₂	5.75E+01
Metal emission rate	lb/h	7.20E-04
	g/s	9.07E-05
Lead		
Metal collected	ug	694.2
Metal concentration	ug/dscm	2.97E+02
	ug/dscm @ 7% O ₂	3.55E+02
Metal emission rate	lb/h	4.45E-03
	g/s	5.60E-04
Manganese		
Metal collected	ug	41.4
Metal concentration	ug/dscm	1.77E+01
	ug/dscm @ 7% O ₂	2.12E+01
Metal emission rate	lb/h	2.65E-04
	g/s	3.34E-05
Mercury		
Metal collected	ug	< 14.7
Metal concentration	ug/dscm	< 6.28E+00
	ug/dscm @ 7% O ₂	< 7.52E+00
Metal emission rate	lb/h	< 9.42E-05
	g/s	< 1.19E-05
Nickel		
Metal collected	ug	9.4
Metal concentration	ug/dscm	4.02E+00
	ug/dscm @ 7% O ₂	4.81E+00
Metal emission rate	lb/h	6.02E-05
	g/s	7.59E-06
Selenium		
Metal collected	ug	3.9
Metal concentration	ug/dscm	1.68E+00
	ug/dscm @ 7% O ₂	2.02E+00
Metal emission rate	lb/h	2.52E-05
	g/s	3.18E-06
Silver		
Metal collected	ug	< 1.9 ND
Metal concentration	ug/dscm	< 8.29E-01 ND
	ug/dscm @ 7% O ₂	< 9.92E-01 ND
Metal emission rate	lb/h	< 1.24E-05 ND
	g/s	< 1.57E-06 ND
Thallium		
Metal collected	ug	< 10.7
Metal concentration	ug/dscm	< 4.57E+00
	ug/dscm @ 7% O ₂	< 5.47E+00
Metal emission rate	lb/h	< 6.85E-05
	g/s	< 8.64E-06
Vanadium		
Metal collected	ug	< 2.0
Metal concentration	ug/dscm	< 8.55E-01
	ug/dscm @ 7% O ₂	< 1.02E+00
Metal emission rate	lb/h	< 1.28E-05
	g/s	< 1.61E-06
Zinc		
Metal collected	ug	133.3
Metal concentration	ug/dscm	5.70E+01
	ug/dscm @ 7% O ₂	6.82E+01
Metal emission rate	lb/h	8.54E-04
	g/s	1.08E-04

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-4. Mercury Speciation

	Sample results					Speciation Calculations			
	Vapor Phase Ionic Mercury (ug)	Particulate Phase Ionic Mercury (ug)	Total Ionic Mercury (ug)	Elemental Mercury (ug)	Total Mercury (ug)	Vapor phase Ionic Mercury (%)	Particulate Phase Ionic Mercury (%)	Total Ionic Mercury (%)	Elemental Mercury (%)
Run 1	1.30	0.06	1.36	9.46	10.82	12.01%	0.55%	12.57%	87.43%
Run 2	1.70	0.06	1.76	9.53	11.29	15.06%	0.53%	15.59%	84.41%
Run 3	4.30	0.06	4.36	10.34	14.70	29.25%	0.41%	29.66%	70.34%
Average	2.43	0.06	2.49	9.78	12.27	19.83%	0.49%	20.32%	79.68%

Vapor Phase Ionic Mercury (Acidified Peroxide Liquid)

Particulate Phase Ionic Mercury (Filter and Front Half Rinse)

Elemental Mercury (Components Downstream of Peroxide Impinger, includes Permanganate Liquid and Rinse)

Table 7-5. Hexavalent Chromium Emission Summary – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	5,120
	acfm	11,160
	dscm/min	145.00
Stack gas temperature	°F	176
Stack gas velocity	ft/min	3,552
Stack gas sample volume	dscf	76.040
	dscm	2.153
Isokinetic	%	93.6
Stack gas moisture content	vol %	44.0
Stack gas carbon dioxide content	vol %, dry	6.3
Stack gas oxygen content	vol %, dry	9.6
Hexavalent chromium		
Metal collected	ug	5.6
Metal concentration	ug/dscm	2.60E+00
	ug/dscm @ 7% O ₂	3.19E+00
Metal emission rate	lb/h	4.99E-05
	g/s	6.28E-06

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-6. Hexavalent Chromium Emission Summary – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	3,780
	acfm	8,470
	dscm/min	107.05
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,694
Stack gas sample volume	dscf	75.030
	dscm	2.125
Isokinetic	%	101.1
Stack gas moisture content	vol %	45.3
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	8.9
Hexavalent chromium		
Metal collected	ug	5.9
Metal concentration	ug/dscm	2.78E+00
	ug/dscm @ 7% O ₂	3.21E+00
Metal emission rate	lb/h	3.93E-05
	g/s	4.95E-06

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-7. Hexavalent Chromium Emission Summary – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	3,890
	acfm	8,770
	dscm/min	110.17
Stack gas temperature	°F	176
Stack gas velocity	ft/min	2,796
Stack gas sample volume	dscf	78.620
	dscm	2.227
Isokinetic	%	103.1
Stack gas moisture content	vol %	46.1
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	9.3
Hexavalent chromium		
Metal collected	ug	7.5
Metal concentration	ug/dscm	3.37E+00
	ug/dscm @ 7% O ₂	4.03E+00
Metal emission rate	lb/h	4.91E-05
	g/s	6.18E-06

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-8. Particulate Matter, Hydrogen Chloride, and Chlorine Emissions Summary – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	5,030
	acfm	11,320
	dscm/min	142.45
Stack gas temperature	°F	175
Stack gas velocity	ft/min	3,606
Stack gas sample volume	dscf	72.660
	dscm	2.058
Isokinetic	%	93.7
Stack gas moisture content	vol %	45.9
Stack gas carbon dioxide content	vol %, dry	6.3
Stack gas oxygen content	vol %, dry	9.6
Hydrogen chloride and chlorine		
HCl collected	mg	11.8
Cl ₂ collected	mg	1.95
Stack gas HCl concentration	mg/dscm	5.73E+00
	mg/dscm @7% O ₂	7.04E+00
Stack gas HCl emission rate	lb/h	1.08E-01
	kg/h	4.90E-02
	g/s	1.36E-02
Stack gas Cl ₂ concentration	mg/dscm	9.48E-01
	mg/dscm @7% O ₂	1.16E+00
Stack gas Cl ₂ emission rate	lb/h	1.79E-02
	kg/h	8.10E-03
	g/s	2.25E-03
Stack gas HCl+Cl ₂ concentration expressed as HCl equivalents	ppmv, dry	4.42E+00
	ppmv, dry @7% O ₂	5.43E+00
Particulate		
Particulate matter collected	mg	34.3
Particulate concentration	gr/dscf	7.29E-03
	gr/dscf @ 7% O ₂	8.95E-03
	mg/dscm	1.67E+01
	mg/dscm @ 7% O ₂	2.05E+01
Particulate emission rate	lb/h	3.14E-01
	kg/h	1.42E-01
	g/s	3.96E-02

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-9. Particulate Matter, Hydrogen Chloride, and Chlorine Emissions Summary – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	3,850
	acfm	8,580
	dscm/min	109.03
Stack gas temperature	°F	174
Stack gas velocity	ft/min	2,730
Stack gas sample volume	dscf	74.990
	dscm	2.124
Isokinetic	%	96.0
Stack gas moisture content	vol %	45.1
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	8.9
Hydrogen chloride and chlorine		
HCl collected	mg	6.95
Cl ₂ collected	mg	2.01
Stack gas HCl concentration	mg/dscm	3.27E+00
	mg/dscm @7% O ₂	3.79E+00
Stack gas HCl emission rate	lb/h	4.72E-02
	kg/h	2.14E-02
	g/s	5.95E-03
Stack gas Cl ₂ concentration	mg/dscm	9.46E-01
	mg/dscm @7% O ₂	1.10E+00
Stack gas Cl ₂ emission rate	lb/h	1.37E-02
	kg/h	6.19E-03
	g/s	1.72E-03
Stack gas HCl+Cl ₂ concentration expressed as HCl equivalents	ppmv, dry	2.80E+00
	ppmv, dry @7% O ₂	3.24E+00
Particulate		
Particulate matter collected	mg	19.4
Particulate concentration	gr/dscf	3.99E-03
	gr/dscf @ 7% O ₂	4.62E-03
	mg/dscm	9.13E+00
	mg/dscm @ 7% O ₂	1.06E+01
Particulate emission rate	lb/h	1.32E-01
	kg/h	5.98E-02
	g/s	1.66E-02

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-10. Particulate Matter, Hydrogen Chloride, and Chlorine Emissions Summary – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	120
Stack gas flow rate	dscfm	4,090
	acfm	8,970
	dscm/min	115.83
Stack gas temperature	°F	174
Stack gas velocity	ft/min	2,856
Stack gas sample volume	dscf	79.290
	dscm	2.246
Isokinetic	%	95.7
Stack gas moisture content	vol %	44.8
Stack gas carbon dioxide content	vol %, dry	7.0
Stack gas oxygen content	vol %, dry	9.3
Hydrogen chloride and chlorine		
HCl collected	mg	6.49
Cl ₂ collected	mg	1.94
Stack gas HCl concentration	mg/dscm	2.89E+00
	mg/dscm @7% O ₂	3.46E+00
Stack gas HCl emission rate	lb/h	4.43E-02
	kg/h	2.01E-02
	g/s	5.58E-03
Stack gas Cl ₂ concentration	mg/dscm	8.64E-01
	mg/dscm @7% O ₂	1.03E+00
Stack gas Cl ₂ emission rate	lb/h	1.32E-02
	kg/h	6.00E-03
	g/s	1.67E-03
Stack gas HCl+Cl ₂ concentration expressed as HCl equivalents	ppmv, dry	2.49E+00
	ppmv, dry @7% O ₂	2.98E+00
Particulate		
Particulate matter collected	mg	33.6
Particulate concentration	gr/dscf	6.54E-03
	gr/dscf @ 7% O ₂	7.83E-03
	mg/dscm	1.50E+01
	mg/dscm @ 7% O ₂	1.79E+01
Particulate emission rate	lb/h	2.29E-01
	kg/h	1.04E-01
	g/s	2.89E-02

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-11. Particle Size Distribution

Particle Size (um)	Wt%
0.1 - 0.5	6.9
0.5 - 1.0	2.4
1.0 - 5.0	34.8
5.0 - 10.0	17.9
10.0 - 100.0	38.0
>100.0	0.0
Total	100.0

Average particle size distribution. Values calculated as the weighted average of the filter and acetone probe rinse particles for each run.

Table 7-18. Total Volatile Organic Compound Emissions (C1 – C7) – Run 1

Volatile Compound	Bag Analytical Result (ppmv, dry)	Condensate Analytical Result (ug/sample)	Stack (a,b,c) Concentration (ppmv, dry)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Total C1	1.72	0	1.72E+00	1.15E+03	2.76E-03
Total C2	0.083 ND	0	< 8.30E-02	< 1.04E+02	< 2.49E-04
Total C3	0.11 ND	0	< 1.10E-01	< 2.02E+02	< 4.85E-04
Total C4	0.08 ND	0.042 ND	< 8.08E-02	< 1.96E+02	< 4.69E-04
Total C5	0.14 ND	0.02436 J,B	< 1.40E-01	< 4.22E+02	< 1.01E-03
Total C6	0.13 ND	0.03108 J	< 1.30E-01	< 4.68E+02	< 1.12E-03
Total C7	0.18 ND	0.0042 ND	< 1.80E-01	< 7.52E+02	< 1.80E-03
Total Volatile Organics	< 2.443	0.10164	< 2.44E+00	< 3.29E+03	< 7.90E-03

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 0.759 dry standard cubic feet
0.02 dry standard cubic meters
- (b) Stack gas flow rate 5,080 dry standard cubic feet per minute
2.40 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-19. Total Volatile Organic Compound Emissions (C1 – C7) – Run 2

Volatile Compound	Bag Analytical Result (ppmv, dry)	Condensate Analytical Result (ug/sample)	Stack (a,b,c) Concentration (ppmv, dry)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Total C1	1.76	0	1.76E+00	1.18E+03	2.14E-03
Total C2	0.083 ND	0	< 8.30E-02	< 1.04E+02	< 1.89E-04
Total C3	0.11 ND	0	< 1.10E-01	< 2.02E+02	< 3.68E-04
Total C4	0.08 ND	0.042 ND	< 8.07E-02	< 1.95E+02	< 3.56E-04
Total C5	0.14 ND	0.01386 J,B	< 1.40E-01	< 4.21E+02	< 7.68E-04
Total C6	0.13 ND	0.03654 J	< 1.30E-01	< 4.68E+02	< 8.53E-04
Total C7	0.18 ND	0.0042 ND	< 1.80E-01	< 7.52E+02	< 1.37E-03
Total Volatile Organics	< 2.483	0.0966	< 2.48E+00	< 3.32E+03	< 6.05E-03

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume
 0.894 dry standard cubic feet
 0.03 dry standard cubic meters
- (b) Stack gas flow rate
 3,860 dry standard cubic feet per minute
 1.82 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-20. Total Volatile Organic Compound Emissions (C1 – C7) – Run 3

Volatile Compound	Bag Analytical Result (ppmv, dry)	Condensate Analytical Result (ug/sample)	Stack (a,b,c) Concentration (ppmv, dry)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Total C1	1.68	0	1.68E+00	1.12E+03	2.15E-03
Total C2	0.083 ND	0	< 8.30E-02	< 1.04E+02	< 1.99E-04
Total C3	0.11 ND	0	< 1.10E-01	< 2.02E+02	< 3.87E-04
Total C4	0.08 ND	0.042 ND	< 8.06E-02	< 1.95E+02	< 3.74E-04
Total C5	0.14 ND	0.0126 J,B	< 1.40E-01	< 4.21E+02	< 8.07E-04
Total C6	0.13 ND	0.03906 J	< 1.30E-01	< 4.68E+02	< 8.97E-04
Total C7	0.18 ND	0.0042 ND	< 1.80E-01	< 7.52E+02	< 1.44E-03
Total Volatile Organics	< 2.403	0.09786	< 2.40E+00	< 3.26E+03	< 6.26E-03

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume
 1.065 dry standard cubic feet
 0.03 dry standard cubic meters
- (b) Stack gas flow rate
 4,060 dry standard cubic feet per minute
 1.92 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-21. Total Semivolatile and Nonvolatile Organic Emissions – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	5,080
	acfm	11,370
	dscm/min	143.87
Stack gas temperature	°F	175
Stack gas velocity	ft/min	3,618
Stack gas sample volume	dscf	134.440
	dscm	3.807
Isokinetic	%	97.7
Stack gas moisture content	vol %	45.5
Stack gas carbon dioxide content	vol %, dry	6.4
Stack gas oxygen content	vol %, dry	9.8
Total Semivolatile Organics by TCO		
Total semivolatiles collected	ug	5320
TCO concentration	ug/dscm	1.40E+03
	ug/dscm @7% O ₂	1.75E+03
TCO emission rate	lb/h	2.66E-02
	kg/h	1.21E-02
	g/s	3.35E-03
Total Nonvolatile Organics by GRAV		
Total nonvolatiles collected	ug	3050
GRAV concentration	ug/dscm	8.01E+02
	ug/dscm @7% O ₂	1.00E+03
GRAV emission rate	lb/h	1.52E-02
	kg/h	6.92E-03
	g/s	1.92E-03

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-22. Total Semivolatile and Nonvolatile Organic Emissions – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	3,860
	acfm	8,610
	dscm/min	109.32
Stack gas temperature	°F	174
Stack gas velocity	ft/min	2,742
Stack gas sample volume	dscf	120.300
	dscm	3.407
Isokinetic	%	98.9
Stack gas moisture content	vol %	45.1
Stack gas carbon dioxide content	vol %, dry	7.2
Stack gas oxygen content	vol %, dry	8.9
Total Semivolatile Organics by TCO		
Total semivolatiles collected	ug	2830
TCO concentration	ug/dscm	8.31E+02
	ug/dscm @7% O ₂	9.61E+02
TCO emission rate	lb/h	1.20E-02
	kg/h	5.45E-03
	g/s	1.51E-03
Total Nonvolatile Organics by GRAV		
Total nonvolatiles collected	ug	2260
GRAV concentration	ug/dscm	6.63E+02
	ug/dscm @7% O ₂	7.68E+02
GRAV emission rate	lb/h	9.59E-03
	kg/h	4.35E-03
	g/s	1.21E-03

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-23. Total Semivolatile and Nonvolatile Organic Emissions – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	4,060
	acfm	8,890
	dscm/min	114.98
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,832
Stack gas sample volume	dscf	125.030
	dscm	3.541
Isokinetic	%	97.7
Stack gas moisture content	vol %	44.5
Stack gas carbon dioxide content	vol %, dry	7.1
Stack gas oxygen content	vol %, dry	9.3
Total Semivolatile Organics by TCO		
Total semivolatiles collected	ug	1924
TCO concentration	ug/dscm	5.43E+02
	ug/dscm @7% O ₂	6.50E+02
TCO emission rate	lb/h	8.26E-03
	kg/h	3.75E-03
	g/s	1.04E-03
Total Nonvolatile Organics by GRAV		
Total nonvolatiles collected	ug	2250
GRAV concentration	ug/dscm	6.35E+02
	ug/dscm @7% O ₂	7.60E+02
GRAV emission rate	lb/h	9.66E-03
	kg/h	4.38E-03
	g/s	1.22E-03

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute
 dscm = Dry standard cubic meters

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-24. PCDD/PCDF Emission Summary – Run 1

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	5,290
	acfm	11,760
Stack gas temperature	°F	176
Stack gas velocity	ft/min	3,744
Stack gas sample volume	dscf	139,210
	dscm	3,943
Isokinetic	%	101.2
Stack gas moisture content	vol%	45.2
Stack gas carbon dioxide	vol %, dry	6.4
Stack gas oxygen	vol %, dry	9.8
PCDD/PCDF		
Total PCDD/PCDF	pg/sample	< 12288
Stack gas PCDD/PCDF concentration	ng/dscm	< 3.12E+00
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 3.90E+00
PCDD/PCDF emission rate	g/s	< 7.78E-09
PCDD/PCDF Toxic Equivalents as 2,3,7,8-TCDD		
Stack gas PCDD/PCDF concentration	ng/dscm	< 5.23E-02
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 6.53E-02
PCDD/PCDF emission rate	g/s	< 1.30E-10

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-25. PCDD/PCDF Emission Summary – Run 2

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	3,780
	acfm	8,320
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,646
Stack gas sample volume	dscf	119.220
	dscm	3.376
Isokinetic	%	100.9
Stack gas moisture content	vol%	44.4
Stack gas carbon dioxide	vol %, dry	7.2
Stack gas oxygen	vol %, dry	8.9
PCDD/PCDF		
Total PCDD/PCDF	pg/sample	< 7223.8
Stack gas PCDD/PCDF concentration	ng/dscm	< 2.12E+00
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 2.45E+00
PCDD/PCDF emission rate	g/s	< 3.78E-09
PCDD/PCDF Toxic Equivalents as 2,3,7,8-TCDD		
Stack gas PCDD/PCDF concentration	ng/dscm	< 4.52E-02
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 5.23E-02
PCDD/PCDF emission rate	g/s	< 8.07E-11

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-26. PCDD/PCDF Emission Summary – Run 3

Parameter	Units	Measured Value
Stack Sampling Parameters		
Net sampling time	minutes	240
Stack gas flow rate	dscfm	4,040
	acfm	8,850
Stack gas temperature	°F	175
Stack gas velocity	ft/min	2,820
Stack gas sample volume	dscf	126.180
	dscm	3.573
Isokinetic	%	99.9
Stack gas moisture content	vol%	44.5
Stack gas carbon dioxide	vol %, dry	7.1
Stack gas oxygen	vol %, dry	9.3
PCDD/PCDF		
Total PCDD/PCDF	pg/sample	< 9067.1
Stack gas PCDD/PCDF concentration	ng/dscm	< 2.49E+00
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 2.98E+00
PCDD/PCDF emission rate	g/s	< 4.75E-09
PCDD/PCDF Toxic Equivalents as 2,3,7,8-TCDD		
Stack gas PCDD/PCDF concentration	ng/dscm	< 5.23E-02
Stack gas PCDD/PCDF concentration	ng/dscm @7% O ₂	< 6.25E-02
PCDD/PCDF emission rate	g/s	< 9.96E-11

Note: dscf = Dry standard cubic feet
 dscfm = Dry standard cubic feet per minute
 acfm = Actual cubic feet per minute

Standard conditions are 68°F, 29.92 in. Hg (20°C, 760 mm Hg)

Table 7-27. PCDD/PCDF Congener and TEQ Emissions – Run 1

Congener No.	PCDD/PCDF Compound	Analytical Result (pg/sample)		Stack (a,b,c) Concentration (ng/dscm)	2,3,7,8-TCDD Toxicity Equivalence Factor	Stack Concentration Toxic Equivalents (ng/dscm)	Emission Rate as 2,3,7,8-TCDD (g/s)
		Front Half	Back Half				
PCDDs							
1	2,3,7,8-TCDD	10 ND	19 Q	< 4.82E-03	1	< 4.82E-03	< 1.20E-11
	Other TCDD	0	1681	4.26E-01			
	Total TCDD	4 Q,J	1700 Q	4.32E-01			
2	1,2,3,7,8-PeCDD	50 ND	33 J	< 8.37E-03	0.5	< 4.19E-03	< 1.05E-11
	Other PeCDD	0	547	1.39E-01			
	Total PeCDD	8.2 Q,J	580 Q	1.49E-01			
3	1,2,3,4,7,8-HxCDD	50 ND	11 J	< 2.79E-03	0.1	< 2.79E-04	< 6.97E-13
4	1,2,3,6,7,8-HxCDD	50 ND	9.6 J	< 2.43E-03	0.1	< 2.43E-04	< 6.08E-13
5	1,2,3,7,8,9-HxCDD	50 ND	16 J	< 4.06E-03	0.1	< 4.06E-04	< 1.01E-12
	Other HxCDD	0	123.4	3.13E-02			
	Total HxCDD	6.3 Q,J	160 Q	4.22E-02			
6	1,2,3,4,6,7,8-HpCDD	6.7 J	24 B,J	7.79E-03	0.01	7.79E-05	1.94E-13
	Other HpCDD	4.3	20	6.16E-03			
	Total HpCDD	11 J	44 J,B	1.40E-02			
7	OCDD	22 Q,B,J	27 B,J	1.24E-02	0.001	1.24E-05	3.10E-14
	Total PCDDs(d)	< 51.5	2511	< 6.50E-01		< 1.00E-02	< 2.50E-11
PCDFs							
8	2,3,7,8-TCDF	2.4 Q,J	230 Q	5.89E-02	0.1	5.89E-03	1.47E-11
	Other TCDF	12.6	5770	1.47E+00			
	Total TCDF	15 Q,J	6000 Q	1.53E+00			
9	1,2,3,7,8-PeCDF	3.3 Q,J	170 Q	4.40E-02	0.05	2.20E-03	5.49E-12
10	2,3,4,7,8-PeCDF	2.9 Q,J	190	4.89E-02	0.5	2.45E-02	6.11E-11
	Other PeCDF	22.8	2240	5.74E-01			
	Total PeCDF	29 Q	2600 Q	6.67E-01			
11	1,2,3,4,7,8-HxCDF	5.7 Q,J	200 Q	5.22E-02	0.1	5.22E-03	1.30E-11
12	1,2,3,6,7,8-HxCDF	3.7 Q,J	100	2.63E-02	0.1	2.63E-03	6.57E-12
13	2,3,4,6,7,8-HxCDF	2.7 B,J	47 B,J	1.26E-02	0.1	1.26E-03	3.15E-12
14	1,2,3,7,8,9-HxCDF	50 ND	5.5 B,J	< 1.40E-03	0.1	< 1.40E-04	< 3.48E-13
	Other HxCDF	0	477.5	1.21E-01			
	Total HxCDF	21 Q,J,B	830 Q,B	2.16E-01			
15	1,2,3,4,6,7,8-HpCDF	8 Q,B,J	150 B	4.01E-02	0.01	4.01E-04	1.00E-12
16	1,2,3,4,7,8,9-HpCDF	50 ND	10 Q,J	< 2.54E-03	0.01	< 2.54E-05	< 6.33E-14
	Other HpCDF	0	40	1.01E-02			
	Total HpCDF	8 Q,B,J	200 B,Q	5.28E-02			
17	OCDF	8.5 Q,B,J	14 B,J	5.71E-03	0.001	5.71E-06	1.43E-14
	Total PCDFs(e)	< 81.5	9644	< 2.47E+00		< 4.22E-02	< 1.05E-10
	Total PCDD/PCDF	< 133	12155	< 3.12E+00		< 5.23E-02	< 1.30E-10

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 139,210 dry standard cubic feet
3.94 dry standard cubic meters
- (b) Stack gas flow rate 5,290 dry standard cubic feet per minute
2.50 dry standard cubic meters per second

(c) For non-detects, stack concentrations and emissions are calculated using zero.
 If the sum of the detection limits of the individual isomers for a given dioxin or furan exceeded the detection limit of the total it was assumed that these individual isomers, when added, constituted the entire total so that any contribution to the total by "other" isomers would be zero.

(d) Total PCDDs = Total TCDD + Total PeCDD + Total HxCDD + Total HpCDD + OCDD

(e) Total PCDFs = Total TCDF + Total PeCDF + Total HxCDF + Total HpCDF + OCDF

Table 7-28. PCDD/PCDF Congener and TEQ Emissions – Run 2

Congener No.	PCDD/PCDF Compound	Analytical Result (pg/sample)		Stack (a,b,c) Concentration (ng/dscm)	2,3,7,8-TCDD Toxicity Equivalence Factor	Stack Concentration Toxic Equivalents (ng/dscm)	Emission Rate as 2,3,7,8-TCDD (g/s)
		Front Half	Back Half				
PCDDs							
1	2,3,7,8-TCDD	10 ND	9.2 Q,J	< 2.72E-03	1	< 2.72E-03	< 4.86E-12
	Other TCDD	0	490.8	1.45E-01			
	Total TCDD	10 ND	500 Q	< 1.48E-01			
2	1,2,3,7,8-PeCDD	50 ND	18 J	< 5.33E-03	0.5	< 2.67E-03	< 4.76E-12
	Other PeCDD	0	232	6.87E-02			
	Total PeCDD	1.3 Q,J	250 Q	7.44E-02			
3	1,2,3,4,7,8-HxCDD	50 ND	8.2 J	< 2.43E-03	0.1	< 2.43E-04	< 4.33E-13
4	1,2,3,6,7,8-HxCDD	50 ND	8.5 J	< 2.52E-03	0.1	< 2.52E-04	< 4.49E-13
5	1,2,3,7,8,9-HxCDD	50 ND	13 J	< 3.85E-03	0.1	< 3.85E-04	< 6.87E-13
	Other HxCDD	0	90.3	2.67E-02			
	Total HxCDD	50 ND	120 Q,J	< 3.55E-02			
6	1,2,3,4,6,7,8-HpCDD	50 ND	23 B,J	< 6.81E-03	0.01	< 6.81E-05	< 1.22E-13
	Other HpCDD	0	19	5.63E-03			
	Total HpCDD	2.2 Q,J	42 J,B	1.31E-02			
7	OCDD	17 B,J	24 B,J	1.21E-02	0.001	1.21E-05	2.17E-14
	Total PCDDs(d)	< 80.5	936	< 2.83E-01		< 6.35E-03	< 1.13E-11
PCDFs							
8	2,3,7,8-TCDF	10 ND	130 Q	< 3.85E-02	0.1	< 3.85E-03	< 6.87E-12
	Other TCDF	0	2970	8.80E-01			
	Total TCDF	10 ND	3100 Q	< 9.18E-01			
9	1,2,3,7,8-PeCDF	50 ND	140	< 4.15E-02	0.05	< 2.07E-03	< 3.70E-12
10	2,3,4,7,8-PeCDF	50 ND	150	< 4.44E-02	0.5	< 2.22E-02	< 3.96E-11
	Other PeCDF	0	1710	5.06E-01			
	Total PeCDF	0.8 Q,J	2000 Q	5.93E-01			
11	1,2,3,4,7,8-HxCDF	2.1 Q,J	190	5.69E-02	0.1	5.69E-03	1.02E-11
12	1,2,3,6,7,8-HxCDF	1.6 Q,J	98	2.95E-02	0.1	2.95E-03	5.26E-12
13	2,3,4,6,7,8-HxCDF	50 ND	47 B,J	< 1.39E-02	0.1	< 1.39E-03	< 2.48E-12
14	1,2,3,7,8,9-HxCDF	50 ND	6 Q,B,J	< 1.78E-03	0.1	< 1.78E-04	< 3.17E-13
	Other HxCDF	0	489	1.45E-01			
	Total HxCDF	5.3 J,Q	830 B,Q	2.47E-01			
15	1,2,3,4,6,7,8-HpCDF	3.7 Q,B,J	160 B	4.85E-02	0.01	4.85E-04	8.65E-13
16	1,2,3,4,7,8,9-HpCDF	50 ND	18 J	< 5.33E-03	0.01	< 5.33E-05	< 9.51E-14
	Other HpCDF	0	52	1.54E-02			
	Total HpCDF	3.7 Q,B,J	230 B	6.92E-02			
17	OCDF	4.5 Q,B,J	23 B,J	8.14E-03	0.001	8.14E-06	1.45E-14
	Total PCDFs(e)	< 24.3	6183	< 1.84E+00		< 3.89E-02	< 6.94E-11
	Total PCDD/PCDF	< 104.8	7119	< 2.12E+00		< 4.52E-02	< 8.07E-11

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 119,220 dry standard cubic feet
 3.38 dry standard cubic meters
 (b) Stack gas flow rate 3,780 dry standard cubic feet per minute
 1.78 dry standard cubic meters per second

(c) For non-detects, stack concentrations and emissions are calculated using zero.
 If the sum of the detection limits of the individual isomers for a given dioxin or furan exceeded the detection limit of the total it was assumed that these individual isomers, when added, constituted the entire total so that any contribution to the total by "other" isomers would be zero.

(d) Total PCDDs = Total TCDD + Total PeCDD + Total HxCDD + Total HpCDD + OCDD

(e) Total PCDFs = Total TCDF + Total PeCDF + Total HxCDF + Total HpCDF + OCDF

Table 7-29. PCDD/PCDF Congener and TEQ Emissions – Run 3

Congener No.	PCDD/PCDF Compound	Analytical Result (pg/sample)		Stack (a,b,c) Concentration (ng/dscm)	2,3,7,8-TCDD Toxicity Equivalence Factor	Stack Concentration Toxic Equivalents (ng/dscm)	Emission Rate as 2,3,7,8-TCDD (g/s)
		Front Half	Back Half				
PCDDs							
1	2,3,7,8-TCDD	10 ND	12 Q	< 3.36E-03	1	< 3.36E-03	< 6.40E-12
	Other TCDD	0	398	< 1.11E-01			
	Total TCDD	10 ND	410 Q	< 1.15E-01			
2	1,2,3,7,8-PeCDD	50 ND	22 J	< 6.16E-03	0.5	< 3.08E-03	< 5.87E-12
	Other PeCDD	0	228	< 6.38E-02			
	Total PeCDD	50 ND	250 Q	< 7.00E-02			
3	1,2,3,4,7,8-HxCDD	50 ND	7.3 Q,J	< 2.04E-03	0.1	< 2.04E-04	< 3.90E-13
4	1,2,3,6,7,8-HxCDD	50 ND	9.7 Q,J	< 2.71E-03	0.1	< 2.71E-04	< 5.18E-13
5	1,2,3,7,8,9-HxCDD	50 ND	16 J	< 4.48E-03	0.1	< 4.48E-04	< 8.54E-13
	Other HxCDD	0	97	< 2.71E-02			
	Total HxCDD	50 ND	130 Q,J	< 3.64E-02			
6	1,2,3,4,6,7,8-HpCDD	2.2 J	26 B,J	< 7.89E-03	0.01	< 7.89E-05	< 1.50E-13
	Other HpCDD	0	24	< 6.72E-03			
	Total HpCDD	2.2 J	50 J,B	< 1.46E-02			
7	OCDD	18 B,J	26 B,J	< 1.23E-02	0.001	< 1.23E-05	< 2.35E-14
	Total PCDDs(d)	< 130.2	866	< 2.48E-01		< 7.45E-03	< 1.42E-11
PCDFs							
8	2,3,7,8-TCDF	10 ND	160 Q	< 4.48E-02	0.1	< 4.48E-03	< 8.54E-12
	Other TCDF	0	3840	< 1.07E+00			
	Total TCDF	10 ND	4000 Q	< 1.12E+00			
9	1,2,3,7,8-PeCDF	50 ND	190	< 5.32E-02	0.05	< 2.66E-03	< 5.07E-12
10	2,3,4,7,8-PeCDF	50 ND	180	< 5.04E-02	0.5	< 2.52E-02	< 4.80E-11
	Other PeCDF	0	2230	< 6.24E-01			
	Total PeCDF	2 Q,J	2600	< 7.28E-01			
11	1,2,3,4,7,8-HxCDF	50 ND	230	< 6.44E-02	0.1	< 6.44E-03	< 1.23E-11
12	1,2,3,6,7,8-HxCDF	50 ND	130	< 3.64E-02	0.1	< 3.64E-03	< 6.94E-12
13	2,3,4,6,7,8-HxCDF	50 ND	56 B	< 1.57E-02	0.1	< 1.57E-03	< 2.99E-12
14	1,2,3,7,8,9-HxCDF	50 ND	8.4 B,J	< 2.35E-03	0.1	< 2.35E-04	< 4.48E-13
	Other HxCDF	0	675.6	< 1.89E-01			
	Total HxCDF	50 ND	1100 B	< 3.08E-01			
15	1,2,3,4,6,7,8-HpCDF	3.5 Q,B,J	190 B	< 5.41E-02	0.01	< 5.41E-04	< 1.03E-12
16	1,2,3,4,7,8,9-HpCDF	50 ND	21 J	< 5.88E-03	0.01	< 5.88E-05	< 1.12E-13
	Other HpCDF	0	69	< 1.93E-02			
	Total HpCDF	3.5 Q,B,J	280 B	< 7.93E-02			
17	OCDF	3.4 Q,B,J	22 B,J	< 7.11E-03	0.001	< 7.11E-06	< 1.36E-14
	Total PCDFs(e)	< 68.9	8002	< 2.24E+00		< 4.48E-02	< 8.54E-11
	Total PCDD/PCDF	< 199.1	8868	< 2.49E+00		< 5.23E-02	< 9.96E-11

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 126.180 dry standard cubic feet
3.57 dry standard cubic meters
- (b) Stack gas flow rate 4,040 dry standard cubic feet per minute
1.91 dry standard cubic meters per second

(c) For non-detects, stack concentrations and emissions are calculated using zero.
If the sum of the detection limits of the individual isomers for a given dioxin or furan exceeded the detection limit of the total it was assumed that these individual isomers, when added, constituted the entire total so that any contribution to the total by "other" isomers would be zero.

(d) Total PCDDs = Total TCDD + Total PeCDD + Total HxCDD + Total HpCDD + OCDD

(e) Total PCDFs = Total TCDF + Total PeCDF + Total HxCDF + Total HpCDF + OCDF

Table 7-30. PAH Compound Emissions – Run 1

PAH Compound	Front Half Analytical Result (ng/sample)	Back Half Analytical Result (ng/sample)	Condensate Analytical Result (ng/sample)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Standard Target Analytes					
Acenaphthene	3.4 BJ	3.5 BJ	1.5 J	2.29E-03	5.51E-09
Acenaphthylene	9.1 J	14 J	0.29 ND	< 6.39E-03	< 1.53E-08
Anthracene	4 J	28	7.8 J	1.09E-02	2.61E-08
Benzo(a)anthracene	1.7 BJ	5.4 J	0.48 ND	< 2.07E-03	< 4.97E-09
Benzo(b)fluoranthene	4.2 BJ	40 B	5.8 J	1.37E-02	3.28E-08
Benzo(k)fluoranthene	3.1 BJ	4.3 J	5.5 J	3.52E-03	8.46E-09
Benzo(g,h,i)perylene	5.6 J	4 J	15 BJ	6.72E-03	1.61E-08
Benzo(a)pyrene	2.7 BJ	2.2 BJ	3.4 BJ	2.27E-03	5.45E-09
Benzo(e)pyrene	4.5 BJ	4.4 BJ	5.1 BJ	3.82E-03	9.18E-09
Chrysene	3.5 BJ	18 J	4.7 BJ	7.15E-03	1.72E-08
Dibenzo(a,h)anthracene	0.32 ND	0.5 ND	0.65 ND	< 4.01E-04	< 9.64E-10
Fluoranthene	27 B	100 B	26 B	4.18E-02	1.00E-07
Fluorene	15 BJ	11 BJ	3.3 J	8.00E-03	1.92E-08
Indeno(1,2,3-cd)pyrene	3.3 BJ	3.8 J	4.7 BJ	3.22E-03	7.74E-09
2-Methylnaphthalene	31 BJ	80 BJ	13 BJ	3.39E-02	8.13E-08
Naphthalene	40 BJ	880 B	30 BJ	2.59E-01	6.23E-07
Phenanthrene	140 B	300 B	39 BJ	1.31E-01	3.14E-07
Pyrene	25 BJ	110 B	20 BJ	4.23E-02	1.02E-07
Special Target Analytes					
Perylene	0.91 ND	3.5 BJ	1.7 ND	< 1.67E-03	< 4.01E-09
Total PAHs	< 324.33	1612.6	187.92	< 5.80E-01	< 1.39E-06

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 129.310 dry standard cubic feet
3.66 dry standard cubic meters
- (b) Stack gas flow rate 5,090 dry standard cubic feet per minute
2.40 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-31. PAH Compound Emissions – Run 2

PAH Compound	Front Half Analytical Result (ng/sample)	Back Half Analytical Result (ng/sample)	Condensate Analytical Result (ng/sample)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Standard Target Analytes					
Acenaphthene	1.1 BJ	3.3 BJ	1.5 J	1.67E-03	3.05E-09
Acenaphthylene	0.28 ND	7.8 J	0.23 ND	< 2.35E-03	< 4.29E-09
Anthracene	0.44 ND	8.1 J	3.5 J	< 3.41E-03	< 6.22E-09
Benzo(a)anthracene	0.36 ND	0.35 ND	0.45 ND	< 3.28E-04	< 5.99E-10
Benzo(b)fluoranthene	0.83 ND	55 B	3.9 J	< 1.69E-02	< 3.09E-08
Benzo(k)fluoranthene	1.1 ND	4.6 J	1.2 ND	< 1.95E-03	< 3.57E-09
Benzo(g,h,i)perylene	0.75 ND	4.4 J	18 BJ	< 6.55E-03	< 1.20E-08
Benzo(a)pyrene	1.4 ND	1.7 ND	2.7 BJ	< 1.64E-03	< 3.00E-09
Benzo(e)pyrene	1.1 ND	1.5 ND	5.3 BJ	< 2.23E-03	< 4.08E-09
Chrysene	0.39 ND	21	3.1 BJ	< 6.93E-03	< 1.27E-08
Dibenzo(a,h)anthracene	0.41 ND	0.92 ND	0.45 ND	< 5.04E-04	< 9.20E-10
Fluoranthene	4.4 BJ	32 B	18 BJ	1.54E-02	2.81E-08
Fluorene	3.3 BJ	10 BJ	2.8 J	4.55E-03	8.32E-09
Indeno(1,2,3-cd)pyrene	0.76 ND	1.4 ND	5.3 BJ	< 2.11E-03	< 3.86E-09
2-Methylnaphthalene	12 BJ	52 BJ	13 BJ	2.18E-02	3.98E-08
Naphthalene	23 BJ	1900 B	34 BJ	5.54E-01	1.01E-06
Phenanthrene	25 BJ	96 B	27 BJ	4.19E-02	7.65E-08
Pyrene	6.4 BJ	30 BJ	15 BJ	1.45E-02	2.66E-08
Special Target Analytes					
Perylene	1.4 ND	1.6 ND	1.3 ND	< 1.22E-03	< 2.22E-09
Total PAHs	< 84.42	2231.67	156.73	< 7.00E-01	< 1.28E-06

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 124,810 dry standard cubic feet
3.53 dry standard cubic meters
- (b) Stack gas flow rate 3,870 dry standard cubic feet per minute
1.83 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-32. PAH Compound Emissions – Run 3

PAH Compound	Front Half Analytical Result (ng/sample)	Back Half Analytical Result (ng/sample)	Condensate Analytical Result (ng/sample)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Standard Target Analytes					
Acenaphthene	2 BJ	6.5 BJ	1.3 ND	< 2.87E-03	< 5.22E-09
Acenaphthylene	3.3 J	5.9 J	0.32 ND	< 2.79E-03	< 5.07E-09
Anthracene	0.37 ND	11 J	0.41 ND	< 3.45E-03	< 6.27E-09
Benzo(a)anthracene	0.21 ND	6.1 J	0.37 ND	< 1.96E-03	< 3.56E-09
Benzo(b)fluoranthene	4.1 BJ	40 B	2.3 J	1.36E-02	2.47E-08
Benzo(k)fluoranthene	1.1 ND	3.9 J	4.7 J	< 2.84E-03	< 5.16E-09
Benzo(g,h,i)perylene	7.5 J	3.7 J	0.67 ND	< 3.48E-03	< 6.32E-09
Benzo(a)pyrene	4.3 BJ	1.1 ND	1.9 ND	< 2.14E-03	< 3.89E-09
Benzo(e)pyrene	3.2 BJ	2.5 BJ	1.6 ND	< 2.14E-03	< 3.89E-09
Chrysene	0.23 ND	5.7 J	0.43 ND	< 1.86E-03	< 3.39E-09
Dibenzo(a,h)anthracene	0.35 ND	0.72 ND	0.65 ND	< 5.04E-04	< 9.16E-10
Fluoranthene	7.3 BJ	25 B	3.4 BJ	1.05E-02	1.90E-08
Fluorene	6.4 BJ	11 BJ	1.8 J	5.63E-03	1.02E-08
Indeno(1,2,3-cd)pyrene	4.1 BJ	3.1 J	0.68 J	2.31E-03	4.20E-09
2-Methylnaphthalene	17 BJ	67 BJ	15 BJ	2.90E-02	5.27E-08
Naphthalene	35 BJ	17000 B	72 BJ	5.01E+00	9.11E-06
Phenanthrene	49 B	65 B	5.8 BJ	3.51E-02	6.38E-08
Pyrene	5 BJ	28 BJ	3.1 BJ	1.06E-02	1.92E-08
Special Target Analytes					
Perylene	1.1 ND	66 B	1.8 ND	< 2.02E-02	< 3.67E-08
Total PAHs	< 151.56	17352.22	118.23	< 5.16E+00	< 9.38E-06

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 120.520 dry standard cubic feet
3.41 dry standard cubic meters
- (b) Stack gas flow rate 3,850 dry standard cubic feet per minute
1.82 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-33. PCB Emissions – Run 1

PCB Compound	Front Half Analytical Result (ng/sample)	Back Half Analytical Result (ng/sample)	Condensate Analytical Result (ng/sample)	Stack (a,b,c) Concentration (ng/dscm)	Emission Rate (g/s)
Co-Planar PCBs					
3,4,3',4'-Tetrachlorobiphenyl (IUPAC 77)	0.03 QB	0.36	0.021 QJ	1.12E-01	2.70E-10
3,4,4',5'-Tetrachlorobiphenyl (IUPAC 81)	0.0083 ND	0.06 QJ	0.01 ND	< 2.14E-02	< 5.14E-11
2,3,4,3',4'-Pentachlorobiphenyl (IUPAC 105)	0.022 QJ	0.067 J	0.035 BJ	3.39E-02	8.13E-11
2,3,4,5,4'-Pentachlorobiphenyl (IUPAC 114)	0.0069 ND	0.011 ND	0.0065 ND	< 6.66E-03	< 1.60E-11
2,4,5,3',4'-Pentachlorobiphenyl (IUPAC 118)	0.087 J	0.13 J	0.078 QBJ	8.06E-02	1.94E-10
3,4,5,2',4'-Pentachlorobiphenyl (IUPAC 123)	0.0075 ND	0.022 J	0.0067 ND	< 9.88E-03	< 2.37E-11
3,4,5,3',4'-Pentachlorobiphenyl (IUPAC 126)	0.0073 ND	0.091 QJ	0.0072 ND	< 2.88E-02	< 6.92E-11
2,3,4,5,3',4'-Hexachlorobiphenyl (IUPAC 156)	0.01 ND	0.061 QCJ	0.013 ND	< 2.29E-02	< 5.51E-11
2,3,4,3',4',5'-Hexachlorobiphenyl (IUPAC 157)	0.01 ND	0.061 QCJ	0.013 ND	< 2.29E-02	< 5.51E-11
2,4,5,3',4',5'-Hexachlorobiphenyl (IUPAC 167)	0.0073 ND	0.027 J	0.0091 ND	< 1.19E-02	< 2.85E-11
3,4,5,3',4',5'-Hexachlorobiphenyl (IUPAC 169)	0.0073 ND	0.02 ND	0.0098 ND	< 1.01E-02	< 2.43E-11
2,3,4,5,3',4',5'-Heptachlorobiphenyl (IUPAC 189)	0.0066 ND	0.013 ND	0.0061 ND	< 7.02E-03	< 1.69E-11
Total PCB Homologs					
Total Monochlorobiphenyls	0.67 B	6 B	0.23 BJ	1.88E+00	4.53E-09
Total Dichlorobiphenyls	9.6 QB	9.8 QB	2 BQ	5.84E+00	1.40E-08
Total Trichlorobiphenyls	11 QB	8 QB	3.8 BQ	6.23E+00	1.50E-08
Total Tetrachlorobiphenyls	2.2 QB	4 BQ	2.5 BQ	2.38E+00	5.71E-09
Total Pentachlorobiphenyls	0.49 QJB	1 QB	0.75 JQB	6.12E-01	1.47E-09
Total Hexachlorobiphenyls	0.093 QJ	0.33 QBJ	0.23 QBJ	1.78E-01	4.28E-10
Total Heptachlorobiphenyls	0.21 ND	0.13 QJ	0.024 QBJ	< 9.94E-02	< 2.39E-10
Total Octachlorobiphenyls	0.1 ND	0.16 ND	0.14 ND	< 1.09E-01	< 2.62E-10
Total Nonachlorobiphenyls	0.029 ND	0.054 ND	0.05 ND	< 3.63E-02	< 8.73E-11
Total Decachlorobiphenyl	0.0096 ND	0.016 ND	0.025 ND	< 1.38E-02	< 3.32E-11
Total PCBs	< 24.4016	29.49	9.749	< 1.74E+01	< 4.18E-08

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

(a) Stack gas sample volume

129.310 dry standard cubic feet

3.66 dry standard cubic meters

(b) Stack gas flow rate

5,090 dry standard cubic feet per minute

2.40 dry standard cubic meters per second

(c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-34. PCB Emissions – Run 2

PCB Compound	Front Half Analytical Result (ng/sample)	Back Half Analytical Result (ng/sample)	Condensate Analytical Result (ng/sample)	Stack (a,b,c) Concentration (ng/dscm)	Emission Rate (g/s)
Co-Planar PCBs					
3,4,3',4'-Tetrachlorobiphenyl (IUPAC 77)	0.0073 ND	0.17 J	0.018 QJ	< 5.53E-02	< 1.01E-10
3,4,4',5'-Tetrachlorobiphenyl (IUPAC 81)	0.0068 ND	0.019 QJ	0.0058 ND	< 8.94E-03	< 1.63E-11
2,3,4,3',4'-Pentachlorobiphenyl (IUPAC 105)	0.0061 ND	0.049 QJ	0.039 BJ	< 2.66E-02	< 4.86E-11
2,3,4,5,4'-Pentachlorobiphenyl (IUPAC 114)	0.0058 ND	0.01 ND	0.0075 QJ	< 6.59E-03	< 1.20E-11
2,4,5,3',4'-Pentachlorobiphenyl (IUPAC 118)	0.018 QJ	0.097 QJ	0.076 BJ	5.40E-02	9.87E-11
3,4,5,2',4'-Pentachlorobiphenyl (IUPAC 123)	0.0063 ND	0.01 ND	0.0036 ND	< 5.63E-03	< 1.03E-11
3,4,5,3',4'-Pentachlorobiphenyl (IUPAC 126)	0.0062 ND	0.069 J	0.0041 ND	< 2.24E-02	< 4.10E-11
2,3,4,5,3',4'-Hexachlorobiphenyl (IUPAC 156)	0.0091 ND	0.048 CJ	0.0069 ND	< 1.81E-02	< 3.31E-11
2,3,4,3',4',5'-Hexachlorobiphenyl (IUPAC 157)	0.0091 ND	0.048 CJ	0.0069 ND	< 1.81E-02	< 3.31E-11
2,4,5,3',4',5'-Hexachlorobiphenyl (IUPAC 167)	0.0063 ND	0.024 J	0.0049 ND	< 9.96E-03	< 1.82E-11
3,4,5,3',4',5'-Hexachlorobiphenyl (IUPAC 169)	0.0062 ND	0.019 ND	0.006 ND	< 8.83E-03	< 1.61E-11
2,3,4,5,3',4',5'-Heptachlorobiphenyl (IUPAC 189)	0.006 ND	0.011 ND	0.0034 ND	< 5.77E-03	< 1.05E-11
Total PCB Homologs					
Total Monochlorobiphenyls	0.061 QBJ	1.2 B	0.24 BJ	4.25E-01	7.76E-10
Total Dichlorobiphenyls	1.5 QB	6.4 QB	1.6 QB	2.69E+00	4.91E-09
Total Trichlorobiphenyls	1.6 BJQ	5.5 QB	2.9 BQ	2.83E+00	5.17E-09
Total Tetrachlorobiphenyls	0.38 QJB	2.8 BQ	2.1 BQ	1.49E+00	2.73E-09
Total Pentachlorobiphenyls	0.03 QJ	0.74 JQB	0.74 JQB	4.27E-01	7.80E-10
Total Hexachlorobiphenyls	0.028 QJ	0.43 BJQ	0.27 BJQ	2.06E-01	3.76E-10
Total Heptachlorobiphenyls	0.19 ND	0.16 QJ	0.03 JQB	< 1.08E-01	< 1.96E-10
Total Octachlorobiphenyls	0.089 ND	0.014 QJ	0.0099 QJ	< 3.19E-02	< 5.83E-11
Total Nonachlorobiphenyls	0.028 ND	0.039 ND	0.027 ND	< 2.66E-02	< 4.86E-11
Total Decachlorobiphenyl	0.0082 ND	0.02 QJ	0.011 ND	< 1.11E-02	< 2.03E-11
Total PCBs	< 3.9142	17.303	7.9279	< 8.25E+00	< 1.51E-08

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

(a) Stack gas sample volume

124.810 dry standard cubic feet

3.53 dry standard cubic meters

(b) Stack gas flow rate

3,870 dry standard cubic feet per minute

1.83 dry standard cubic meters per second

(c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-35. PCB Emissions – Run 3

PCB Compound	Front Half Analytical Result (ng/sample)	Back Half Analytical Result (ng/sample)	Condensate Analytical Result (ng/sample)	Stack (a,b,c) Concentration (ng/dscm)	Emission Rate (g/s)
Co-Planar PCBs					
3,4,3',4'-Tetrachlorobiphenyl (IUPAC 77)	0.017 QJ	0.12 QJ	0.0071 ND	< 4.22E-02	< 7.67E-11
3,4,4',5'-Tetrachlorobiphenyl (IUPAC 81)	0.0079 ND	0.061 ND	0.0064 ND	< 2.21E-02	< 4.01E-11
2,3,4,3',4'-Pentachlorobiphenyl (IUPAC 105)	0.0069 ND	0.093 J	0.017 QBJ	< 3.42E-02	< 6.22E-11
2,3,4,5,4'-Pentachlorobiphenyl (IUPAC 114)	0.0066 ND	0.012 ND	0.0081 QJ	< 7.82E-03	< 1.42E-11
2,4,5,3',4'-Pentachlorobiphenyl (IUPAC 118)	0.031 J	0.16 J	0.023 QBJ	6.27E-02	1.14E-10
3,4,5,2',4'-Pentachlorobiphenyl (IUPAC 123)	0.0069 ND	0.012 ND	0.017 QBJ	< 1.05E-02	< 1.91E-11
3,4,5,3',4'-Pentachlorobiphenyl (IUPAC 126)	0.0074 ND	0.043 QJ	0.0053 ND	< 1.63E-02	< 2.97E-11
2,3,4,5,3',4'-Hexachlorobiphenyl (IUPAC 156)	0.0091 ND	0.056 CJ	0.012 QCJ	< 2.26E-02	< 4.10E-11
2,3,4,3',4',5'-Hexachlorobiphenyl (IUPAC 157)	0.0091 ND	0.056 CJ	0.012 QCJ	< 2.26E-02	< 4.10E-11
2,4,5,3',4',5'-Hexachlorobiphenyl (IUPAC 167)	0.0067 ND	0.021 QJ	0.0058 ND	< 9.81E-03	< 1.78E-11
3,4,5,3',4',5'-Hexachlorobiphenyl (IUPAC 169)	0.0078 ND	0.021 ND	0.0083 ND	< 1.09E-02	< 1.98E-11
2,3,4,5,3',4',5'-Heptachlorobiphenyl (IUPAC 189)	0.0065 ND	0.013 ND	0.0045 ND	< 7.03E-03	< 1.28E-11
Total PCB Homologs					
Total Monochlorobiphenyls	0.18 QBJ	0.91 B	0.19 BJ	3.75E-01	6.81E-10
Total Dichlorobiphenyls	2.6 BQ	4.9 QB	0.68 QBJ	2.40E+00	4.36E-09
Total Trichlorobiphenyls	2.6 BQ	6.1 BQ	0.88 QBJ	2.81E+00	5.10E-09
Total Tetrachlorobiphenyls	0.51 QBJ	2.9 BQ	0.73 JQB	1.21E+00	2.20E-09
Total Pentachlorobiphenyls	0.058 QJ	0.95 JQB	0.28 QJB	3.77E-01	6.86E-10
Total Hexachlorobiphenyls	0.047 JQ	0.47 QBJ	0.1 QBJ	1.81E-01	3.29E-10
Total Heptachlorobiphenyls	0.2 ND	0.15 QJ	0.21 ND	< 1.64E-01	< 2.98E-10
Total Octachlorobiphenyls	0.094 ND	0.15 ND	0.1 ND	< 1.01E-01	< 1.83E-10
Total Nonachlorobiphenyls	0.03 ND	0.052 ND	0.032 ND	< 3.34E-02	< 6.07E-11
Total Decachlorobiphenyl	0.0086 ND	0.015 ND	0.013 ND	< 1.07E-02	< 1.95E-11
Total PCBs	< 6.3276	16.597	3.215	< 7.66E+00	< 1.39E-08

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

(a) Stack gas sample volume

120.520 dry standard cubic feet

3.41 dry standard cubic meters

(b) Stack gas flow rate

3,850 dry standard cubic feet per minute

1.82 dry standard cubic meters per second

(c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-36. Organochlorine Pesticide Emissions – Run 1

OCP Compound	Front Half Analytical Result (ug/sample)	Back Half Analytical Result (ug/sample)	Condensate Analytical Result (ug/sample)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Standard Target Analytes					
Aldrin	0.036 ND	0.014 ND	0.034 ND	< 2.41E-02	< 5.54E-08
a-BHC	0.026 ND	0.022 ND	0.016 ND	< 1.84E-02	< 4.22E-08
b-BHC	0.033 ND	0.063 ND	0.034 ND	< 3.73E-02	< 8.58E-08
g-BHC (Lindane)	0.014 ND	0.014 ND	0.012 ND	< 1.15E-02	< 2.64E-08
d-BHC	0.015 ND	0.022 J,COL	0.025 ND	< 1.78E-02	< 4.09E-08
a-Chlordane	0.013 ND	0.021 J,COL	0.014 ND	< 1.38E-02	< 3.17E-08
g-Chlordane	0.078 ND	0.043 ND	0.018 ND	< 3.99E-02	< 9.17E-08
4,4'-DDD	0.083 ND	0.093 ND	0.14 ND	< 9.07E-02	< 2.09E-07
4,4'-DDE	0.039 ND	0.052 J	0.028 ND	< 3.42E-02	< 7.85E-08
4,4'-DDT	0.023 ND	0.063 J,COL	0.026 J	< 3.22E-02	< 7.39E-08
Dieldrin	0.013 ND	0.015 ND	0.012 ND	< 1.15E-02	< 2.64E-08
Endosulfan I	0.013 ND	0.018 ND	0.014 ND	< 1.29E-02	< 2.97E-08
Endosulfan II	0.014 ND	0.06 J,COL	0.018 ND	< 2.64E-02	< 6.07E-08
Endosulfan sulfate	0.023 ND	0.013 ND	0.016 ND	< 1.49E-02	< 3.43E-08
Endrin	0.05 ND	0.063 ND	0.051 ND	< 4.71E-02	< 1.08E-07
Heptachlor	0.016 ND	0.013 ND	0.02 J,COL	< 1.41E-02	< 3.23E-08
Methoxychlor	0.038 ND	0.11 ND	0.037 ND	< 5.31E-02	< 1.22E-07
Special Target Analytes					
Chlorobenzilate	0.083 ND	0.093 ND	0.15 J,COL	< 9.36E-02	< 2.15E-07
Endrin aldehyde	0.018 ND	0.04 ND	0.02 J,B,COL	< 2.24E-02	< 5.15E-08
Endrin ketone	0.017 ND	0.017 ND	0.025 ND	< 1.69E-02	< 3.89E-08
Heptachlor epoxide	0.015 ND	0.042 J,COL	0.012 ND	< 1.98E-02	< 4.55E-08
Diallate	11 ND	9.7 ND	0.78 ND	< 6.17E+00	< 1.42E-05

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 122.990 dry standard cubic feet
3.48 dry standard cubic meters
- (b) Stack gas flow rate 4,870 dry standard cubic feet per minute
2.30 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-37. Organochlorine Pesticide Emissions – Run 2

OCP Compound	Front Half Analytical Result (ug/sample)	Back Half Analytical Result (ug/sample)	Condensate Analytical Result (ug/sample)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Standard Target Analytes					
Aldrin	0.036 ND	0.014 ND	0.034 ND	< 2.52E-02	< 4.62E-08
a-BHC	0.026 ND	0.022 ND	0.023 J	< 2.13E-02	< 3.91E-08
b-BHC	0.033 ND	0.063 ND	0.052 J,COL	< 4.45E-02	< 8.14E-08
g-BHC (Lindane)	0.014 ND	0.014 ND	0.012 ND	< 1.20E-02	< 2.20E-08
d-BHC	0.015 ND	0.019 ND	0.11 COL	< 4.33E-02	< 7.92E-08
a-Chlordane	0.013 ND	0.028 J,COL	0.014 ND	< 1.65E-02	< 3.03E-08
g-Chlordane	0.078 ND	0.043 ND	0.018 ND	< 4.18E-02	< 7.65E-08
4,4'-DDD	0.083 ND	0.093 ND	0.14 ND	< 9.49E-02	< 1.74E-07
4,4'-DDE	0.039 ND	0.052 J	0.028 ND	< 3.57E-02	< 6.55E-08
4,4'-DDT	0.023 ND	0.012 ND	0.022 ND	< 1.71E-02	< 3.14E-08
Dieldrin	0.013 ND	0.015 ND	0.012 ND	< 1.20E-02	< 2.20E-08
Endosulfan I	0.013 ND	0.018 ND	0.014 ND	< 1.35E-02	< 2.48E-08
Endosulfan II	0.014 ND	0.023 ND	0.018 ND	< 1.65E-02	< 3.03E-08
Endosulfan sulfate	0.023 ND	0.013 ND	0.016 ND	< 1.56E-02	< 2.86E-08
Endrin	0.05 ND	0.063 ND	0.051 ND	< 4.93E-02	< 9.02E-08
Heptachlor	0.016 ND	0.013 ND	0.11 COL	< 4.18E-02	< 7.65E-08
Methoxychlor	0.038 ND	0.11 ND	0.035 ND	< 5.50E-02	< 1.01E-07
Special Target Analytes					
Chlorobenzilate	0.083 ND	0.093 ND	0.13 ND	< 9.19E-02	< 1.68E-07
Endrin aldehyde	0.018 ND	0.04 ND	0.18 B,COL	< 7.15E-02	< 1.31E-07
Endrin ketone	0.017 ND	0.017 ND	0.025 ND	< 1.77E-02	< 3.25E-08
Heptachlor epoxide	0.015 ND	0.015 ND	0.025 J,COL	< 1.65E-02	< 3.03E-08
Diallate	11 ND	9.7 ND	0.78 ND	< 6.45E+00	< 1.18E-05

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 117.540 dry standard cubic feet
 3.33 dry standard cubic meters
- (b) Stack gas flow rate 3,880 dry standard cubic feet per minute
 1.83 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

Table 7-38. Organochlorine Pesticide Emissions – Run 3

OCP Compound	Front Half Analytical Result (ug/sample)	Back Half Analytical Result (ug/sample)	Condensate Analytical Result (ug/sample)	Stack (a,b,c) Concentration (ug/dscm)	Emission Rate (g/s)
Standard Target Analytes					
Aldrin	0.036 ND	0.014 ND	0.034 ND	< 2.36E-02	< 4.54E-08
a-BHC	0.026 ND	0.022 ND	0.016 ND	< 1.80E-02	< 3.46E-08
b-BHC	0.033 ND	0.074 J,COL	0.035 J,COL	< 3.99E-02	< 7.68E-08
g-BHC (Lindane)	0.014 ND	0.014 ND	0.012 ND	< 1.12E-02	< 2.16E-08
d-BHC	0.015 ND	0.019 ND	0.078 J,COL	< 3.15E-02	< 6.06E-08
a-Chlordane	0.013 ND	0.016 ND	0.014 ND	< 1.21E-02	< 2.33E-08
g-Chlordane	0.078 ND	0.043 ND	0.018 ND	< 3.90E-02	< 7.52E-08
4,4'-DDD	0.083 ND	0.26 J,COL	0.14 ND	< 1.36E-01	< 2.61E-07
4,4'-DDE	0.039 ND	0.047 ND	0.028 ND	< 3.20E-02	< 6.17E-08
4,4'-DDT	0.023 ND	0.021 ND	0.023 ND	< 1.88E-02	< 3.62E-08
Dieldrin	0.013 ND	0.015 ND	0.012 ND	< 1.12E-02	< 2.16E-08
Endosulfan I	0.013 ND	0.018 ND	0.014 ND	< 1.26E-02	< 2.43E-08
Endosulfan II	0.014 ND	0.023 ND	0.018 ND	< 1.54E-02	< 2.98E-08
Endosulfan sulfate	0.023 ND	0.013 ND	0.016 ND	< 1.46E-02	< 2.81E-08
Endrin	0.05 ND	0.063 ND	0.051 ND	< 4.61E-02	< 8.87E-08
Heptachlor	0.016 ND	0.013 ND	0.056 J,COL	< 2.39E-02	< 4.60E-08
Methoxychlor	0.038 ND	0.11 ND	0.037 ND	< 5.20E-02	< 1.00E-07
Special Target Analytes					
Chlorobenzilate	0.083 ND	0.097 J,COL	0.14 ND	< 8.99E-02	< 1.73E-07
Endrin aldehyde	0.018 ND	0.04 ND	0.022 J,B,COL	< 2.25E-02	< 4.33E-08
Endrin ketone	0.017 ND	0.017 ND	0.025 ND	< 1.66E-02	< 3.19E-08
Heptachlor epoxide	0.015 ND	0.015 ND	0.013 J,COL	< 1.21E-02	< 2.33E-08
Diallate	11 ND	9.7 ND	0.78 ND	< 6.03E+00	< 1.16E-05

NOTE: All concentrations in this table are uncorrected for oxygen concentration.

- (a) Stack gas sample volume 125,710 dry standard cubic feet
3.56 dry standard cubic meters
- (b) Stack gas flow rate 4,080 dry standard cubic feet per minute
1.93 dry standard cubic meters per second
- (c) For non-detects, stack concentrations and emissions are calculated using the detection limit.

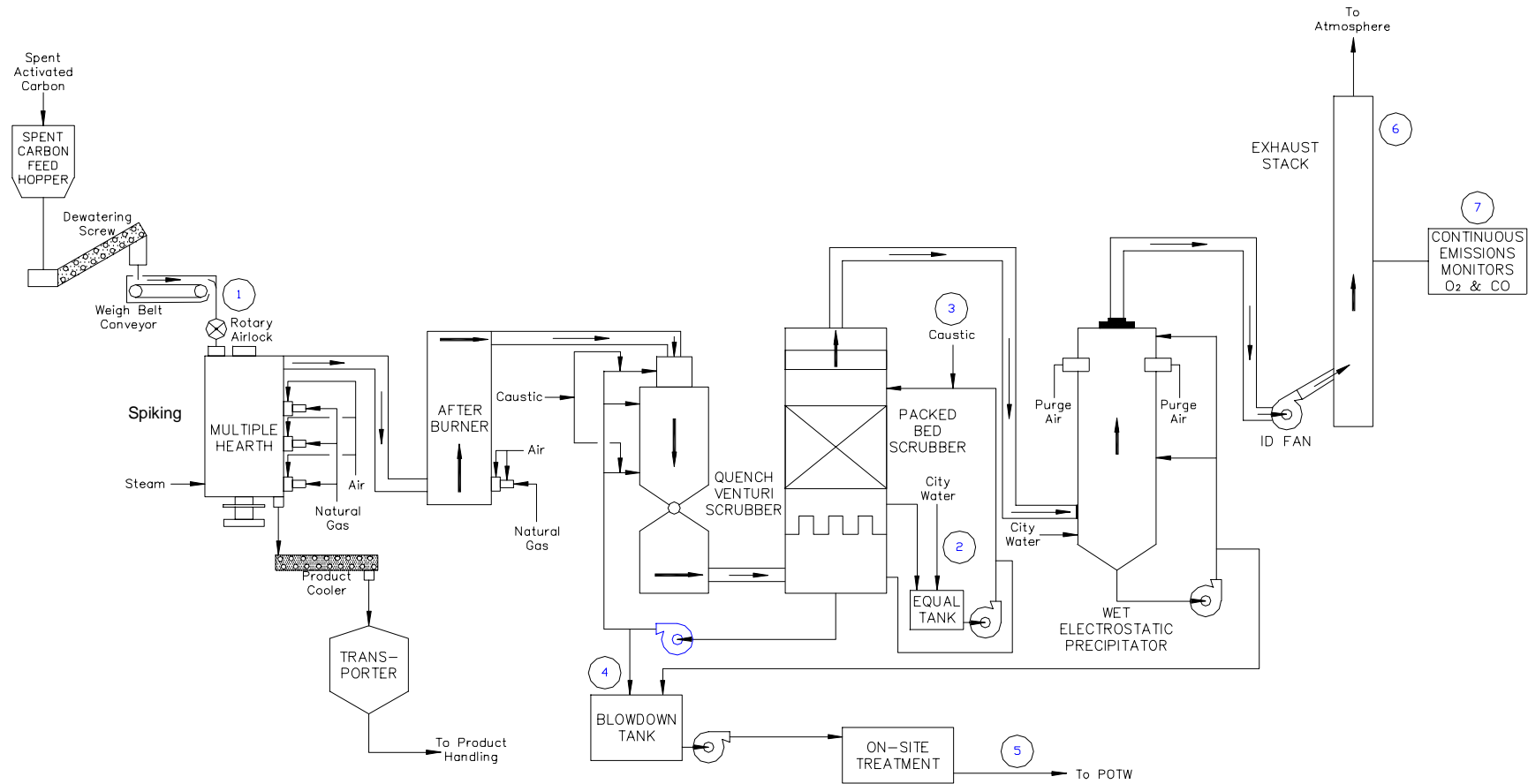


Figure 2-1. Sampling Locations.



US Filter Westates Carbon Reactivation Facility Description

NATURE OF BUSINESS

The USFilter Westates Parker, Arizona facility is a carbon reactivation facility, which reactivates granular activated carbon. Activated carbon is utilized in treatment equipment for the removal, by adsorption, of organic compounds from liquid and vapor phase process and waste streams. The reactivated carbon becomes spent after a period of time. Spent means that the activated carbon has reached its adsorptive capacity. Once the activated carbon is spent, it must be either disposed of or reactivated (recycled), which is a much more environmentally sound alternative, at a facility such as WCAI-Parker.

TYPES OF INDUSTRY SERVED

Activated carbon is used in treatment equipment to remove organic compounds from liquid and vapor phase waste streams. The treatment equipment is used in a wide variety of municipal and commercial applications. The industries which use this equipment, mainly to comply with the Clean Air Act and Clean Water Act, include petroleum refineries and marketing facilities, solvent cleaning facilities, auto manufacturing and repair facilities, aircraft manufacturing facilities and other facilities that generate organic waste streams. Additionally, activated carbon is used in a variety of environmental clean-up applications.

ONSITE FACILITIES

Spent carbon is received in containers and tank trucks which are approved for use by the U.S. Department of Transportation (DOT). After inspection and acceptance at the facility, the containerized spent carbon is transferred, via a hopper using a slurry method, into one of four spent carbon storage tanks.

From the spent carbon storage tanks the water-carbon slurry is pumped to a reactivation unit feed tank. Prior to introduction into a Nichols design multiple hearth furnace, the water-carbon slurry is dewatered by use of an inclined dewatering screw. The dewatered carbon is then weighed and fed into the reactivation furnace. Once the spent carbon is introduced into the reactivation unit, it is heated to remove moisture, and desorb organics at temperatures ranging from 800 degrees Fahrenheit to 1650 degrees Fahrenheit.

Many of the organics desorbed from the carbon in the reactivation unit are thermally destroyed in the high-temperature environment of the reactivation unit. In order to ensure adequate destruction and removal of any remaining organics, the reactivation unit is equipped with an external afterburner. The afterburner is provided to thermally oxidize any organics remaining in the off-gas stream. The reactivation unit is also equipped with additional air pollution control (APC) equipment.

A venturi scrubber is provided to remove particulate matter, a packed-bed scrubber for acid gas and particulate removal and lastly, a wet electrostatic precipitator (WESP) is provided for additional particulate matter control removal. The exhaust of the plant, via the stack, is basically 180 degree Fahrenheit steam.

The reactivated carbon, discharged from the bottom of the reactivation unit, is cooled using a large water-jacketed screw. The screw decreases the carbon temperature from 1600 degrees Fahrenheit to 200 degrees Fahrenheit. The reactivated carbon exiting the screw is transported, via a closed pipe, to the product packaging building where it is screened and packaged for reuse.

PLANT STAFFING

WCAI operates 24-hours per day, seven days per week and therefore is staffed continuously by operating personnel. The plant employs approximately 28 people, which includes the following:

- (1) Director, Plant Operations
- (1) Plant Manager
- (1) Environmental Health and Safety Manager
- (1) Profile Chemist
- (1) Traffic Controller
- (1) Administrative Assistant
- (4) Plant Operators
- (4) Assistant Plant Operators
- (2) Millwright/Electricians
- (10) Material Handler

SAFETY AND ENVIRONMENTAL COMPLIANCE

The WCAI facility has worked over 2,293 days (over 6 years) without a lost workday accident. Additionally, the facility is audited once per year by the Environmental Protection Agency Region IX and has not had a violation in the past seven (7) years.

COMMUNITY IMPACTS

WCAI employee payroll, including fringes, is approximately \$1,028,000 per year, a majority of which is spent in the Parker community. Additionally the plant pays approximately \$100,000 in local and state transaction and property taxes annually.

The facility also contributes to the community by making financial contributions to DARE and is a proud sponsor of Little League and soccer teams. WCAI has sponsored the District VI Soccer Tournament, which historically includes 200 participants.



U.S. Environmental Protection Agency
Pacific Southwest / Region 9



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Risk Assessment at Evoqua Water Technologies

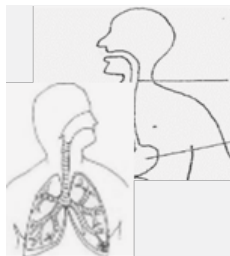
Steps to Risk Assessment

Measure Emissions

EPA conducted a trial burn at the facility to find out amounts of chemicals coming out of the Evoqua facility's smokestack.



Identify Possible Exposure Routes

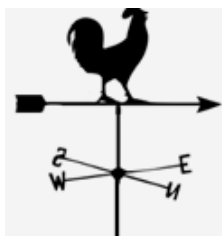


EPA considered exposures via:

- **Breathing** in of chemicals from the smokestack;
- **Eating** food or **touching** soils that have absorbed chemicals; and
- **Eating** fish potentially affected by chemicals in wastewater.

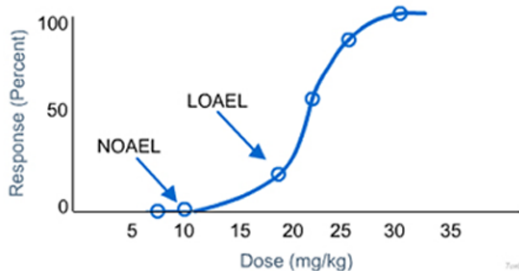
Determine Chemical Concentrations

EPA determined the concentrations of chemicals through those exposure pathways which could reach human and animal populations.



Calculate Potential Impacts

Based on information from existing scientific studies with these chemicals, EPA calculates the potential impacts to humans and animals.



Evoqua Quick Facts

What does the facility do?

The Evoqua facility treats spent carbon – a filtration material – by putting it in a furnace to remove contamination.

Where is the facility?

The facility is approximately a mile southeast of Parker, AZ.

How long has the Evoqua facility been around?

The Evoqua facility has been operating since 1992. But it has had different names throughout its lifetime including Siemens, US Filter, and Westates Carbon.

Why did EPA do a Risk Assessment?

The Evoqua facility is regulated by EPA under the Resource Conservation and Recovery Act (RCRA) because it handles hazardous waste. A Risk Assessment is one way to make sure that the facility is operating safely.

What is EPA doing now?

EPA will also be making a decision about whether or not to issue a RCRA permit to allow the facility to continue managing hazardous waste. Such a permit would create additional requirements for operations at the facility.

Risk Considerations

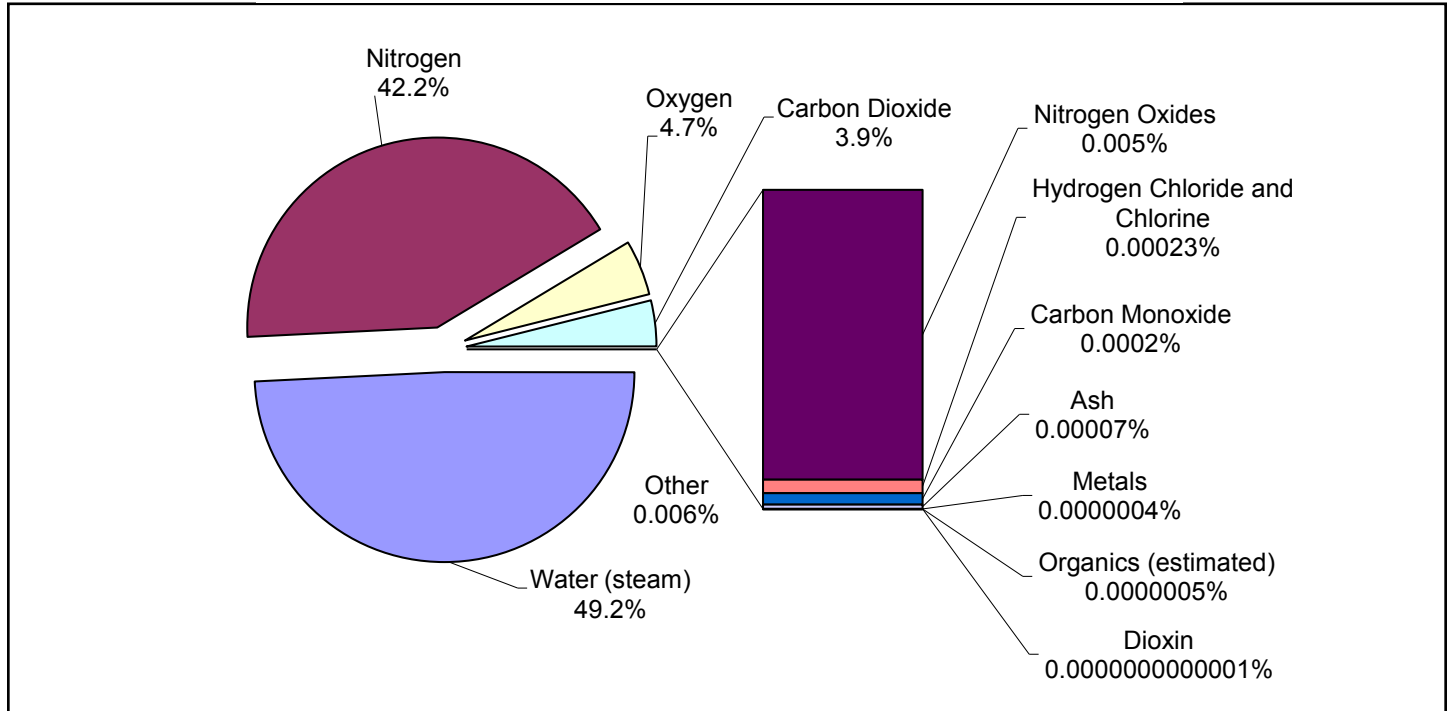
In conducting the risk assessment, EPA considered the following populations:

- Elderly
- Pregnant
- Children
- Facility Workers
- Farmers, Fishermen, and Hunters

1 in 100,000 is EPA's risk threshold. This means that in a town of 100,000 people, at most 1 additional person might develop cancer over a lifetime (70 years) of exposure to chemicals emitted from the Evoqua facility.

With regard to this threshold, EPA has determined that impacts from long-term exposure to the Evoqua facility emissions are insignificant.

What Typically Comes Out of the Smokestack?



Contacts

Please contact the following with questions or comments:

“Mike” Mahfouz Zabaneh, Project Manager
Phone: (415) 972-3348
zabaneh.mahfouz@epa.gov

Dr. Patrick Wilson, Senior Regional Toxicologist
Phone: (415) 972-3354
wilson.patrick@epa.gov

Mailing Address:

U.S. EPA Region 9 (LND-4-2)
75 Hawthorne Street
San Francisco, CA 94105

For media inquiries, please contact:
Margot Perez-Sullivan
Phone: (415) 947-4149
perezsullivan.margot@epa.gov

The complete text of the risk assessment is available online at:
www.epa.gov/region9/waste/evoqua

U.S. Environmental Protection Agency, Region 9
75 Hawthorne Street (LND-4-2)
San Francisco, CA 94105
Attn: Mahfouz Zabaneh

Official Business
Penalty for Private Use, \$300

Address Service Requested

FIRST-CLASS MAIL
POSTAGE & FEES
PAID
U.S. EPA
Permit No. G-35

Versión en Español incluida

La solicitud completa está disponible al público general para su revisión o para copiar, y se puede encontrar en las siguientes ubicaciones:

Biblioteca pública las tribus indias del Río Colorado
26600 Mohave Rd.
Parker, AZ 85344
(928) 669-1332

Biblioteca pública de Parker
1001 South Navajo Avenue
Parker, AZ 85344
(928) 669-2622

Para más información:

Puede encontrar una copia electrónica completa de la solicitud de permiso y obtener más información sobre la instalación de Evoqua Parker en el sitio web de la EPA: www.epa.gov/region9/waste/evoqua

Información, opiniones, consultas, y peticiones para ponerse en la lista de correo de la EPA con respecto a esta solicitud de RCRA, puede ser dirigido a través del proceso de revisión de la solicitud a la siguiente Gerente de Proyecto de RCRA de la EPA.

“Mike” Mahfouz Zabaneh, P.E.,
Ingeniero ambiental/Gerente de proyecto
Teléfono: (415) 972-3348
Fax: (415) 947-3533
zabaneh.mahfouz@epa.gov

Dirección postal:
US EPA Region 9, LND-4-2
75 Hawthorne Street
San Francisco, CA 94105

**Para consultas de medios de comunicación,
por favor póngase en contacto con:**
Margot Perez-Sullivan
Teléfono: (415) 947-4149
perezsullivan.margot@epa.gov

Para comunicarse con los solicitantes del permiso, por favor póngase en contacto con:

Monte McCue, Gerente de Planta
Evoqua Water Technologies, L.L.C.
2523 Mutahar St.
Parker, Arizona 85344
Tel (928) 669-5758 Ext 17 / Fax: (928) 669-5775
monte.mccue@evoqua.com
www.evoqua.com

Wilfred Nabahe, Director
Environmental Protection Office
Colorado River Indian Tribes
26600 Mohave Road
Parker, AZ 85344-7737
Phone: (928) 662-4336 / Fax: (928) 662-4337
epo@crit-nsn.gov



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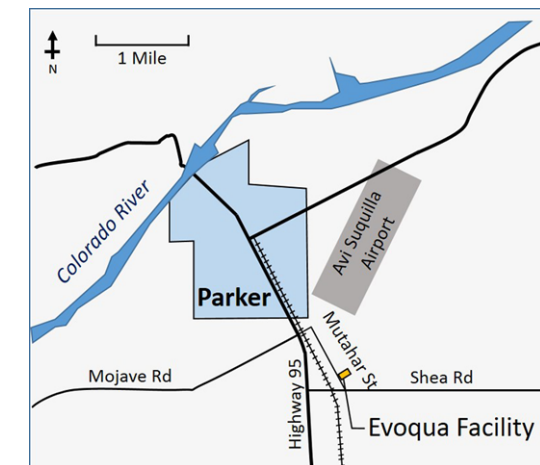
Community Information Fact Sheet for the Evoqua Water Technologies LLC Facility Near Parker, Arizona (Formerly Siemens, US Filter, and Westates/2523 Mutahar St., Parker, AZ 85344)

Facility Description

Evoqua Water Technologies LLC (Evoqua) operates a carbon regeneration facility located on the Colorado River Indian Tribes (CRIT) reservation near Parker, Arizona. Evoqua's process involves treating spent carbon in a regeneration furnace to purify it and make it available for reuse as a commercial product. The carbon Evoqua receives has been used to remove contaminants from air emissions and contaminated water. Annually, Evoqua receives over 5,000 tons of spent carbon from 30 - 35 states across the United States. About 11% of this spent carbon is considered hazardous waste and is regulated by the U.S. Environmental Protection Agency (EPA).



Photo of facility/Foto de la instalación



Map of facility/Mapa de la instalación

RCRA Regulatory History

Under the Resource Conservation and Recovery Act (RCRA), EPA is responsible for permitting facilities that manage RCRA-regulated hazardous wastes on tribal lands. Starting in 1991, EPA required new carbon regeneration furnaces to obtain hazardous waste permits. Like Evoqua (then known as US Filter/Westates), several facilities were already operating or had begun construction on carbon regeneration furnaces. These pre-existing facilities operate under “interim status” regulations while applying for a RCRA hazardous waste permit.

The first part of the permit application for the Evoqua Parker facility was submitted to EPA in 1995. There have been several sets of comments and requests for information from EPA that Evoqua addressed. As a result, several revisions to the permit application have been submitted by Evoqua to EPA.

Current Status

Evoqua certified the latest application submittal on March 17, 2016. CRIT, the beneficial landowner of the tribal land where the facility is located, is a co-applicant on the permit application. On April 8, 2016, the CRIT Tribal Council passed a resolution to endorse their December 2009 signature on the permit application. Two co-applicants' signatures made the application complete. The application was submitted on April 25, 2016, and was effective May 9, 2016.

After EPA staff reviews the complete permit application, EPA will announce a tentative decision on whether to issue or deny the permit and will open a 45-day public comment period. The complete application is available online at the link shown below. Copies can also be found at the locations indicated below. Please note that earlier documents, including on EPA's website, may still use previous facility names such as Siemens, US Filter, and Westates.

Community Involvement

EPA would like to hear from you during the 45-day public comment period that will be announced at a future date. A second fact sheet will be mailed out announcing the start of the public comment period and other pertinent information. During this period, EPA will hold a public meeting in Parker, Arizona. At the public meeting, general information will be provided about the facility. At the close of the informational public meeting, EPA will open a formal hearing during which the public may present comments regarding the tentative decision directly to EPA officials. Public comments may be submitted to the Agency during the entire 45-day comment period.

The complete application is currently available to the general public for review or copying and can be found at the following locations:

Colorado River Indian Tribes Public Library
26600 Mohave Rd.
Parker, AZ 85344
(928) 669-1332

Parker Public Library
1001 South Navajo Avenue
Parker, AZ 85344
(928) 669-2622

For further information:

You can find a complete electronic copy of the permit application and more information on the Evoqua Parker facility at EPA's website: www.epa.gov/region9/waste/evoqua

Information, opinions, inquiries, and requests to be added to EPA's mailing list regarding this RCRA application may be directed throughout the application review process to the EPA RCRA Project Manager:

"Mike" Mahfouz Zabaneh, P.E.,
Environmental Engineer/Project Manager
Phone: (415) 972-3348
Fax: (415) 947-3533
zabaneh.mahfouz@epa.gov

Mailing address:
US EPA Region 9, LND-4-2
75 Hawthorne Street
San Francisco, CA 94105

**For media inquiries,
please contact:**
Margot Perez-Sullivan
Phone: (415) 947-4149
perezsullivan.margot@epa.gov

To communicate with the permit applicants, please contact:

Monte McCue, Plant Manager
Evoqua Water Technologies, L.L.C.
2523 Mutahar St.
Parker, Arizona 85344
Phone: (928) 669-5758 Ext 17
Fax: (928) 669-5775
monte.mccue@evoqua.com
www.evoqua.com

Wilfred Nabahe, Director
Environmental Protection Office
Colorado River Indian Tribes
26600 Mohave Road
Parker, AZ 85344-7737
Phone: (928) 662-4336
Fax: (928) 662-4337
epo@crit-nsn.gov



Agencia de Protección Ambiental de
EE.UU. Suroeste del Pacífico/Región 9



Para Arizona, California, Hawaii, Nevada, las Islas del Pacífico y 148 tribus

División de terrenos
Oficina de permisos • Junio de 2016

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Hoja de información comunitaria para la instalación de Evoqua Water Technologies LLC cerca de Parker, Arizona (Antes Siemens, US Filter y Westates/2523 Mutahar St., Parker, AZ 85344)

Descripción de la instalación

Evoqua Water Technologies LLC (Evoqua) opera una instalación de regeneración de carbón, situada en la reserva de las tribus de indios del Río Colorado (CRIT, por sus iniciales en inglés) cerca de Parker, Arizona. El proceso de Evoqua consiste de tratar el carbón usado en un horno de regeneración para purificarlo y hacerla disponible para su reutilización como producto comercial. El carbón que Evoqua recibe ha sido utilizado para eliminar los contaminantes de las emisiones de aire y de agua contaminada. Cada año, Evoqua recibe más de 5.000 toneladas de carbón usado de 30-35 estados de todo Estados Unidos. Alrededor del 11% de este carbón se considera residuos peligrosos y está regulado por la Agencia de protección ambiental de Estados Unidos (EPA, por sus iniciales en inglés).

Por favor refiérase a la foto y mapa de la instalación en la primera página en la versión en Inglés.

Historia reguladora de RCRA

EPA es responsable bajo la ley de conservación y recuperación de los recursos (RCRA, por sus iniciales en inglés) de dar permiso a las instalaciones que manejan residuos peligrosos regulados por RCRA en tierras tribales. A partir de 1991, la EPA requiere que nuevos hornos de regeneración de carbón obtienen permisos de residuos peligrosos. Evoqua (antes conocida como US Filter/Westates), igual a varias otras instalaciones, estaba operando o habían comenzado la construcción de hornos de regeneración de carbón. Estas instalaciones existentes operan bajo regulaciones de "interim status" mientras solicitan un permiso de residuos peligrosos de RCRA.

La primera parte de la solicitud de permiso para la instalación de Evoqua Parker fue entregado a EPA en 1995. Han habido varios comentarios y solicitudes de EPA para mas información que Evoqua trató. Como resultado, varias revisiones de la solicitud de permiso han sido entregado a EPA por Evoqua.

Estado actual

Evoqua certificó la última versión de la solicitud el 17 de marzo de 2016. CRIT, el terrateniente benéfico de la tierra tribal donde está localizado la instalación, es un co-solicitante en la solicitud de permiso. El 8 de abril de 2016, el Consejo Tribal de CRIT aprobó una resolución para respaldar su firma de diciembre de 2009 en la solicitud del permiso. Estas dos firmas de los co-solicitantes hicieron la solicitud completa. La solicitud fue presentada el 25 de abril de 2016, y era en efecto el 9 de mayo 2016.

Después de que el personal de EPA revise la completa solicitud de permiso, la EPA tomará una decisión provisional sobre la conveniencia de emitir o denegar el permiso y abrirá un período de comentarios públicos de 45 días. La solicitud completa está disponible en el sitio web presentado en la sección "Para mas información". Podrá obtener copias también en los lugares indicados a continuación. Por favor, tenga en cuenta que los documentos anteriores, incluidos los del sitio web de la EPA, pueden utilizar nombres de instalaciones anteriores tales como Siemens, US Filter y Westates.

Participación de la comunidad

A EPA le gustaría oír sus opiniones durante el período de comentarios públicos de 45 días que se anunciará en una fecha futura. Se le enviará por correo una segunda hoja para anunciar el comienzo del periodo de comentarios públicos y de cualquier otra información pertinente. Durante este período, la EPA tendrá una reunión pública en Parker, Arizona. En la reunión pública, se proporcionará información general acerca de la instalación. Al concluir la reunión pública informativa, la EPA abrirá una audiencia formal durante la cual el público puede presentar comentarios sobre la decisión provisional directamente a los funcionarios de la EPA. Pueden presentarse los comentarios públicos a la Agencia durante el entero período de comentarios de 45 días.



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Fact Sheet: Proposed Permit for the Evoqua Water Technologies LLC Facility Near Parker, Arizona (Formerly Siemens, US Filter, and Westates / 2523 Mutahar St., Parker, AZ 85344)

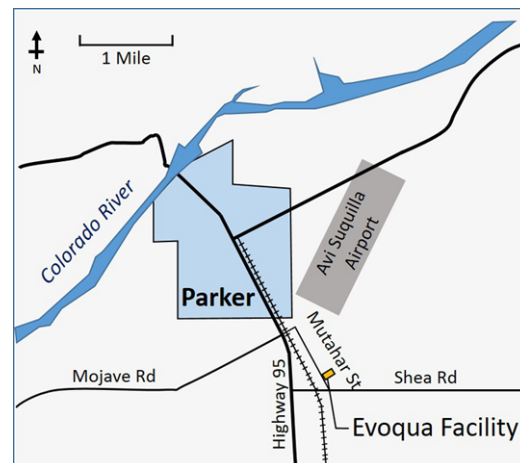
The U.S. Environmental Protection Agency (EPA) is proposing to issue a permit for hazardous waste management for the Evoqua Water Technologies LLC facility (Evoqua) near Parker, Arizona. The public has until November 15, 2016 to provide comments on the proposal and its accompanying draft permit. A public hearing on the proposal will be held by EPA on November 1, 2016 at the Bluewater Resort and Casino in Parker.

Facility Description

Evoqua operates a carbon regeneration facility located on the Colorado River Indian Tribes (CRIT) reservation near Parker, Arizona. Evoqua's process involves treating spent carbon in a regeneration furnace to purify it and make it available for reuse as a commercial product. The spent carbon that is shipped to the facility has been used to remove contaminants from air emissions and contaminated water at industrial and cleanup sites throughout the nation. Annually, the Evoqua facility receives over 5,000 tons of spent carbon from 30 - 35 states across the United States. About 11% of this spent carbon is considered hazardous waste and is regulated by EPA.



Photo of facility



Map of facility

RCRA Regulatory History

Under the Resource Conservation and Recovery Act (RCRA), EPA is responsible for permitting facilities that manage RCRA-regulated hazardous wastes on tribal lands. Starting in 1991, EPA required new carbon regeneration furnaces to obtain hazardous waste permits. At that time, the Evoqua facility (then known as US Filter/Westates) was already undergoing construction of a carbon regeneration furnace which meant it was eligible to operate under "interim status" RCRA regulations while applying for a RCRA hazardous waste permit.

The first part of the permit application for the Evoqua facility was submitted to EPA in 1995. There have been several sets of comments and requests for information from EPA that Evoqua addressed. As a result, several revisions to the permit application have been submitted by Evoqua to EPA. On May 9, 2016 EPA found that the permit application – signed by both the operator, Evoqua, and the beneficial landowner, CRIT – was complete.

Current Status

Based on the permit application and RCRA regulations, EPA is proposing a permit that sets operating requirements for the Evoqua facility to ensure protection of public health and the environment. The public has until November 15, 2016 to review the draft permit and supporting documents and provide comments to EPA. The complete application, the draft permit, the statement of basis, and other supporting documentation are available online at www.epa.gov/region9/waste/evoqua. Copies can also be found at the locations indicated below. Please note that earlier documents, including on EPA's website, may still use previous facility names such as Siemens, US Filter, and Westates.

Community Involvement

EPA would like to hear from you during the public comment period that starts on October 1 and ends on November 15, 2016. EPA will hold a public meeting and public hearing on November 1 at 7 p.m. in the Mohave Conference Room at the Bluewater Resort and Casino, located at 11300 Resort Drive in Parker, Arizona.

At the public meeting, general information will be provided about the facility. At the close of the informational public meeting, EPA will open a formal public hearing during which the public may present comments regarding the tentative decision directly to EPA officials. Any comments submitted verbally during the public hearing or in writing during the public comment period will be responded to in writing after the close of the comment period.

The complete application, the draft permit, the statement of basis, and other supporting documentation are currently available to the public for review or copying and can be found at the following locations:

U.S. EPA
75 Hawthorne St., 3rd Floor
San Francisco, CA 94105
(415) 947-4597

CRIT Museum and Library
26600 Mohave Rd.
Parker, AZ 85344
(928) 669-1332

Parker Public Library
1001 South Navajo Ave.
Parker, AZ 85344
(928) 669-2622

The complete application, the draft permit, the statement of basis, and other supporting documentation are on EPA's website at www.epa.gov/region9/waste/evoqua. Questions regarding this proposal or the draft permit may be directed to the EPA RCRA Project Manager: "Mike" Mahfouz Zabaneh, P.E. at (415) 972-3348 or zabaneh.mahfouz@epa.gov. Requests for documents contained in EPA's Administrative Record for this proposed decision may be submitted using the Freedom of Information Act at: <https://www.epa.gov/foia>.

Send comments to:

U.S. EPA Region 9, LND-4-2, 75 Hawthorne Street, San Francisco, CA 94105 or zabaneh.mahfouz@epa.gov.

For media inquiries, please contact:

Margot Perez-Sullivan; Phone: (415) 947-4149; perezsullivan.margot@epa.gov.

To communicate with the Evoqua facility, please contact:

Monte McCue, Plant Manager, Evoqua Water Technologies, L.L.C., 2523 Mutahar St., Parker, Arizona 85344; Phone: (928) 669-5758 Ext. 17; Fax: (928) 669-5775; monte.mccue@evoqua.com.



COLORADO RIVER INDIAN TRIBES

Colorado River Indian Reservation

ROUTE 1, BOX 23-B
PARKER, ARIZONA 85344
TELEPHONE (928) 669-9211

September 10, 2003

Karen Scheuermann
US EPA Region 9
75 Hawthorne Street
San Francisco, CA. 94105

RE: Designated Area of Potential Effects for US Filter/Westates, Parker AZ.

Dear Ms. Scheuermann:

At the meeting on Friday, August 1, 2003, with the Environmental Protection Agency (EPA), Town of Parker, US Filter/Westates, Arizona State Historic Preservation Office and representatives from the Colorado River Indian Tribes, on the issue of implementing the process of consultation within the guidelines of the Section 106 of the National Historic Preservation Act (NHPA), a process was begun regarding granting a permit decision for US Filter/Westates which operates on the Colorado River Indian Reservation (CRIR). Necessary discussion of roles and interactions of parties was gathered for establishing procedures for future consultation planning and government to government consultation.

One of the results from the meeting was the recommendation to establish the immediate Area of Potential Effect (APE) for cultural and spiritual effect. The cultural landscape in question comprises a significant core portion of traditional aboriginal territory for riverine Yuman and Numic speaking American Indian groups. This area is very significant to these native peoples in cultural, historical, ecological, religious and cosmological terms. Review of past archaeology interpretations, elders recommendations from previous projects and oral stories from tribal members, helped institute the difficult decision to set boundaries on lands that hold traditional beliefs concerning tribal origins, cultural history, ceremonial activities and sacred sites. While the US Filter/Westates facility was sited on tribal land in 1992, in a area set apart for industrial activity, it impacts other important aspects of a cultural landscape. The cultural landscape use area is not limited to air, water, and land. The cultural importance of these environmental media must be taken into consideration in addition to cultural and spiritual effects. Therefore, in establishing the area of potential effect, the decision was based on factors pertaining to these.

The mesa on which the US Filter/Westates sits on is bounded in the south by the Bouse Wash and by Mesquite Mountain, in the north by the Whipple Mountains, Black Peak to the east and the Parker Valley to the west. The most dominant feature of the Valley is the Colorado River and its

floodplain. Clearly, the river was the most important water source for the Indian peoples who lived in and cultivated the alluvial soils of the valley.

This desert environment includes plant communities of creosote bush, seasonal grasses, mesquite, sage, scrub brush and a number of other plants that were important to the Indian inhabitants for food, medicine, ceremonies and manufacture. Animals such as coyote, fox, rabbits, lizards, and various bird and fish species utilized the riparian habitat and were also important resources used by the Indian peoples of the area.

As the consultation compliance begins, there are some concerns. They are:

- To lessen adverse effects and preserve cultural values. ✓
- The review of intellectual property rights and the issues concerning confidentiality.
- Should the Tribes desire further consultation concerning the identifications of traditional cultural places, in accordance with various federal laws.

There are several federal laws in effect which take into account locations and cultural landscapes deemed sacred to particular Native Americans individuals and tribes. Under the auspices of these laws, US EPA must put in the record the effects of the US Westates facility have on these locations as identified by Native Americans tribes during this permitting process. These laws include the National Historic Preservation Act of 1966 (NHPA), as amended; National Environmental Policy Act of 1969 (NEPA) as amended; Native American Graves Protection and Repatriation Act of 1990 (NAGPRA), as amended; American Indian Religious Freedom Act of 1978 (AIRFA); Executive Order 13007-Indian Sacred Sites; Clean Air Act, as amended; and the Clean Water Act, as amended; and Environmental Justice. ✓

In closing, we look forward to a positive working relationship with those involved in the process of compliance of Section 106 of the National Historic Preservation Act. You may call Museum Director, Betty L. Cornelius, at (928) 669-9211 should you have any questions.

Sincerely,



Daniel Eddy Jr.
Chairman

Colorado River Indian Tribes